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Mr. Todd Mullins, FFA Manager Kentucky Department for Environmental Protection Division of Waste Management 200 Fair Oaks Lane, 2nd Floor Frankfort, Kentucky 40601

Ms. Jennifer Tufts Remedial Project Manager U.S. Environmental Protection Agency, Region 4 61 Forsyth Street Atlanta, Georgia 30303

Dear Mr. Mullins and Ms. Tufts:

TRANSMITTAL OF THE REMEDIAL DESIGN REPORT *IN SITU* SOURCE TREATMENT USING DEEP SOIL MIXING FOR THE SOUTHWEST GROUNDWATER PLUME VOLATILE ORGANIC COMPOUND SOURCE AT THE C-747-C OIL LANDFARM (SOLID WASTE MANAGEMENT UNIT 1) AT THE PADUCAH GASEOUS DIFFUSION PLANT PADUCAH, KENTUCKY, DOE/LX/07-1276&D2

Please find enclosed for approval the *Remedial Design Report In Situ Source Treatment Using Deep Soil Mixing for the Southwest Groundwater Plume Volatile Organic Compound Source at the C-747-C Oil Landfarm (Solid Waste Management Unit 1) at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky*, DOE/LX/07-1276&D2, (RDR) document. We look forward to receiving approval from your respective organizations in the next 30 days.

This final RDR for Solid Waste Management Unit (SWMU 1) incorporates responses to comments provided by the U.S. Environmental Protection Agency and the Kentucky Department for Environmental Protection based on their reviews of the D1 (90%) RDR and agreements developed in parallel discussions among the Federal Facility Agreement (FFA) parties regarding optimization of the D1 design. Discussions on design optimization stemmed from resolution of the estimate of volatile organic contaminant mass and mass distribution, an understanding of increased treatment efficiency based on the use of steam, an increase in the source area volume from that assumed at the time of the Focused Feasibility Study, the opportunity to reduce the remedy time frame regarding reduction of impacts to groundwater, and the objective of effective resource management regarding implementation costs.

If you have any questions or require additional information, please contact David Dollins at (270) 441-6819.

Sincerely,

William E. Murphie

Manager

Portsmouth/Paducah Project Office

Enclosures:

- 1. Remedial Design Report
- 2. Redline of Remedial Design Report
- 3. CRS for EPA Comments on 90% Remedial Design Report
- 4. CRS for KDEP Comments on 90% Remedial Design Report

e-copy w/enclosures:

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CERTIFICATION

Document Identification:

Remedial Design Report In Situ Source Treatment Using Deep Soil Mixing for the Southwest Groundwater Plume Volatile Organic Compound Source at the C-747-C Oil Landfarm (Solid Waste Management Unit 1) at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky, DOE/LX/07-1276&D2

I certify under penalty of law that this document and all attachments were prepared under my direction or supervision in accordance with a system designed to ensure that qualified personnel properly gather and evaluate the information submitted. Based on my inquiry of the person or persons directly responsible for gathering the information, the information submitted is, to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment for knowing violations.

LATA Environmental Services of Kentucky, LLC

Mark J. Duff Paducah Project Manager

6-21-13 Date Signed

I certify under penalty of law that this document and all attachments were prepared under my direction or supervision in accordance with a system designed to ensure that qualified personnel properly gather and evaluate the information submitted. Based on my inquiry of the person or persons directly responsible for gathering the information, the information submitted is to the best of my knowledge and belief, true, accurate, and complete. I am aware that there are significant penalties for submitting false information, including the possibility of fine and imprisonment for knowing violations.

U.S. Department of Energy (DOE)

William E. Murphie, Manager

Portsmouth/Paducah Project Office

Date Signed

Remedial Design Report In Situ Source Treatment Using Deep Soil Mixing for the Southwest Groundwater Plume Volatile Organic Compound Source at the C-747-C Oil Landfarm (Solid Waste Management Unit 1) at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky



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Remedial Design Report

In Situ Source Treatment Using Deep Soil Mixing
for the Southwest Groundwater Plume Volatile Organic
Compound Source at the C-747-C Oil Landfarm
(Solid Waste Management Unit 1)
at the Paducah Gaseous Diffusion Plant,
Paducah, Kentucky

Date Issued—June 2013

U.S. DEPARTMENT OF ENERGY Office of Environmental Management

Prepared by
LATA ENVIRONMENTAL SERVICES OF KENTUCKY, LLC
managing the
Environmental Remediation Activities at the
Paducah Gaseous Diffusion Plant
under contract DE-AC30-10CC40020

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ACRONYMS

acfm actual cubic feet per minute

ARAR applicable or relevant and appropriate requirement

bgs below ground surface
BTU British thermal unit
CI confidence interval
COC contaminant of concern

DNAPL dense nonaqueous-phase liquid
DOE U.S. Department of Energy
DQO data quality objective
DSS Decision Support Software

EPA U.S. Environmental Protection Agency

E/PP excavation/penetration permit

EVS-ES Environmental Visualization Systems Expert System

FFA Federal Facility Agreement
FFS focused feasibility study
FID flame ionization detector
GAC granular activated carbon
GC gas chromatograph

HP horsepower

HU hydrogeologic unit

IDW inverse distance weighting

KDEP Kentucky Department for Environmental Protection

KO knock-out tank
LDA large diameter auger
LUC land use control

MACT Maximum Achievable Control Technologies

MDL method detection limit
MW monitoring well
NAL no action level
OU operable unit

PAH polycyclic aromatic hydrocarbon

PC personal computer

PGDP Paducah Gaseous Diffusion Plant

PID photoionization detector psig per square inch gauge

QAPP Quality Assurance Project Plan

RA remedial action

RAO remedial action objective RAWP remedial action work plan RDR remedial design report

RDSI remedial design support investigation

RDWP remedial design work plan
RGA Regional Gravel Aquifer
RI remedial investigation
ROD record of decision
SI site investigation
SPT standard penetration test

SWMU

UCRS

solid waste management unit Upper Continental Recharge System vapor conditioning system VCS variable frequency drive VFD volatile organic compound VOC WAG

waste area grouping zero-valent iron ZVI

EXECUTIVE SUMMARY

This Remedial Design Report (RDR) has been prepared for the *In Situ* Source Treatment Using Deep Soil Mixing with Interim Land Use Controls (LUCs) Remedial Action (RA) for the Southwest Plume volatile organic compound (VOC) source area, Solid Waste Management Unit 1 at the Paducah Gaseous Diffusion Plant (PGDP) in Paducah, Kentucky. This remedial design report was prepared in accordance with the Comprehensive Environmental Response, Compensation, and Liability Act and is the response action selected in the *Record of Decision for Solid Waste Management Units 1, 211-A, 211-B, and Part of 102 Volatile Organic Compound Sources for the Southwest Groundwater Plume at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky, DOE/LX/07-0365&D2/R1 (ROD) (DOE 2012a).*

The response action for VOCs selected in the ROD is required to address the release of hazardous substances into the environment that are sources of groundwater contamination and present unacceptable risk from direct exposure to residual VOCs and non-VOCs. Removal of VOCs, like trichloroethene, from the soils in the Southwest Plume source areas will contribute to the final cleanup of the Groundwater Operable Unit at PGDP.

The ROD specified an *in situ* source treatment using deep soil mixing with interim LUCs. The RA also will include the implementation of interim LUCs consisting of the Excavation/Penetration Permit Program and the posting of warning signs at the source area(s).

This report contains information regarding the design of the *in situ* source treatment using deep soil mixing remediation system, including discussions of the following:

- Mixing soil using large diameter augers;
- Injecting hot air and steam to volatize targeted contaminants;
- Injecting zero-valent iron as a polishing step for treating residual VOCs;
- Treating recovered vapor through a vapor conditioning/treatment system;
- Treating condensate via localized air stripping and/or granular activated carbon;
- Excavating 2 ft of surface soil, stockpiling, and respreading after the completion of mixing; and
- Collecting data and monitoring.

This D2 RDR incorporates responses to comments provided by the U.S. Environmental Protection Agency and the Commonwealth of Kentucky based on their reviews of the D1 (90%) RDR and in agreements developed in parallel discussions among the Federal Facility Agreement parties regarding optimization of the D1 design.



1. INTRODUCTION

This Remedial Design Report (RDR) presents the design for the remedial action (RA) to be implemented at the Southwest Groundwater Plume source area at Paducah Gaseous Diffusion Plant (PGDP) at Solid Waste Management Unit (SWMU) 1. The remedy planned for SWMU 1 is documented in the *Record of Decision for Solid Waste Management Units 1, 211-A, 211-B, and Part of 102 Volatile Organic Compound Sources for the Southwest Groundwater Plume at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky, DOE/LX/07-0365&D2 (ROD) (DOE 2012a). The overall design process is described in the <i>Remedial Design Work Plan for Solid Waste Management Units 1, 211-A, and 211-B Volatile Organic Compound Sources for the Southwest Groundwater Plume at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky*, DOE/LX/07-1268&D2/R1 (RDWP) (DOE 2012b).

Remedial design information provided in this report includes the following:

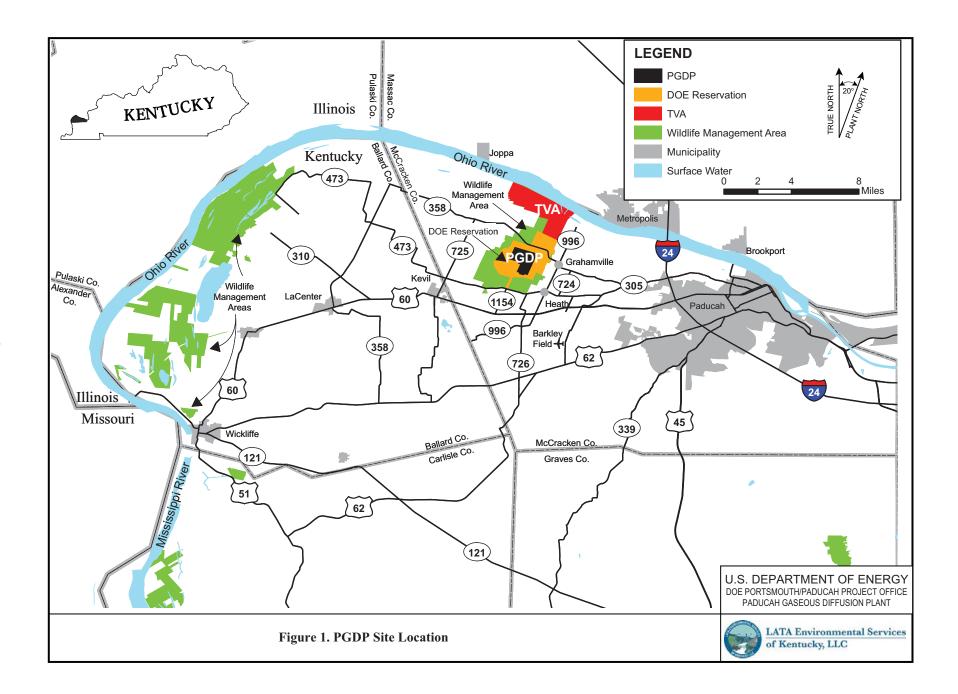
- Site description
- Technology description
- Remedial action objectives
- Design requirements
- Construction requirements

PGDP, located approximately 10 miles west of Paducah, Kentucky, and 3.5 miles south of the Ohio River in the western part of McCracken County, is an active uranium enrichment facility owned by the U.S. Department of Energy (DOE) (Figure 1). Bordering PGDP to the northeast, between the plant and the Ohio River, is the Tennessee Valley Authority Shawnee Fossil Plant.

The Southwest Groundwater Plume refers to an area of groundwater contamination at PGDP in the Regional Gravel Aquifer (RGA), which is south of the Northwest Groundwater Plume and west of the C-400 Cleaning Building (also known as the C-400 Building). The plume was identified during the Waste Area Grouping (WAG) 27 Remedial Investigation (RI) in 1998 (DOE 1999). Additional work to characterize the plume was performed as part of the WAG 3 RI (DOE 2000a) and Data Gaps Investigation (DOE 2000b). As discussed in these reports, the primary groundwater contaminant of concern for the Southwest Groundwater Plume (hereinafter referred to as the Southwest Plume) is trichloroethene (TCE). Other contaminants found in the plume include additional volatile organic compounds (VOCs), metals, and the radionuclide technetium-99 (Tc-99).

DOE conducted a site investigation (SI) in 2004 to address the uncertainties associated with potential source areas to the Southwest Plume that remained after previous investigations. The SI further profiled the current level and distribution of VOCs in the dissolved-phase plume along the west plant boundary. Results of the SI were reported in the *Site Investigation Report for the Southwest Groundwater Plume at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky*, DOE/OR/07-2180&D2/R1 (DOE 2007). The Focused Feasibility Study (FFS) (DOE 2010a) is based on the SI (DOE 2007), as well as previous investigations. A Remedial Design Support Investigation (RDSI) was performed in 2012 consistent with the RDWP (DOE 2012b). Existing analytical data from the SWMU 1 source area is included on a CD as Appendix A.

The RA includes the implementation of *in situ* soil mixing with large diameter augers (LDAs) combined with the introduction of hot air and/or steam for thermal volatilization and stripping of VOCs in the soil and groundwater in the target treatment zone and injection of zero-valent iron (ZVI). The RA also



includes the implementation of interim land use controls (LUCs) consisting of the Excavation/Penetration Permit Program (E/PP) and the posting of warning signs at the source areas.

An RDSI is included in the RA that was completed during July, August, and September 2012. The data collected while implementing the RDSI was used to further delineate areas of TCE impacts in the Upper Continental Recharge System (UCRS) soils and in the upper RGA [hydrogeologic unit (HU4)]. The additional data was used to refine the area to be treated by the soil mixing process. Refer to Section 1.3 for more detailed information regarding the RDSI.

This RDR design report provides information regarding the remediation system, based on unit processes and activities to be included in the *in situ* source treatment. These processes and activities will include the following:

- Mixing soil using LDAs;
- Heating soil *in situ* by application of hot air/steam;
- Removing VOCs and steam from heated subsurface zones by vacuum extraction;
- Treating recovered vapor off-gas via vapor conditioning/treatment systems;
- Injecting a ZVI slurry mixture;
- Treating condensate via localized air stripping and/or granular activated carbon (GAC); and
- Collecting real-time data and monitoring contaminant concentrations in vapor phase during extraction and treatment.

This D2 RDR for SWMU 1 incorporates responses to comments provided by the U.S. Environmental Protection Agency (EPA) and the Commonwealth of Kentucky based on their reviews of the D1 (90%) RDR and in agreements developed in parallel discussions among the Federal Facility Agreement (FFA) parties regarding optimization of the D1 design. Discussions on design optimization stemmed from resolution of the estimate of volatile organic contaminant mass and mass distribution, an understanding of increased treatment efficiency based on the use of steam, an increase in the source area volume from that assumed at the time of the FFS, the opportunity to reduce the remedy time frame regarding reduction of impacts to groundwater, and the objective of effective resource management regarding implementation costs. Design optimization discussions were held on April 10, 2013, in Atlanta, Georgia, on May 7, May 15, and May 16, 2013, and on June 16 and 17, 2013, via audio/Web-based conferencing. The following items composed the basis of discussion for optimization and describe the consensus/technical agreement reached by the parties regarding impacts to the final design.

- Inclusion of Historical Analytical Results for TCE in Soil: The parties reviewed available historical results for TCE in soil and determined that results from the following investigations contained analytical data that could be used to supplement the data obtained during the 2012 Remedial Design Support Investigation.
 - WAG 27 RI, 1998; and
 - SI Report for the Southwest Groundwater Plume, 2004.

These data formed the basis of evaluation in the FFS, Proposed Plan and ROD. The parties agreed that data generated as part of the Phase II SI (DOE 1992) would not be used in developing the map of

the TCE source area based on differences in investigation data quality objectives and changes in analytical technology.

- **Distribution of TCE Contamination in Soil at SWMU 1:** The TCE soil analytical data set was interpolated using C Tech Environmental Visualization Systems Expert System (EVS-ES). EVS-ES provides a number of methods for interpolating the data. The FFA parties reviewed the results of interpolating with the following methods:
 - Inverse distance weighting (IDW);
 - Nearest neighbor; and
 - Kriging.

Ultimately, the FFA parties agreed to use Kriging as the interpolation method with Octant search for developing the vertical and horizontal extent of the TCE contamination with the use of the following agreed to approaches:

- The TCE concentration area exceeding the TCE cleanup level of 73 μg/kg was determined using nominal (50% confidence interval) Kriging interpolation and is estimated to be approximately 13.500 ft².
- A 90% confidence interval of the Kriging interpolation was used to determine the location of the 1,000 μ g/kg and 10,000 μ g/kg TCE isoconcentration areas, which are estimated to be approximately 9,900 ft² and 3,700 ft², respectively.

The volume of TCE estimated to be present within the area of each isoconcentration was calculated and greater than 96% of the TCE volume is located within the 90% confidence interval of the $1,000~\mu g/kg.4$

Treatment Efficiency—The treatment technology employed in the final design has a demonstrated record of performance that indicates the contaminant removal rates in excess of 99% are expected, as opposed to the 91% removal rate assumed in the FFS, Proposed Plan, and ROD. The increase removal is rate is due to the combination of steam enhanced vapor stripping, combined with soil mixing and injection of ZVI.

Remedy Time Frame—Based on an anticipated treatment efficiency (> 99%) in combination with increased understanding of VOC mass distribution (> 96% of the VOC mass is located within the area within the 1,000µg/kg TCE contour), and mixing of soils that are \geq 1,000 µg/kg TCE, plus selected targeted boring in areas outside the 1,000 µg/kg contour, it is anticipated that the leaching of residual VOCs will impact RGA groundwater at levels that exceed the maximum contaminant level of 5 µg/L TCE for approximately 40 years as opposed to 68 years (as assumed in the ROD with treatment (at 91% treatment efficiency) of soils that are \geq 73 µg/kg TCE).

Large Diameter Auger/Soil Mixing Area—The FFA parties evaluated a number of approaches to determining the area to be mixed. The 90% RDR included mixing of all areas \geq 73 µg/kg TCE. Subsequent discussions focused on conditions and evaluations described above with the intent of satisfying the goal of the ROD by reducing impacts to the RGA groundwater within the time frame identified in the ROD. Based on the available information the parties agreed to the following soil mixing configuration:

• The perimeter of the soil boring array will consist of large diameter auger borings placed on center along the 1,000 μ g/kg TCE contour.

- Borings within the area defined by ≥ 1,000 µg/kg TCE and ≤ 10,000 µg/kg TCE will retain a target overlap of 10%. Boring placement may require some boring to have greater than 10% overlap and some boring to have less than 10% overlap.
- Borings within the area defined by $\geq 10,000~\mu g/kg$ TCE will retain a target overlap of 17.5%. Boring placement may require some boring to have greater than 17.5% overlap and some boring to have less than 17.5% overlap.
- Two areas will have targeted borings that are placed in areas that contain apparent uncertainty based on isoconcentration configurations. These area are as follows:
 - Along the east side of the northern lobe in the vicinity of soil sample boring locations 001–169 and 001–303, a series of borings will be located outside the perimeter of borings that are located on center of the 1,000 μg/kg TCE contour. Approximately 4–6 borings will be located outboard of the perimeter array. These borings will not have overlap.
 - Along the east-southeastern side of the source area in the vicinity of soil sample boring locations 001-308 and 001-160, a series of borings will be located outside the perimeter of borings that are located on center of the 1,000 μg/kg TCE contour. Approximately 7–9 borings will be located outboard of the perimeter array. These borings will not have overlap.

1.1 REGIONAL GEOLOGY AND HYDROGEOLOGY

PGDP is underlain by a sequence of clay, silt, sand, and gravel layers deposited on limestone bedrock. The sediments above the limestone bedrock are grouped into three major stratigraphic units: (1) loess, (2) continental deposits, and (3) McNairy Formation. The continental deposits are further divided into the subunits of upper continental deposits and lower continental deposits. Hydrogeologically, there are three major units: (1) UCRS, upper continental deposits; (2) RGA, lower continental deposits; and (3) McNairy Flow System.

The upper-most stratigraphic unit consists of fill (upper 2 ft or less in the area of the RDSI) and a layer of wind-deposited silt, or loess, extending from the surface to a depth of approximately 20 ft below ground surface (bgs). Beneath the loess, the upper continental deposits, a subunit of the continental deposits consisting of discontinuous sand and gravel layers interbedded with silt and clay, extend to an average depth of approximately 55 ft bgs. These deposits comprise the local hydrostratigraphic unit known as the UCRS. The lower continental deposits, also a subunit of the continental deposits, is a highly permeable layer of gravelly sand and chert gravel, typically extending from approximately 55 to 92 ft bgs. These deposits comprise the local hydrostratigraphic unit known as the RGA. Below the continental deposits is the McNairy Formation, a sequence of marine silts, clays, and fine sands that extends from approximately 92 to 350 ft bgs. These deposits comprise the local hydrostratigraphic unit known as the McNairy Flow System.

The UCRS is subdivided into the HU1, HU2, and HU3 units and consists of the loess (HU1) and the underlying upper continental deposits (HU2 and HU3). The sand and gravel lenses of the HU2 unit are separated from the underlying RGA by a 12- to 18-ft thick silty or sandy clay interval designated as the HU3 aquitard. The aquitard reduces the vertical flow of groundwater from the sands and gravels of the HU2 unit to the gravels of the RGA. The RGA is the uppermost aquifer in the Southwest Plume source areas. The RGA consists of an upper thin sand unit (HU4), which is the basal unit of the Upper

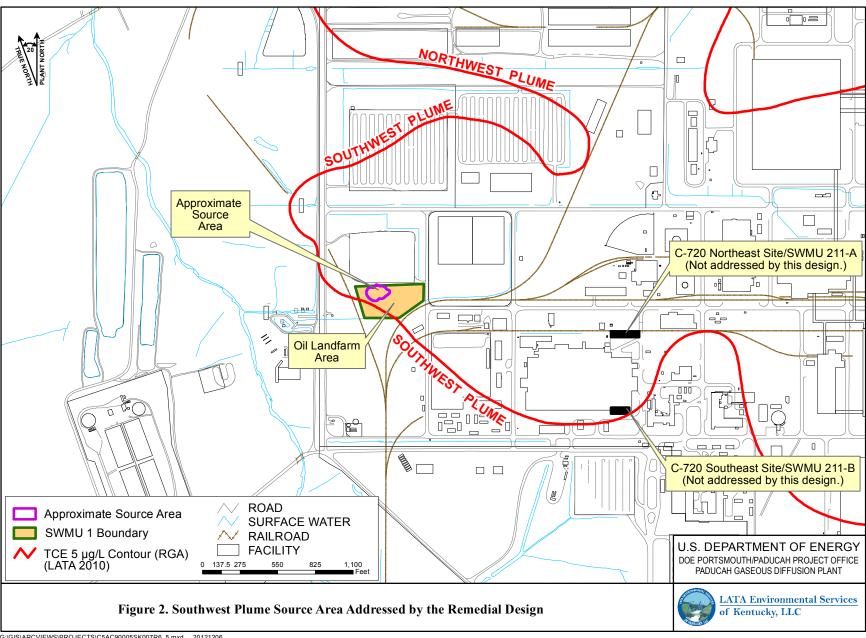
Continental Deposits, and a 30-ft thick sandy gravel unit (HU5), which comprises the Lower Continental Deposits beneath most of PGDP. Below the RGA is the McNairy Flow System, which corresponds to the McNairy Formation. The uppermost portion of the McNairy Flow System typically is a clay or silty clay, which restricts groundwater flow between the RGA and McNairy Flow System.

The depth of the water table within the UCRS varies considerably across PGDP. Monitoring wells (MWs) MW161 and MW162 are directly adjacent to the northern edge of SWMU 1 and are screened in the RGA from 78 to 83 ft (bgs) and the UCRS from 18 to 24 ft (bgs), respectively. Both monitoring wells were installed in 1991 and have had periodic water levels measured from 1991 to the present. MW162 (UCRS) has an average water level of 12.6 ft, while MW161 (RGA) has had an average water level over the same time period of 45.8 ft. Water within the UCRS tends to flow downward to the RGA. Groundwater flow in the RGA generally is to the northwest, although there is evidence for some divergent flow to the east and to the west as part of the Northeast and Southwest Plumes, respectively. Flow direction for RGA groundwater in the area of SWMU 1 is northwest. Divergent flow is limited primarily to the area of the PGDP site and is influenced mainly by anthropogenic recharge due to loss of water from plant piping systems for raw, sanitary, cooling, and fire water and focused infiltration from engineered runoff controls, such as paved areas, building roofs, lagoons, and ditches most of which are predominantly north and east of the SWMU 1 area.

1.2 TREATMENT SITE LOCATION

The treatment location for this RA is SWMU 1, C-747-C Oil Landfarm (Oil Landfarm), which is located near the western edge of the PGDP. The location of the SWMU 1 source area (Oil Landfarm) is shown in Figure 2 and is the focus of this RDR. SWMU 1 lies south of the C-745-A Cylinder Storage Yard. Railroads with associated drainage ditches bound SWMU 1 on the south, west, and southeast; 4th Street lies to the east and provides gravel road access to the SWMU 1 area.

No underground utilities are located in the area to be soil mixed. Storm drains associated with the C-745-A Cylinder Storage Yard lies to the north. Buried storm drains also are located to the south away from the area to be soil mixed. Raw water and plant water lines are located on the southern edge of SWMU 1. See Figure 2. The SWMU 1 area has been investigated several times in support of remedy selection and development of this remedial design including the Phase II SI (1991); WAG 27 RI (1997); Southwest Plume SI (2004); and the RDSI (2012). The potential Southwest Plume source areas investigated in the Southwest SI included the C-747-C Oil Landfarm (Oil Landfarm) (SWMU 1); C-720 Building Area near the northeast and southeast corners of the building [C-720 Northeast Site (SWMU-211A) and C-720 Southeast Site (SWMU 211B)]; and the storm sewer system between the south side of Building C-400 and Outfall 008 (Storm Sewer) (part of SWMU 102) (DOE 2007). As a result of the Southwest Plume SI sampling, the storm sewer subsequently was excluded as a potential VOC source to the Southwest Plume.



1.3 REMEDIAL DESIGN SUPPORT INVESTIGATION

The RDSI was conducted in 2012 to gather supplemental data necessary for the design and implementation of the *in situ* source treatment deep soil mixing remedial action selected for SWMU 1. Furthermore, this RDSI field effort involved the collection of contaminant characterization and engineering design-related data at the C-720 SWMUs. This data will be used to support the Federal Facility Agreement parties' decision regarding selection and implementation of either enhanced *in situ* bioremediation or long-term monitoring strategies and the subsequent remedial design efforts. The design and implementation of either the enhanced *in situ* bioremediation or long-term monitoring RA for the C-720 Building will follow the remedial action at SWMU 1 by an estimated two years.

An RDSI Characterization Plan was developed as part of the RDWP to support the implementation of the selected alternatives for remediation at the Southwest Plume and to resolve data gaps identified through a data quality objectives process (DOE 2010b). Data collected during the RDSI, coupled with data from previous investigations, has allowed for a more refined delineation of TCE concentrations in the UCRS soils and in the upper RGA (HU4) to better define the size and shape of the overall treatment area for this remedial action. The RDSI consisted of 18 primary borings and 4 contingency borings. The contingency borings were drilled and incorporated consistent with decision rules contained in the RDSI work plan and to allow refinement of the lateral extent of the source treatment area. Results of the RDSI sampling efforts collected in support of the RDR are included in Table 1 and are based on analytical results received from the fixed-base laboratory. A total of 13 boreholes contained an average TCE result that exceeded the soil cleanup level of 73 micrograms per kilogram (μ g/kg) (see Draft-Final Average column in Table 1). There were 11 boreholes that exceeded the TCE soil cleanup level in samples collected below the interval beginning at 55 ft bgs. Five boreholes had average concentrations that exceed the cleanup levels for TCE degradation compounds and 1,1-dichloroethene (DCE).

Specifically, there is one borehole that exceeded cleanup levels for *cis*-1,2-DCE, vinyl chloride, and 1,1-DCE accounting of three of the four instances. The other instance of cleanup level exceedance was for *cis*-1,2-DCE. All exceedances of the TCE breakdown products and 1,1-DCE also coincided with the exceedances of TCE, as would be expected. As such, it will not be necessary to conduct mixing and treatment of other VOC areas located outside of the overall TCE treatment area footprint.

Soil sampling results from RDSI sampling efforts at SWMU 1 are presented on Table 1. For each RDSI soil boring location (001-301 through 001-322), the depth-specific data has been presented for each detected VOC and an arithmetic average has been calculated for each detected VOC at each soil boring location. Arithmetic average concentrations have been calculated for borings in instances where the VOC was not detected above the sample-specific method detection limit (MDL). For the depth intervals within the boring that were nondetect for the VOC, one-half of the MDL was used in calculating the average borehole VOC concentration within the boring. The average values then were rounded to the nearest whole number.

In addition to the RDSI data, 49 historical soil borings were used in the development of the dataset used to support the selection of the area to be soil mixed. These historical soil borings were drilled as part of the WAG 27 and Southwest Plume SIs, performed in 1997 and 2004, respectively. The sample results from those borings are contained in Table 3. The sample results also were used to determine the area of SWMU 1 to be soil mixed and is discussed in Section 1.4, Environmental Visualization Software Evaluation-TCE Extent and Mass Estimate.

Table 1. Southwest Plume RDSI Characterization Data

										DRAFT Final a	nd Preliminary S	oil Analytical Dat	ta (SWMU 1	, C-747-C Oil	Landfarm)											
	Date of	Depth		PID		TO	CE (μg/Kg)			cis -1	2-DCE (μg/Kg)	•		trans	-1,2-DCE (μg/l	Kg)			VC (μg/Kg)				1,1	L DCE (μg/Kg)		
							(10, 0,																ĺ	11 01 01		
Boring ID			Actual Sample		Preliminary	Preliminary	Draft Final	Draft Final		Preliminary	Draft Final	Draft Final		Preliminary	Draft Final		Draft Final	Preliminary	Draft Final		Draft Final		Preliminary	Draft Final		Draft Final
	(collection)	bgs	Depth bgs (ft)	(ppb)	Reported	Average ^{1,2}	Reported Qu	al ⁸ Average ⁹	Reported	Average ^{1,2}	Reported Q	ual ⁸ Average ⁹	Reported	Average ^{1,2}	Reported	Qual ⁸	Average ⁹	Reported Average ^{1,2}	Reported	Qual ⁸	Average ⁹	Reported	Average ^{1,2}	Reported	Qual ⁸	Average ⁹
			Ifarm UCRS Soil Cleanu				73				600				1080				34					130		_
			5 NA	0	120	120	140	140	ND	0.24	0.56	U 0.28	8 ND	0.375	0.44	4 U	0.22	ND 0.1	7 0.	.4 U	0.2	ND	0.65	1.5	U	0.75
			10 8.0	200	290	290	350	350	ND	4.3	10	U 5	5 ND	3.35	8.2	2 U	4.1	ND 11.	5 2	.8 U	14	ND ND	10	24	U	12
			15 13.0	437			1300	1300	ND	4.3	10	U 5	5 ND	3.35	7.8	3 U	3.9	ND 11.		.7 U	13.5	ND ND	10	23	U	11.5
	7/20/2012		20 15.5	399			770	770	ND	3.9	8.9	U 4.45			7	7 U	3.5	ND 10.		4 U	12		9	21		10.5
	1, 20, 2022		25 20.5	56			590	590	ND	3.8	8.3	U 4.15			6.5		3.25	ND 1		2 U	11		9	19		9.5
			30 27.0 35 34.9	1,717			6300	6300	360	360 420	430	430			8.1 7.9		4.05	ND 11.		8 U	14 13.5		10 9.5	24		12
001-311			40 35.1	19,820 2,650			8300 5500	8300 5500	420 310	310	510 370	510 370			7.5		39.5 3.7	ND 1 ND 10.		5 U	13.5		9.5	23 22		11.5
			45 40.5	9,280			2400	2400	130	130	160	J 160		3.03	7.5		3.75	ND 10.		.5 U	12.5		9.5	22		11
		1	5D ³ 40.5	9,280	1	+	1200	2400	78	130	91	1 100	ND ND	3.2	7.4		5.75	ND 1	2		12.3	ND ND	5.5	22		**
			50 47.0	676			1400	1400	31	31	36	J 36		3.05	7.2		3.6	ND 10.			12.5		g	22		11
	7/23/2012		55 54.0	899			1100	1100	42	42	50	J 50		3.45	8.4		4.2	ND 1		8 U	14		10.5	25		12.5
			60 57.5	982			1500	1500	72	72	85	J 85		3.3	7.8		3.9	ND 11.			13.5		10	23		11.5
		Prelim. Bo	rehole Average Analyti			2089		2471		115		138	8	3			6	1	0		12	2	9			10
			5 3.5	0	5.8	5.8	6.3	J 6.3	ND	0.2505	0.56	U 0.28	8 ND	0.4	0.87	7 U	0.435	ND 0.1	8 0.	.4 U	0.2	ND	0.7	1.5	U	0.75
			10 9.9	1,556				1000	460	460	540	540				3 U	4	ND 11.			13.5			24		12
	7/23/2012		15 12.0	3,408			8300	8300	2600	2600	3000	3000			7.7		3.85	58 5			13			23		11.5
			20 16.0	312,000			960000	960000	ND 250	1300	2900	U 1450			2200		1100	ND 350			3800			6700		3350
			25 20.1	2,415			3300	3300	250	250	280	280			7.8	_	3.8	ND 1			13.5			23		11.5
001-310			30 29.5 35 31.5	41,290 8,271	380000		440000 24000	440000 24000	ND 810	200 810	460 960	U 230			360	+ +	180	ND 50 ND 45.			600 55		460 40	1100 94		550 47
001-310			40 37.0	29,230			28000	28000	1300	1300	1500	J 1500			81	-	40.5	ND 43.			140		100	240		120
			45 44.5	28,180			40000	40000	1500	1500	1800	1800			42	+	21	ND 6			70		55	130		65
	7/24/2012		50 47.5	21,170	37000	37000	45000	45000	1300	1300	1600	1600	0 ND	17	41	1 U	20.5	ND 5	5 14	.0 U	70) ND	50	120	U	60
			55 50.1	24,140	37000	37000	44000	44000	1500	1500	1800	1800	0 ND		40) U	20	ND 5	5 14	·0 U	70		50	120	U	60
			60 55.1	36,120			2800	2800	ND	4.85	11	U 5.5			8.6	5 U	4.3	ND 1		.9 U	24.5			26	U	13
		Prelim. Bo	rehole Average Analyti	cal Value (0-60')		119437		133034		935		1097		111			118	36			406		322			358
			5 4.0	0	19		22	22	ND	0.25	0.59	U 0.295			0.92		0.455	ND 0.1			0.21		0.7	1.6		0.8
			10 7.5 15 12.5	0	28	28	34 19	34	4.9	11 4.9	14 5.9	J 5.9			0.92	2 0	0.455 0.455	ND 0.17 ND 0.17			0.21 0.21		0.65 0.65	1.6 1.6		0.8
	7/24/2012		5D ³ 17.0	0	14) 10	17	13	4.9	4.9	5.7	J 3.3	ND ND		0.92	2 11	0.433	ND 0.17	0.4		0.21	ND ND	0.03	1.6		0.8
		1	20 17.0	28,100		2.6	2.9	J 2.9		0.6	0.67	J 0.67			0.92	1 11	0.5	ND 0.21			0.24		0.8	1.8		0.9
			25 22.5	2,402			4100	4100	1700	1700	1900	1900		3.3	7.5	5 U	3.75	ND 1	_		13		10	22		11
004 200			30 25.1	161			3800	3800	1700	1700	1700	1700		3.35	6.7	7 U	3.35	ND 11.			11.5		10	20		10
001-309			35 31.5	2,407	3700	3700	3700	3700	1300	1300	1300	1300	0 ND	3.25	6.5	5 U	3.25	ND 1	1 2	2 U	11	ND	10	20	U	10
			40 35.1	1,452	2600	2600	2600	2600	820	820	820	820	0 ND	3.05	6.1	1 U	3.5	ND 10.	5 2	1 U	10.5	ND ND	9	18	U	9
	7/25/2012		45 40.5	6,070			2100	2100	950	950	950	950		3.15	6.3	3 U	3.15	ND 10.			10.5		9.5	19		9.5
	7,23,2012		50 45.5	1,670			2500	2500	860	860	860	860		3.15	6.3	3 U	3.15	ND 1			11		9.5	19	-	9.5
			55 52.5	1,838			2500	2500	440	440	440	440		3.3	6.6	5 U	3.3	ND 1			11	. ND	10	20		10
		Drelim Ro	60 59.5 rehole Average Analyti	4,340		2000 1905	2000	2000 1948	670	670 705	670	722		3.4	6.8	8 0	3.4	ND 11.	5 2	.3 0	11.5	ND	70	20	U	10
		T Tellini. Do	5 3.5	0	ND		0.4	U 0.2	ND	0.275	0.61	U 0.305		0.43	0.96	5 U	0.48	ND 0.19	5 0.4	.4 U	0.22	. ND	0.75	1.6	U	0.8
			10 9.5	292			0.61	J 0.61		30	35	35		0.38	0.89		0.445	3.2 3.			3.8		0.65	1.5		0.75
			15 14.9	9,209	1900	1900	2300	2300	360	360	440	440	0 ND	3.7	8.9	9 U	4.45	ND 12.	5 3	0 U,*	15	ND ND	11	27	U	13.5
		2	0 10 15.1	1,508	2300	2300	780	780	350	350	190	J 190	0 ND	0.41	0.92	2 U	0.46	9.4 9.	4 1	.1	11	2.7	2.7	3	J	3
			25 21.0	473			4.2	J 4.2		3	3.5	J 3.5			0.84		0.42	ND 0.1			0.19			1.4		0.7
			30 26.5	0	62		64	64	53	53	58	58			1.1	+	0.55	3.7 3.			4.7			1.9		0.95
001-304	7/26/2012		35 30.5	527			130	130		44	110	110			1.1		0.55	2.3 2.			7.4			1.9		0.95
		3.	5D ³ 30.5	527			60	246	47	110	55		ND		0.84		2.0	2.3	2.		42.5	ND		1.4		
			40 36.5 45 42.5	22	210 ND		240 15	U 7.5		110 3.95	9.3 9.1	U 4.65			7.2		3.6 3.55	ND 1 ND 10.		5 U,* 4 U,*	12.5 12		9.5	22 21		10.5
			50 46.5	611			240	240	170	170	190	J 190			8.7	7 11	4.35	ND 13.		0 U,*	15		12	26		10.3
			55 50.1	1,250			770	770	280	280	320	320			7.8	B U	3.9	ND 11.		6 U,*	13		10	23		11.5
			60 55.1	246			820	820	260	260	310	310		3.7	8.9	e u	4.45	ND 12.		0 U,*	15		11	26	U	13
		Prelim. Bo	rehole Average Analyt	cal Value (0-60')		571		446		139		138	8	2			2		8		9)	6			7
			5 3.5	0	ND		0.45	U 0.225	1	0.31	0.7	U 0.35					0.55				0.25			1.9		0.95
			10 9.5	0	ND		0.39	U 0.195		0.25	0.6	U 0.3			0.93		0.465	ND 0.1			0.215			1.6	-	0.8
			15 12.5	0	0.78		0.94	U 0.47	ND 0.70	0.255	0.61	U 0.305			0.96		0.49	ND 0.18			0.22			1.6		0.8
			20 17.0 25 21.5	0	5.6 ND		6.2	J 6.2 U 0.205	0.79	0.79	0.88	J 0.88			0.89		0.445	ND 0.18 ND 0.4	_		0.205 0.225			1.5 1.7	-	0.75 0.85
			25 21.5 30 26.5	0	9.4		0.41	0 0.205	ND 1.8	0.29 1.8	0.63 2.1	U 0.315			0.98		0.49	ND 0.4 ND 0.16			0.225			1.7		0.85
001-312	7/26/2012		35 31.5	0	67		80	80	1.8	1.0	15	15			0.91		0.455	ND 0.17	_		0.205		3.7	4.4	-	4.4
	, .,		40 39.0	0	80		95	95	14	14	16	16			0.94		0.47	ND 0.1			0.215		4.7	5.6		5.6
			45 43.0	0	32	32	38	38	6.4	6.4	7.6	J 7.6	6 ND		0.98		0.49	ND 0.1			0.225		1.9	2.3	J	2.3
			50 49.9	0	4.5		5.3	J 5.3		1	1.2	J 1.2			0.84		0.42	ND 0.16			0.19			1.4		0.7
			55 54.5	0	58		69	69		11	13	13			0.87		0.435	ND 0.1			0.2		3.2	3.8	-	3.8
		Duniling D	60 55.5	0	56		65	65	10	10	12	12	2 ND	0.38	0.89	∌ U	0.445	ND 0.17	5 0.4	1 U	0.205	2.7	2.7	3.1	J	3.1
<u> </u>		Prelim. Bo	rehole Average Analyti	car value (0-60')		26		31		5		(D	0			0		U		0	7	2			2

	Date of	Depth		PID		T(CE (μg/Kg)		Di		nd Preliminary Soil	Analytical Dat	a (SWMU 1,		Landfarm)	Kg)			VC (μg/Kg)				1.1	DCE (µg/Kg)		
Boring ID	Dute of	эсри.													-/ (F-6/											
BOTTING ID	(collection)	bgs	Actual Sample Depth bgs (ft)	(ppb)	Preliminary Reported	Preliminary Average ^{1,2}	Draft Final Reported Qu	Draft Final Average		Preliminary Average ^{1,2}	Draft Final Reported Qual	Draft Final 8 Average	Reported	Preliminary Average ^{1,2}	Draft Final Reported	Qual ⁸	Draft Final Average ⁹	Reported Average ¹	Draft Final Reported		Draft Final Average ⁹	Reported	Preliminary Average ^{1,2}	Draft Final Reported		raft Final verage ⁹
	1	Oil Landf	farm UCRS Soil Cleanup	Level (µg/Kg)			73				600	T			1080				34					130		
			5 4.0 10 7.5	0	ND ND		0.42 0.42	U 0.21		0.3 0.265	0.65 U	U 0.325 U 0.32		0.47 0.415	1	1 U	0.5 0.5	ND 0.2 ND 0.			0.23 0.23		0.8	1.7 1.7		0.8
			15 14.5	0	1.9		2.2	J 2.2		0.255	0.56	U 0.28		0.385	0.87	7 U	0.435	ND 0.1			0.23		0.65	1.7		0.75
			20 16.5	0	11	. 11	12	12	0.66	0.66	0.74	J 0.74	-	0.35	0.78	8 U	0.39	ND 0.			0.18	ND	0.6	1.3	U	0.65
		20		0	11		12	5000	0.69	250	0.87	J	ND	2.4	0.81		4.45		0.3			U	10	1.4		40.
			25 23.0 30 25.1	92 1,978	4100 3400	4100 3400	5000 4100	5000 4100	260 220	260 220	310 260	310 260		3.4 0.325	8.3 7.9		4.15 3.95	ND 1:	5 28 11 2		14 13.5		10 10	25 23		12.5 11.5
001-315	7/27/2012		35 33.5	15,018	3500	3500	4300	4300	300	300	370	370) ND	3.5	8.5		4.25	ND	12 29		14.5	ND	10.5	25		12.5
			40 35.5 45 40.1	9,630 15,100	2100 4200	2100	2400	2400	200	200 370	230 440	230		3.15 3.45	7.3		0.365	ND 10			12.5		9.5 10.5	22 25		12
			50 45.1	4,920	4000	4200	5100 4900	5100 4900	370 360	360	440	440		3.45	8.3 8.3		4.15 4.15	ND 1:			14 14		10.5	25		12.5 12.5
			55 50.1	10,700	2800		3200	3200	250	250	290	290		4.05	9.4		4.95	ND 13			16		12	28		14
			60 59.5 65 62.5	4,708 3,487	400 2500		4600 2900	460 2900	ND 120	4.8 120	11 1	U 5.5 J 130		3.75 4.05	8.5 9.2		4.2 4.6	ND 17	1.5 29 14 31		14.5 15.5		11 12	25 28		12.5
			ehole Average Analytic		2500	2078	2900	2490		160	130	191		4.05	9.2	2 0	4.0	ND	8	1 0	10.5		8	28	U	14
			5 3.0	0	ND	0.195	0.36	U 0.18	ND	0.3	0.56	U 0.28		0.47	0.87		0.435	ND 0.2			0.2		0.8	1.5		0.7
			10 9.0 15 13.0	0	ND ND	0.195	0.41	U 0.205	ND ND	0.3	0.63 U	U 0.315 U 0.275	1	0.47 0.47	0.99		0.495 0.43	ND 0.2 ND 0.4			0.225 0.195	ND ND	0.8	1.7 1.5		0.85
			20 19.0	0	ND ND	0.195	0.34	U 0.18	ND ND	0.3	0.53	U 0.275		0.47	0.82		0.43	ND 0.4	_		0.195	ND ND	0.8	1.5		0.73
		20	D ³ 19.0	0	ND)	0.34	U	ND		0.52	U	ND		0.81			ND	0.3	7 U		ND		1.4	U	
			25 20.5	553	0.55		0.33	U 0.165	-	0.66	0.51	U 0.255		0.47	0.0		0.4	ND 0.2			0.185		0.8	1.4		0.7
001-318	7/30/2012		30 29.0 35 34.0	24	110 170	110	65 200	J 200	67 160	67 160	47 190	J 190		0.47 3.4	0.86		0.43 4.1	ND 0.2			0.195 14		3.3 10	2.4		2.4
		41	0 ⁵ 35.5	58	170	170	190	J 190	160	160	190	J 190) ND	3.4	8.4	4 U	4.2	ND 1	5 29	9 U	1.45	ND	10	25	U	12.5
			45 41.0	4	110	110	61	61	64	64	44	44		0.47	1	1 U	0.5	0.94 0.			0.23		5.5	3.5		3.5
			50 46.0 55 50.5	16	29 7.4	29	19 6.4	J 6.4	8.2 1.8	8.2 1.8	5.9 1.6	J 5.9 J 1.6		0.47 0.47	0.95		0.475 0.41	ND 0.2 ND 0.2			0.215 0.185	2.3 ND	2.3 0.8	1.9 1.4		1.9
			60 56.5	0	24	24	22	22	24	24	22	22	ND	0.47	0.89		0.445	ND 0.2			0.205	ND	0.8	1.5		0.75
		Prelim. Bor	ehole Average Analytic	al Value (0-60')	AID.	52	0.41	47		41	0.63	42		1	0.00	0 11	1	ND 0.3	2	5 11	0.225	ND.	3	4.7		0.01
			5 3.7 10 8.5	0	ND 4.5	0.195	0.41 4.6	U 0.205	ND 2.3	0.3 2.3	0.63 U	U 0.315 J 2.3	1	0.47 0.47	0.99		0.495 0.47	ND 0.2 ND 0.2			0.225 0.215	ND ND	0.8	1.7 1.6		0.85
			15 12.0	0	7.9	7.9	7.8	J 7.8	6.2	6.2	6.1	J 6.1	ND	0.47	0.93	3 U	0.465	ND 0.2	15 0.43	3 U	0.215	ND	0.8	1.6		0.8
			20 15.5 25 21.0	0 2,176	9	9	7.9 6.6	J 7.9	11 27	11 27	9.7 17	9.7		0.47 0.47	0.83		0.415 0.465	ND 0.2 ND 0.2			0.19 0.21		0.8	1.4 1.6		0.7
			30 29.9	506	190	190	240	J 240	350	350	420	420		0.47	8.2		4.1		10 28		14		3.4	24		12
001-317	7/30/2012		35 30.5	895	140		230	J 230	250	250	440	440		0.47	8	8 U	4	7	7 2		13.5		2.7	24		17
			40 38.5 45 40.5	2,607 450	3.5 92	3.5	3.4 150	J 3.4	2.4 100	2.4 100	2.3 180	J 2.3		0.47 0.47	0.91		0.455 0.495	ND 0.2 ND 0.2			0.21 0.225	2.7 4.3	2.7 4.3	1.6 8.2		0.8
			50 47.0	4,926	87	87	93	93	37	37	40	40	+	0.47	1	1 U	0.5	ND 0.2			0.23	5.1	5.1	5.5	J	5.
			55 50.1	328	ND	0.195	0.36	U 0.18	ND	0.3	0.55	U 0.275	1	0.47 0.47	0.86	6 U	0.43	ND 0.2			0.2	ND	0.8	1.5		0.75
		Prelim. Bor	60 56.0 ehole Average Analytic	al Value (0-60')	29	29	28	28 64	8.1	8.1 66	7.8	J 7.8		0.47	0.9	9 0	0.45	ND 0.2	15 0.4: 2	1 0	0.205	ND	0.8	1.5	U	0.7
			5 4.9	1,196	ND	0.165	0.33	U 0.165	ND	0.255	0.51	U 0.255	S ND	0.4	0.8	8 U	0.4	ND 0.1	85 0.3	7 U	0.185	ND	0.7	1.4		0.7
			10 6.0	4,003	ND		0.33	U 0.165		0.25	0.5	U 0.25		0.395	0.79		0.395	ND 0.			0.18		0.65	1.3		0.6
		10	D ³ 6.0 15 10.1	4,003 6,571	ND ND		0.38	U 0.165	ND	0.255	0.58 U	U 0.255	ND 5	0.4	0.91		0.4	ND 0.	0.42		0.185	ND	0.7	1.6 1.4		0.7
			20 17.0	0	ND		0.31	U 0.155		4.8	4.8	J 4.8		0.37	0.74	4 U	0.37	1.3			1.3		0.65	1.3	U	0.6
			25 23.0 30 29.9	9,091 6,875	320 2400		320 2400	320 2400	430 1200	430 1200	430 1200	430 1200		3.85 3.3	7.7	+	0.385	ND 1:	13 20		13 11.5		11.5 10	23 20		11.
001-316	7/31/2012		35 31.5	4,443	2900		2900	2900	1300	1300	1300	1300	1	3.5	0.0	7 U	3.5		12 24		11.5		10.5	21		10.5
			40 35.5	8,915	1500	1500	1500	1500	410	410	410	410		3.3	6.6		3.3		11 22		11		10	20		10
			45 41.0 50 46.5	2,242 14	12 52		12 52	12 52	3.6 7.7	3.6 7.7	3.6 7.7	J 3.6 J 7.7		0.41 0.415	0.82		0.41 0.415	ND 0.1 ND 0.			0.185 0.19		0.7 2.1	1.4 2.1		2.1
			55 54.0	0	6	6	6	J 6	0.59	0.59	0.59	J 0.59		0.39	0.78		0.39	ND 0.	18 0.30		0.18	ND	0.65	1.3		0.6
			60 57.0	0 (0.00)	14	14 600	14	14 600		1.4	1.4	J 1.4		0.415	0.83	3 U	0.415	ND 0.	19 0.38	8 U	0.19	ND	0.7	1.4	U	0.
		rieiiii. Bor	ehole Average Analytic 5 3.0	.ai vaiue (0-60°)	ND		0.35	U 0.175		280 0.27	0.54	U 0.27		0.42	0.84	4 U	0.42	ND 0.	19 0.38	8 U	0.19	ND	0.7	1.4	U	0.1
			10 7.0	0	1.3	1.3	1.3	J 1.3	ND	0.265	0.53	J 0.265	ND.	0.41	0.82	2 U	0.41	ND 0.	19 0.38	8 U	0.19	ND	0.7	1.4	U	0.
			15 14.0 20 19.0	0	1.8 ND		0.36	J 1.8		0.245 0.275	0.49 U	U 0.245 U 0.275	1	0.38 0.435	0.76		0.38 0.435	ND 0.1	75 0.35		0.175 0.2		0.65 0.75	1.3 1.5		0.65
			25 21.5	0	13		13	13		8.4	8.4	8.4	1	0.435	0.87		0.435	ND 0.			0.2		0.75	1.3		0.6
			30 28.5	5,709	ND	0.75	200	J 200	81	81	110	J 110	ND ND	3.55	8.3	3 U	4.15	ND	12 28	8 U	14	ND	10.5	25	U	12.
001-314	7/31/2012		35 32.0 40 36.5	695 511	220 240		220 270	220 270		120 4.3	9.7 U	J 120 U 4.85	1	3.2 3.35	6.4 7.6		3.2	ND 1:	.5 20		11 13		9.5 10	19 23		9. 11.
			45 44.0	883	790	790	950	950	540	540	640	640		3.45	8.2		4.1	ND 1			14		10	24		11.
			50 49.0	732	850		1000	1000		570	700	700		3.5	8.4		4.2		12 29		14.5		10.5	25		12.
			55 50.1 60 57.5	2,451 1,846	440 180		510 210	J 210	230 ND	230 4.4	270 10	270 U 5	ND ND	3.35 3.4	7.8 7.9		0.39 3.95	ND 1:			13.5 13.5		10 10	23 24		11.5
			65 60.5	137	350	350	410	410	170	170	200	J 200) ND	3.45	8	8 U	4	ND 1:			13.5		10.5	24		12
		Prelim. Bor	ehole Average Analytic	al Value (0-60')		237		291		133		158	}	2			2		7		8		6			

Table 1. Southwest Plume RDSI Characterization Data (Continued)

	D-tf	Danah		DID		TCE (··	- (v-)		DF		d Preliminary Soil	Analytical Dat	a (SWMU 1,						VC (1.1	DCE (/V-)	
	Date of	Depth		PID		TCE (µ	g/Kg)			CIS-1,	2-DCE (µg/Kg)			trans -1,	2-DCE (μg/Kg)				VC (μg/Kg)			1,1	DCE (μg/Kg)	
Boring ID			Actual Sample		,		aft Final	Draft Final		Preliminary	Draft Final	Draft Final			Draft Final	Draft Final		Preliminary	Draft Final	Draft Final		Preliminary	Draft Final	Draft Final
(c	collection)	bgs	Depth bgs (ft)	(ppb)	Reported A	, i		ual ⁸ Average ⁹ Rep	ported A	Average ^{1,2}	Reported Qual	Average ⁹	Reported	-	Reported Qual	8 Average ⁹	Reported	Average ^{1,2}		Qual ⁸ Average ⁹	Reported	Average ^{1,2}	Reported Qu	ıal ⁸ Average ⁹
		Oil Landfari	m UCRS Soil Cleanup 4.5	p Level (μg/Kg)	ND	0.155	0.36	U 0.18	ND	0.24	0.56	0.28	ND	0.375	0.87 U	U 0.435	ND	0.17	34 0.4	U 0.2	2 ND	0.65	1.5	U 0.75
		10	8.0	0	ND	0.16	0.39	U 0.195	ND	0.245	0.6	J 0.3		0.385	0.94	U 0.433	ND	0.175	0.43	U 0.215		l	1.6	U 0.75
		10D ³	8.0	0	ND		0.42	U	ND		0.64	J	ND		1 (U	ND		0.46	U	ND		1.7	U
		15	12.5	0	ND	0.17	0.41	U 0.205	ND	0.26	0.63	0.315		0.41	0.98 l	U 0.49	ND	0.19	0.45	U 0.225			1.7	U 0.85
		20 25	18.0 23.5	0	ND ND	0.16 0.16	0.37	U 0.185 U 0.17	ND ND	0.25 0.24	0.57	U 0.285 U 0.265		0.39	0.9 U 0.83 U	U 0.45 U 0.415	ND ND	0.18 0.175	0.41	U 0.205		l	1.5 1.4	U 0.75
001-307	8/1/2012	30	26.0	0	0.98	0.98	1.2	J 1.2	1.8	1.8	2.1	J 2.1	1	0.395	0.93 U	U 0.465	ND	0.18	0.43	U 0.215		l	2.7	J 2.7
001-307	6/1/2012	35	33.0	0	0.83	0.83	0.97	J 0.97	1.4	1.4	1.7	J 1.7		0.395	0.93 l	U 0.465	ND	0.18	0.43	U 0.215		-	2.3	J 2.3
		40	37.0 43.0	0	ND 7.2	0.175 7.2	0.4 8.4	U 0.2 J 8.4	ND 3	0.275	0.61 3.5	J 0.305 J 3.5	1	0.435 0.37	0.95 U	U 0.475 U 0.43	ND ND	0.195 0.17	0.44	U 0.22		0.75 2.1	1.6 2.4	U 0.8
		50	48.5	0	5.8	5.8	6.9	J 6.9	4.2	4.2	4.9	J 4.9		0.39	0.91 l	U 0.455	ND	0.175	0.42	U 0.21		2.7	3.2	J 3.2
		55	52.5	0	7.1	7.1	8.3	J 8.3	4.4	4.4	5.1	J 5.1		0.38	0.89 l	U 0.445	ND	0.175	0.41	U 0.205			4.1	J 4.1
		Prelim Boreh	57.5 ole Average Analytic	0 ('na-() aule/	7.2	7.2	8.5	J 8.5	4.1	4.1	4.8	J 2.4	ND ND	0.385	0.91 U	U 0.455	ND	0.175	0.42	U 0.21	2.9	2.9	3.4	J 1.7
		5	4.9	0-00	ND	0.165	0.41	U 0.205	ND	0.155	0.62	J 0.31	ND	0.4	0.98 l	U 0.49	ND	0.185	0.45	U 0.225	ND	0.7	1.7	U 0.85
		10	9.0	0	2.3	2.3	2.7	J 2.7	ND	0.26	0.63	0.315	ND	0.41	0.99 ا	U 0.495	ND	0.185	0.45	U 0.225	ND.	0.7	1.7	U 0.85
	-	15 20	12.5 16.0	0	2.4 5.1	2.4 5.1	2.8 5.8	J 2.8 J 5.8	ND 1	0.24	0.56	J 0.28 J 1.2		0.38	0.87 U	U 0.435 U 0.39	ND ND	0.175 0.155	0.4	U 0.2			1.5 1.3	U 0.75 U 0.65
	-	20D ³	16.0	0	2.2	5.1	2.6	J 3.8	ND	1	0.58	J 1.2	ND ND	0.34	0.78 t	U 0.39	ND ND	0.135	0.36	U 0.19	ND ND		1.5	U
		25	23.5	0	38	38	45	45	15	15	18	18		0.34	0.93 l	U 0.465	ND	0.18		U 0.215	S ND	0.65	1.6	U 0.8
001-308	8/1/2012	30	29.5	659	270	270	310	310	66 ND	66	76	J 76		3.4	7.7	U 3.65	ND	11.5	26	U 13		l	23	U 11.5
	-	35 40	34.0 37.0	5,998 1,192	0.66 ND	0.66	0.74 0.44	J 0.74 U 0.22	ND ND	0.245	0.56	U 0.28 U 0.34		0.385 0.485	0.87 U	U 0.435 U 0.55	ND ND	0.175 0.22	0.4	U 0.245		l	1.5	U 0.75
		45	44.9	69	410	410	490	490	120	120	150	J 150		3.55	8.4 l	U 4.2	ND	12		U 14.5		l	25	U 12.5
		50	48.5	0	190	190	230	J 230	49	49	59	J 59		3.35	8.1 U	U 4.05	ND	11.5	-	U 14			24	U 12
		55 60	54.9 58.5	150 500		210 180	250 200	250 200	58 38	58 38	68 42	J 68 42		3.2 0.4	7.6 U	U 3.8 U 0.44	ND ND	0.18		U 13		l	23	U 11.5 J 2.4
			ole Average Analytic		100	109	200	128	30	29	.2	35		1	0.00	2	.,,	4	51.1	5	5	4	2.1.	5
		5	4.0	0	ND	0.165	0.4	U 0.2	ND	0.255	0.62	0.31		0.395	0.97 l	U 0.485	ND	0.18		U 0.22			1.7	U 0.85
	-	10	9.0 14.5	0	4.3	4.3 15	5.2 17	J 5.2	ND 6.5	0.25 6.5	0.59 7.5	J 0.295 J 7.5		0.39 0.365	0.92 U	U 0.46 U 0.42	ND ND	0.175 0.165	0.42 0.38	U 0.21		l	1.6 1.4	U 0.8
		20	19.5	0	0.38	0.38	0.43	J 0.43	ND	0.255	0.57	0.285		0.4	0.9 ا	U 0.45	ND	0.18	0.41	U 0.205			1.5	U 0.75
	-	25 30	21.0 27.5	0	ND 2.5	0.16 2.5	0.36	U 0.18	ND 1.3	0.295	0.55 1.6	J 0.275 J 1.6		0.385	0.87 U	U 0.435 U 0.465	ND ND	0.175 0.18	0.4	U 0.215		l	1.5 1.6	U 0.75
001-303	8/2/2012	35	34.5	12		0.36	0.41	J 0.41	0.93	0.93	1.1	J 1.1		0.33	0.96	U 0.403	ND	0.19	0.43	U 0.22		l	1.6	U 0.8
		40		281	290	290	340	340	180	180	210	J 210		3.45	8.2 l	U 4.1	ND	12		U 14			25	U 12.5
		45 50	43.5 49.5	2,016 530	290 430	290 430	340 510	340 510	190 240	190 240	220 280	J 220 280		3.45	8.1 l	U 4.05	ND ND	12 11.5		U 14		l	24 24	U 12
		55	50.1	5,530	25	25	29	29	20	20	23	23		0.405	0.93	U 0.465	ND	0.185	0.43	U 0.215		l	1.6	U 0.8
		60	58.5	8,551	680	680	19	U 9.5	320	320	11	J 5.5		0.395	8.6 l	U 4.3	13	13	29	U 14.5	6.6	6.6	26	U 13
		Prelim. Boreh	ole Average Analytic 4.5	cal Value (0-60')	2.9	145 2.9	3.6	J 3.6	ND	0.265	0.65	0.325		0.425	1 1	U 0.5	ND	0.19	0.46	U 0.23	S ND	0.7	1.7	U 0.755
		10	8.5	0	29	29	35	35	ND	0.24	0.57	J 0.285		0.375	0.89	U 0.445	ND	0.175	0.41	U 0.205			1.5	U 0.75
		15	14.0	0	45	45	54	54	2	2	2.4	J 2.4		0.365	0.91 l	U 0.455	ND	0.175	0.42	U 0.21			1.6	U 0.8
		20 25	18.5 24.5	0	13 530	13 530	14 640	14 640	5.6 ND	5.6 4.45	6.2	J 6.2 J 5.5		0.365 3.45	0.81 U	U 0.405 U 4.2	ND ND	0.165 12		U 0.185		l	1.4 25	U 0.7 U 12.5
		30		246		130	160	J 160	ND	4.43	11	J 5.5		3.43	8.6 U	U 4.3	ND	12		U 14.5		l	26	U 13
001-305	8/2/2012	35		1,826	330	30	380	380	ND	4.2	9.8	4.9		3.3	7.6 U	U 3.8	ND	11		U 13	+		23	U 11.5
	-	40 45	39.9 43.5	870 2,344		1500 390	1800 470	1800 470	ND ND	4.15 4.3	9.7	J 4.85	ND ND	3.25 3.35	7.6 U 8.1 U	U 3.8 U 4.05	ND ND	11 11.5		U 13.5			23	U 11.5
	-	50	45.5	28,514	3.5	3.5	4.1	J 4.1	ND	0.25	0.6	0.3		0.395	0.94	U 0.47	ND	0.18	0.43	U 0.215		l	1.6	3.0 U
		55	53.0	2,330		11	13	13	ND	0.26	0.61	0.305		0.41	0.95 L	U 475	ND	0.19	0.44	U 0.22			1.6	U 0.8
	-	Prelim. Boreh	55.1 ole Average Analytic	224 cal Value (0-60')	160	160 237	190	190 314	3.5	3.5	4.1	J 2.05	ND	0.41	0.98 l	U 0.49 41	ND	0.19	0.45	U 0.225	ND	0.7	1.7	U 0.85
		5	3.5	0	ND	0.155	0.37	U 0.185	ND	0.24	0.56	0.28		0.375	0.88 U		ND	0.17		U 0.2	2 ND	0.65	1.5	U 0.75
		5D ³	3.5	0	ND	0.165	0.39	U	ND	6.5-	0.6)	ND	0.00	0.94	U	ND		0.43	U	ND		1.6	U
	-	10 15	8.0 13.5	0	ND ND	0.165 0.155	0.4	U 0.2 U 0.185	ND ND	0.25 0.24	0.62	U 0.31 U 0.285		0.39 0.375	0.96 U	U 0.48 U 0.445	ND ND	0.18 0.17		U 0.22			1.7 1.5	U 0.85 U 0.75
	<u> </u>	20	17.0	0	ND	0.16	0.35	U 0.175	ND	0.245	0.55	J 0.275		0.38	0.85 U	U 0.425	ND	0.175		U 0.195			1.5	U 0.75
		25	22.0	45	1.1	1.1	1.2	J 1.2	ND	0.23	0.5	0.25		0.355	0.79 U	U 0.395	ND	0.165	0.36	U 0.18		l	1.3	U 0.65
001-306	8/3/2012	30 35	25.1 32.0	1	30 27	30 27	36 32	36	1.5	1.5 1.5	1.8	J 1.8 J 0.85		0.38 0.405	0.91 l 0.96 l	U 0.455 U 0.48	ND ND	0.175 0.185	0.42 0.44	U 0.21			1.6 1.6	U 0.8
	F	40	39.0	50	58	58	67	67	3.8	3.8	4.4	J 2.2	1	0.385	0.88 U	U 0.44	ND	0.175	0.4	U 0.2			1.5	U 0.75
		45	40.5	0	75	75	86	86	5.1	5.1	5.9	J 2.95		0.365	0.84 U	U 0.42	ND	0.165	0.38	U 0.19		l	1.4	U 0.7
	-	50 55	49.5 53.0	0 1,215	64 37	64 37	74 43	J 74	ND 3.1	4.35 3.1	3.6	J 5 J 1.8	ND ND	0.385	7.9 l 0.89 l	U 3.95 U 0.445	ND ND	11.5 0.175	27 0.41	U 13.5			23 1.5	U 11.5 U 0.75
	<u> </u>	60	56.0	39	110	110	130	130	7.9	7.9	9.4	J 4.7		0.39	0.93 U	U 0.465	ND	0.18		U 0.215		l	1.6	8.0 U
		Prelim Boreh	ole Average Analytic	cal Value (0-60')		34		39		2		2		1		1		1		1	L	1		7

	Date of	Depth		PID		TCF	(μg/Kg)			nd Preliminar , <mark>2-DCE (μg/Kg</mark>		Analytical Data	(SWMU 1	trans -1.	andfarm)			\	VC (μg/Kg)		11	DCE (μg/Kg)	
Boring ID	Bate o.	Dept		5	D			Draft Final	Preliminary			Draft Final				Draft I	inal			Draft Final	Preliminary		Draft Final
	(collection)	bgs	Actual Sample Depth bgs (ft)	(ppb)		Average ^{1,2}		Qual ⁸ Average ⁹ Reported	1.2	Draft Final Reported	Qual ⁸	Average ⁹	Reported	1.2	Draft Final Reported Qua	0	0	Preliminary Average ^{1,2}	Draft Final Reported Qual ⁸	Average ⁹ Reported	Average ^{1,2}	Draft Final Reported Qual ⁸	Average ⁹
	ı	Oil Landfa	rm UCRS Soil Clea 3.5	nup Level (μg/Kg) 227	21	21	73	24 ND	0.28	600 0.61	U	0.305	ND	0.44	0.96	U	0.48 N	0.2	34 0.44 U	J 0.22 NE	0.75	130 1.6 U	0.8
		10	7.5	599	83	83	100	100 1.4	1.4	1.8	J	1.8	ND	0.385	0.94	U	0.47 N	0.175	0.43 L	J 0.215 NE	0.65	1.6 U	0.8
	-	15 20	-	1,419 22,230	46 150	46 150	55 170	55 3.1 170 7.3		3.7 8.1		3.7 8.1	ND ND	0.385 0.38	0.92 0.85	U	0.46 N 0.425 N		0.42 U 0.39 U	J 0.21 NE J 0.195 NE		1.6 U 1.4 U	0.817
	-	25 25D		54,270 54,270	ND 120	7	15	U 7.5 ND		9.1	U	4.55	ND ND	3.3	7.1	U	3.55 N		24 L	J 12 NE		21 U	21
		30		31,310	12000	12000	14000	14000 950		1100		1100	ND	6.5	16	U	16 N		53 L	J 53 NE		46 U	23
001-313	8/6/2012	35		58,714 70,550	15000 12000	15000 12000	18000 14000	18000 1000 14000 770		1200 900		1200 900	ND ND	17	41 16	U	20.5 N	+ +	140 U	J 70 NE J 27 NE		120 U 48 U	60
		45	5 40.1	17,730	900	900	1100	1100 ND	4.3	10		5	ND	3.35	8	U	4 N	11.5	27 L	J 13.5 NE	10	24 U	12
	-	50		5,745 4,187	220 ND	220 7.5	260 17	260 ND U 8.5 ND		9.9 9.8		4.95 4.9	ND nd	3.3 3.35	7.8 7.6	U	3.9 N 3.8 n	+	26 L 26 L	J 13 NE		23 U 23 U	11.5
		60 62.5		2,749 2796	12 640	12 640	14 760	14 ND 760 ND		0.6 10		0.3	ND ND	0.405	0.93 7.9	U	0.465 N 3.95 N		0.43 L 27 L	J 0.215 NE J 13.5 NE		1.6 U 23 U	0.8
			hole Average Anal		040	3161	760	3731	212	10	U	249	ND	4	7.9	U	5.95	13		17	11	25 0	14
	-	10	5 4.5	0	ND ND	0.18 0.165	0.4	U 0.2 U 0.2 ND	0.255	0.62	U	0.31 0.305	ND	0.405	0.97 0.96	U	0.495 0.49 N	0.185	0.44 U	J 0.22 J 0.22 NE	0.7	1.7 U 1.6 U	0.85
	-	15		0	0.98	0.98	1.2	J 1.2 ND	0.26	0.62	U	0.31	ND	0.41	0.98	U	0.49 N	0.185	0.45 L	J 0.225 NE	0.7	1.7 U	0.8
	0/6/2012	20		0	2.3	2.3	48 2.7	48 7.9 J 2.7 ND		0.56	U	0.28	ND ND	0.405 0.345	0.93 0.87		0.465 N 0.435 N		0.43 U	J 0.215 NE J 0.2 NE		1.6 U 1.5 U	0.8
	8/6/2012	30D		0	1.7 1.6	1.7	2	J 2 ND		0.62	U	0.31	ND ND	0.41	0.98	U	0.49 N		0.45 L	J 0.225 NE		1.7 U	0.85
001-319 ⁴	-	35		0	2.3	2.3	2.7	J 2.7 ND	0.23	0.54	U	0.27	ND	0.365	0.85	U	0.425 N		0.39 L	J 0.195 NE		1.5 U	0.75
	-	40		0	45 3.2	45 3.2	55 3.9	55 1.5 J 3.9 ND		1.5 0.56		0.75 0.28	ND	0.365	0.88	U	0.65 0.44 N	0.165	0.58 L 0.4 L	J 0.29 J 0.2 NE	0.6	2.2 U 1.5 U	0.75
		50 55		115	21	21	24 130	24 0.92		1.1	J	1.1	ND ND	0.365 0.415	0.85	U	0.425 N 0.47 N		0.39 L	J 0.195 NE J 0.215 NE		1.5 U	0.75
	8/7/2012	60		1,712 1,373	9.2	9.2	10	130 7.9 10 0.83		0.92	J	0.92	ND	0.415	0.94 0.87	U	0.47 N 0.435 N		0.43 L 0.4 L	J 0.2 NE	0.65	1.6 U 1.5 U	0.75
	-	65 Prelim, Borel		593 ytical Value (0-60')	5.2	5.2 19	5.7	J 5.7	2	0.52	J	0.52		0	0.79	U	0.395	0	0.36 L	U 0.18 NE	0.6	1.3 U	0.69
		ŗ	5 4.0	0	ND	0.16	0.39	U 0.195 ND		0.59		0.295	ND	0.39	0.93	U	465 N			J 0.215 NE		1.6 U	0.8
	-	10		43 1,175	ND 160	0.155 160	0.37 180	U 0.185 ND 180 8.2		0.58 9.6		0.29 9.6	ND ND	0.37 0.365	0.9	U	0.45 N 0.445 N		0.41 U	J 0.205 NE J 0.205 NE		1.5 U	0.75
		20 25		1,074 198	5.9 110	5.9 110	7 130	J 7 ND	0.235	0.55 6.1		0.275 6.1	ND ND	0.365 0.4	0.86 0.97	U	0.43 N 0.485 N		0.39 U 0.44 U	J 0.195 NE J 0.22 NE		1.5 U 1.7 U	0.75
	-	30	28	5,007	610	610	720	720 42		49	J	49	ND	3.3	7.8	U	0.39 N	11.5	27 L	J 23.5 NE	10	23 U	11.
001-320 ⁴	8/7/2012	35		2,548 2,275	950 910	950 910	1100 1100	1100 70 1100 63		83 74		83 74	ND ND	3.35 3.45	7.9	U	3.95 N 4 N		27 L 27 L	J 13.5 NE J 13.5 NE		23 U 24 U	11.5
		45 50		3,601 448	1200 210	1200 210	1500 250	1500 91 250 16		110 19		110	ND ND	3.45 3.2	8.4 7.7	U	4.2 N 3.65 N		28 L 26 L	J 14 NE J 13 NE		25 U 23 U	12.
	-	55	5 52.0	507	400	400	480	480 27	27	32		19 32	ND	3.4	8	U	4 N	11.5	26 C	J 13.5 NE	10	24 U	11.3
	-	Prelim. Borel		937 ytical Value (0-60')	1.2	1.2 380	1.3	J 1.3 ND	0.3	0.69	U	0.385	ND	0.47	1.1	U	0.55 N	0.215	0.49 L	0.245 NE	0.8	1.8 U	0.9
		Į.	5 4.0	335		1.3	1.5	J 1.5 ND		0.57		0.285	ND	1	0.9	U	0.45 N			J 0.205 NE		1.5 U	0.75
	-	10	+	16 0	2.7	2.7	3.3	J 3.3 4.3 J 3.1 7	4.3 7	5.2 8.5		5.2 8.5	ND ND	0.375 0.355	0.92 0.86	U	0.46 N 0.43 N		0.42 U,* 0.39 U,*	* 0.21 NE * 0.195 NE		1.6 U 1.5 U	0.7
	-	20		107 23		0.165 0.155	0.36 0.34	U 0.18 ND U 0.17 ND	1	0.56 0.52		0.29 0.26	ND ND	0.395 0.375	0.87 0.82	U	0.445 N 0.41 N		0.4 L 0.37 L	J 0.2 NE J 0.185 NE		1.5 U 1.4 U	0.7
		25D	3 20.5	23	1.1			1.6					ND			-	N	O		NE)		=
001-3214	8/8/2012	30		3,315 312	28 8.4	28 8.4	35 9.5	35 68 9.5 17		83 19		83 19	ND	0.4	0.98	U	0.49 N 0.415	0.185 U 0.415	0.45 U,* 0.38 U,*	* 0.225 5.3 * 0.19	5.3	6.5 J 2.2 J	6.l 2.:
		40	38	136 113	ND 8.4	0.175 8.4	0.41	U 0.205 ND 10 13	0.27	0.63	U	0.315 15	ND ND	0.42	0.99 0.95	U	0.495 N 0.475 N	0.195	0.45 U,*	* 0.225 NE * 0.215 3.8		1.7 U 4.5 J	0.8
		50	0 49.5	0	8.4	8	9.3	J 9.3 15	15	15 18		18	ND	0.38	0.88	U	0.44 N	0.175	0.4 L	0.2 1.9	1.9	2.3 J	2.:
	-	55	5 54.0 0 59.0	0	15 14	15 14	18 17	18 27 17 21		32 26		32 26	ND ND	0.375 0.38	0.89 0.92	U	0.445 N 0.46 N		0.41 U	J 0.205 4.4 * 0.21 4.5		5.2 J 5 J	5.:
		Prelim. Borel		ytical Value (0-60')	2	7	0.20	9	14	0.61	-	17	ND	0			0	0		0	2	1.6	
	<u> </u>	10	5 4.0 0 9	63 0	ND ND	0.175 0.165	0.39 0.38	U 0.195 ND U 0.19 ND	t	0.61 0.59		0.305 0.295	ND ND	0.39	0.95 0.92	U	0.475 N 0.46 N	0.18	0.43 U,* 0.42 u,*	* 0.215 NE * 0.21 NE	0.65	1.6 U 1.6 u	0.
		15 20		13 NA	ND	0.155	0.36	U 0.18 ND	0.24	0.56	U	0.28	ND	0.38	0.87	U	0.435 N	0.175	0.4 L	J 0.2 NE	0.65	1.5 U	0.7
		25	5 21.5	0	ND	0.17	0.4	U 0.2 ND		0.62		0.31	ND	0.41	0.97	U	0.485 N		0.45 U,*	* 0.225 NE		1.7 U	0.8
001-322 ⁴	8/8/2012	30		54 167	27 5.2	27 5.2	32 5.8	32 18 J 5.8 3.5		21 3.9		21 3.9	ND	0.405	0.96 0.91	U	0.48 0.455 N	0.48 0 0.185	1.4 . 0.42 U,*	J 1.4 NE * 0.21 NE		1.7 U 1.6 U	0.8
		40	35.1	261	3.9	3.9 86	4.5 100	J 4.5		2.3	J	2.3 50			0.87	U	0.435 N	0.175	0.4 U,*	* 0.2 NE * 0.195 NE	0.65	1.5 U	0.7
		50	0 48.5	51	69	69	80	80 40	40	46		46	ND ND	0.365 0.37	0.85 0.86	U	0.425 N 0.43 N	0.17	0.39 U,* 0.39 U	J 0.195 NE	0.65	1.5 U 1.5 U	0.7
		55	5 54.9 0 57.5	244 129	2.7	2.7	53 3.2	53 29 J 3.2 2.6	1	34		34 3.1	ND ND	0.36 0.44	0.85	U	0.425 Ni 1 Ni		0.39 L 0.47 L	U 0.195 NE U 0.235 NE		1.5 U 1.8 U	0.7
		Prelim. Borel	hole Average Anal	ytical Value (0-60')		22		25	14		,	15	-	0			1	0		0	1		

Table 1. Southwest Plume RDSI Characterization Data (Continued)

										DRAFT Final	and Preliminary Soil	Analytical Dat	a (SWMU 1	., C-747-C Oil	Landfarm)									
	Date of	Depth		PID		T	CE (μg/Kg)			cis	-1,2-DCE (μg/Kg)			trans -	1,2-DCE (μg/Kg)				VC (μg/Kg)			1,	1 DCE (μg/Kg)	
Boring ID	(collection)	bgs	Actual Sample Depth bgs (ft)	(ppb)	,	Preliminary Average ^{1,2}	Draft Final Reported		t Final	Preliminary rted Average ^{1,2}	Draft Final Reported Qual	Draft Final Average 9	Reported	Preliminary Average ^{1,2}	Draft Final Reported C	Draft	0	Preliminary d Average ^{1,2}	Draft Final Reported	Draft F	0	Preliminary Average ^{1,2}	Draft Final Reported Qual ⁸	Draft Final Average
		Oil Landfar	m UCRS Soil Clea	anup Level (µg/Kg)			73				600			<u> </u>	1080	<u> </u>			34			<u> </u>	130	
		5	4.0	0	ND	0.16	0.38	U	0.19	ND 0.24	0.59 U	J 0.295	ND	0.38	0.92	U	0.46 N	D 0.175	0.42	U	0.21 N	0.65	1.6 L	0.8
		10	5.1	1	ND	0.165	0.39	U	0.195	ND 0.25	0.6 U	J 0.3	ND	0.39	0.93	U	0.465 N	D 0.18	0.43	U).215 N	0.65	1.6 L	0.8
		15	10.1	10	ND	0.155	0.35	U	0.175	ND 0.23	0.54 U	J 0.27	ND ND	0.37	0.84	U	0.42 N	D 0.17	0.84	U	0.42 N	0.65	1.4 L	0.7
		15D ³	10.1	10	ND)				ND			ND				N	D			N	0		
		20	17	0	ND	0.185	0.41	U	0.205	ND 0.28	0.63 l	J 0.315	ND	0.445	0.99	U	0.495 N	D 0.205	0.45	U).225 N	0.75	1.7 L	0.85
		25	20.5	0	ND	0.165	0.4	U	0.2	ND 0.25	0.61 U	J 0.305	ND.	0.39	0.95	U	0.475 N	D 0.18	0.44	U	0.22 N	0.65	1.6 L	0.8
001-301	8/9/2012	30	25.1	71	6.9	6.9	7.9	J	7.9	4.3 4.3	4.9	J 4.9	ND	0.355	0.81	U	0.405 N	D 0.165	0.37	U).185 N		1.4 L	0.7
001 001	0,3,2012	35	31	92	15	15	17		17	12 17	2 13	13	ND ND	0.385	0.88	U	0.44 N	D 0.175	0.4	U	0.2 N			0.75
		40	35.5	33	25	25	28		28	17 1	7 20	20	ND ND	0.38	0.87	U	0.435 N	D 0.175	0.4	U	0.2 N		l	0.75
		45	44	189	0.	57	67		67	40 40	47	47	' ND	0.355	0.82	U	0.41 N	D 0.16	0.38	U	0.19 N		1.4 L	0.7
		50	45.1	328			96		96	58 58	67	67	110	0.36	0.83		0.415 N	D 0.165		U	0.19 N		1.4 L	0.7
		55	50.1	510		12	13		13	19 19	21	21	. ND	0.375	0.85	U	0.425 N	D 0.17	0.39	U	0.195 N		1.5 L	0.75
		60	57.5	448	27				30	19 19	21	21		0.65	1.4	U	0.7 N	D 0.295	0.66	U	0.33 N	1.1	2.5 L	1.25
		Prelim. Boren		lytical Value (0-60')	ND	19			22	14		16		0 405	0.07		0.405	0 105	0.44		0.22 N	1	47 1	1
		10	2.0	0	ND ND	0.17		U	0.2	ND 0.20		J 0.31 J 0.28	_	0.405 0.37	0.97 0.88	U	0.485 N 0.44 N	D 0.185 D 0.17	0.44	U	0.22 N 0.2 N			0.85 0.75
		10	3.3	45	ND ND	0.155	0.36	11	0.185	ND 0.23		J 0.28	_	0.37	0.88	11	0.44 N	D 0.17	0.4	11	0.2 N		1.5 U	0.75
		20	18	0	ND	0.155	0.37	11	0.175	ND 0.24		J 0.27	1	0.375	0.85	11	0.425 N	D 0.173	0.39	11	0.195 N		1.5 U	0.75
		25	24	0	22	22		-	26	0.2	15	15	_	0.575	0.91		0.455	0.17	1.8	Ĭ	1.8	0.03	2.2	2.2
		30	28.5	1,140	25	25	28		28	9.5 9.5	11	11	. ND	0.415	0.93		0.465 N	D 0.19	0.43	U	0.215 N	0.7	1.6 L	0.8
001-302	8/10/2012	35	31	414	280	280	310	J	310	72 73	2 82	J 82	. ND	6.5	15	U	7.5 N	D 22	50	U	25 N	19	43 L	21.5
		40	36.5	35	37	37	43		43	14 14	1 16	16	ND.	0.455	1.1	U	0.55 N	D 0.21	0.48	U	0.24 3.	5 3.5	4.1	4.1
		45 ⁷	NA	NA																				
		50	47.5	578	21	. 21	24		24	5.3 5.3	5.9	J 5.9	ND	0.435	0.97	U	0.485 N	D 0.2	0.44	U	0.22 N	0.75	1.7 U	0.85
		55	53.0	278	200	200	230	J	230	39 39	46	J 46	ND.	3.8	9	U	4.5 N	D 13	31	U	15.5 N	11.5	27 L	13.5
		57.5	55.5	493	150				180	27 2	7 32	32		0.45	1.1	U	0.55 N	D 0.205	0.49	U	0.245 2.	8 2.8	3.4	3.4
		Prelim. Boreh	ole Average Ana	lytical Value (0-60')		67			77	1	7	19)	1			1	4			4	4	,	4

Notos

- 1 For analytical results reported as non-detect (ND), a value equal to one half of the method detection levels (MDLs) was used to calculate the preliminary draft final average borehole soil VOC values which were then rounded to the nearest whole number.
- 2 Final average borehole values will be calculated using the sample quantitation limit (SQL). SQLs will be provided from the contract lab as part of the final data package.
- ${\it 3\ Denotes\ duplicate\ (QA/QC)\ sample,\ duplicate\ samples\ were\ not\ used\ in\ the\ sample\ VOC\ averaging\ calculations.}$
- 4 Contingency Boring Locations
- 5 2 sets of analytical data reported by TA for the 35-40' interval at boring 001-318, SMO determined that reported values should be used. TCE Borehole Average changed from 66 μg/Kg to 52 μg/Kg.
- 6 Reportedly no 15-20 foot sample collected from 001-322.
- 7 Reportedly no 40-45 foot sample collected from 001-302.
- 8 <u>Qualifier Definitions:</u> U Non-detect; J Result is less than the RL but greater than or equal to the MDL and the concentration is an approximate value; X Surrogate is outside control limits; E Result exceeds the control limits; H Sample was prepped or analyzed beyond the specified holding time; * RPD of the LCS and LCSD exceeds the control limits.
- 9 For analytical results identified with a (U) qualifier, a value equal to one half of the sample quantitation limit (SQL) was used to calculate the Draft Final average borehole soil VOC values.
- 10 SMO adjusted analytical data for sample 001-304 collected at 20 ft (8-28-2012).

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Table 2. Southwest Plume Historical Characterization Data

Boring ID	Date of Collection	Depth, bgs	Prefix	Concentration	Qual
001-105	2/25/1998	10	<	700	U
001-105	2/25/1998	5	<	600	U
001-106	2/26/1998	10	<	400	U
001-106	2/26/1998	5	<	600	U
001-107	2/25/1998	10	<	500	U
001-107	2/25/1998	5	<	600	U
001-108	2/25/1998	10	<	500	U
001-108	2/25/1998	5	<	600	U
001-109	2/24/1998	10	<	500	U
001-109	2/24/1998	5	<	500	U
001-110	2/24/1998	10	<	500	U
001-110	2/24/1998	5	<	500	U
001-111	2/23/1998	10	<	500	U
001-111	2/23/1998	5	<	600	U
001-113	2/23/1998	10	<	600	U
001-113	2/23/1998	5	<	800	U
001-114	2/24/1998	10	<	500	U
001-114	2/24/1998	5	<	600	U
001-115	2/25/1998	10	<	600	U
001-115	2/25/1998	5	<	600	U
001-116	2/27/1998	10		100	J
001-116	2/27/1998	5	<	500	U
001-117	2/25/1998	10	<	500	U
001-117	2/25/1998	5	<	500	U
001-118	2/25/1998	10	<	600	U
001-118	2/25/1998	5	<	700	U
001-119	2/25/1998	10	<	700	U
001-119	2/25/1998	5	<	700	U
001-126	2/26/1998	10	<	600	U
001-126	2/26/1998	5	<	700	U
001-127	2/26/1998	10	<	400	U
001-127	2/26/1998	5	<	500	U
001-128	2/26/1998	10	<	400	U
001-128	2/26/1998	5	<	700	U
001-129	2/24/1998	10	<	500	U
001-129	2/24/1998	5	<	600	U
001-130	2/23/1998	10	<	500	U
001-130	2/23/1998	5	<	500	U
001-131	2/23/1998	10	<	600	U
001-131	2/23/1998	5	<	800	U
001-132	2/23/1998	10	<	270	U
001-132	2/23/1998	5	<	600	U
001-133	2/23/1998	10	<	600	U
001-133	2/23/1998	5	<	600	U

Table 2. Southwest Plume Historical Characterization Data (Continued)

Boring ID	Date of Collection	Depth, bgs	Prefix	Concentration	Qual
001-134	2/24/1998	10	<	500	U
001-134	2/24/1998	5	<	500	U
001-135	2/26/1998	10	<	400	U
001-135	2/26/1998	5	<	600	U
001-152	3/5/1998	10		170	J
001-152	3/5/1998	5		55	J
001-153	3/5/1998	10		2100	
001-153	3/5/1998	5		480	
001-154	3/5/1998	10		26	J
001-154	3/5/1998	5		60	J
001-155	3/6/1998	10		460	
001-156	3/6/1998	10		48000	
001-156	3/6/1998	5		31000	
001-157	3/6/1998	10		87000	
001-157	3/6/1998	5		12000	
001-158	3/6/1998	10		10000	
001-158	3/6/1998	5		2200	
001-159	3/6/1998	10		100	J
001-160	3/9/1998	10		200	J
001-160	3/9/1998	5		100	J
001-161	3/6/1998	10		200	J
001-161	3/6/1998	5		100	J
001-162	3/9/1998	10	<	500	U
001-162	3/9/1998	5	<	600	U
001-165	3/16/1998	17		439000	
001-165	3/17/1998	20		1900	
001-165	3/17/1998	25		50000	
001-165	3/17/1998	30		85000	
001-165	3/17/1998	35		74000	
001-165	3/17/1998	43		45000	
001-165	3/17/1998	45		66000	
001-165	3/17/1998	50		25000	
001-166	3/18/1998	5		5000	
001-166	3/18/1998	12		12000	
001-166	3/18/1998	18		14000	
001-166	3/18/1998	21		22000	
001-166	3/18/1998	27		23000	
001-166	3/18/1998	33		18000	
001-166	3/18/1998	38		11000	
001-166	3/18/1998	42		300	J
001-166	3/18/1998	47	<	800	U
001-166	3/18/1998	50	<	700	U
001-168	3/21/1998	5	<	900	U
001-168	3/21/1998	13		170	J

Table 2. Southwest Plume Historical Characterization Data (Continued)

Boring ID	Date of Collection	Depth, bgs	Prefix	Concentration	Qual
001-168	3/21/1998	18		40	J
001-168	3/21/1998	23		800	
001-168	3/21/1998	25		26000	
001-168	3/21/1998	29		26000	
001-168	3/21/1998	33		5500	
001-168	3/21/1998	38		2700	
001-168	3/21/1998	43		5000	
001-168	3/21/1998	47		4200	
001-168	3/21/1998	50		4300	
001-169	3/23/1998	18	<	900	U
001-169	3/23/1998	23		42	J
001-169	3/23/1998	28		100	J
001-169	3/23/1998	33		800	
001-169	3/23/1998	36		1200	
001-169	3/23/1998	38		700	J
001-169	3/23/1998	42		12000	
001-169	3/23/1998	45		18000	
001-169	3/24/1998	50		9400	
001-171	4/2/1998	5	<	900	U
001-171	4/2/1998	10	<	900	U
001-171	4/2/1998	18	<	800	U
001-171	4/2/1998	20	<	1400	U
001-171	4/2/1998	25	<	900	U
001-171	4/2/1998	30	<	900	U
001-171	1/1/1998	35	<	1100	U
001-171	4/2/1998	40	<	1400	U
001-171	4/2/1998	45	<	900	U
001-171	4/2/1998	50	<	1300	U
001-172	4/3/1998	15	`	900	J
001-172	4/3/1998	20	<	900	U
001-172	4/3/1998	25		7000	
001-172	4/4/1998	31		1700	
001-172	4/4/1998	35	<	1100	U
001-172	4/4/1998	40	<	900	U
001-172	4/4/1998	45	<	900	U
001-172	4/4/1998	50		400	J
001-172	4/6/1998	5	<	900	U
001-173	4/6/1998	13	<	900	U
001-173	4/6/1998	18	<	900	U
001-173	4/6/1998	25		15	J
001-173	4/6/1998	30	<	1400	U
001-173	4/6/1998	35	<	1100	U
001-173	4/6/1998	43	<	1100	U
001-173	4/6/1998	45		8	J

Table 2. Southwest Plume Historical Characterization Data (Continued)

Boring ID	Date of Collection	Depth, bgs	Prefix	Concentration	Qual
001-173	4/6/1998	50	<	1000	U
001-174	4/8/1998	15	<	900	U
001-174	4/8/1998	20	<	800	U
001-174	4/8/1998	28	<	1100	U
001-174	4/8/1998	30		200	J
001-174	4/8/1998	38	<	1000	U
001-174	4/8/1998	43	<	900	U
001-174	4/8/1998	45	<	1000	U
001-174	4/8/1998	50	<	800	U
001-179	4/23/1998	15	<	800	U
001-179	4/23/1998	20	<	1100	U
001-179	4/23/1998	25	<	800	U
001-179	4/23/1998	30	<	800	U
001-179	4/23/1998	35	<	1000	U
001-179	4/23/1998	40	<	1000	U
001-179	4/23/1998	45	<	900	U
001-179	4/23/1998	50	<	900	U
001-201	5/26/2004	15.5		690	
001-201	5/27/2004	30		1700	EXY
001-201	5/27/2004	50.5		1000	EXY
001-201	5/27/2004	56		210	
001-202	6/9/2004	0		780	
001-202	6/9/2004	13		110	
001-202	6/9/2004	30.5		2400	Е
001-202	6/9/2004	47		3500	
001-202	6/9/2004	59.5		3400	
001-203	5/27/2004	15	<	2	U
001-203	5/28/2004	33	<	2	U
001-203	5/28/2004	47	<	2	U
001-203	5/28/2004	51.5	<	2	U
001-204	6/10/2004	20.5		200	
001-204	6/10/2004	30.5		60	
001-204	6/11/2004	45.5		370	
001-204	6/11/2004	58.5		290	
001-205	6/2/2004	18		22	
001-205	6/2/2004	30		860	
001-205	6/2/2004	46		210	
001-205	6/2/2004	54.5		3.2	

1.4 ENVIRONMENTAL VISUALIZATION SOFTWARE EVALUATION AND VOC MASS ESTIMATE

TCE results in soil were interpolated using the C Tech EVS-ES to estimate the mass of TCE at SWMU 1 and the horizontal and vertical extent of contamination at isoconcentration levels of 73 μ g/kg, 1,000 μ g/kg, and 10,000 μ g/kg. The primary purpose of the TCE mass estimate is to assist in the design of the off-gas treatment system. In addition, the EVS-ES estimate of extent is used to determine the layout of the LDA borings.

EVS is similar to other Environmental Decision Support Software (DSS), such as SitePro and Spatial Analysis and Decision Assistance, and was evaluated by EPA and DOE in 1998 with five other DSS packages. EVS underwent an environmental technology verification report in March 2000 that concluded that "the main strengths of EVS-PRO are its outstanding 3-D visualization capabilities and its capability to rapidly process, analyze and visualize data" and "the demonstration showed the EVS-PRO software can be used to generate reliable and useful analyses for evaluating environmental contamination problems."

Several interpolation techniques, including IDW, nearest neighbor, and kriging were evaluated, with kriging ultimately selected as the primary interpolation technique. Kriging is a stochastic technique similar to IDW averaging in that it uses a linear combination of weights at known points to estimate the value at the grid nodes. Kriging is named after D.L. Krige, who used the kriging underlying theory to estimate ore content (Krige 1951). Kriging uses a variogram (also called a semivariogram), which is a representation of the spatial and data differences between some or all possible "pairs" of points in the measured data set. The variogram then describes the weighting factors that will be applied for the interpolation.

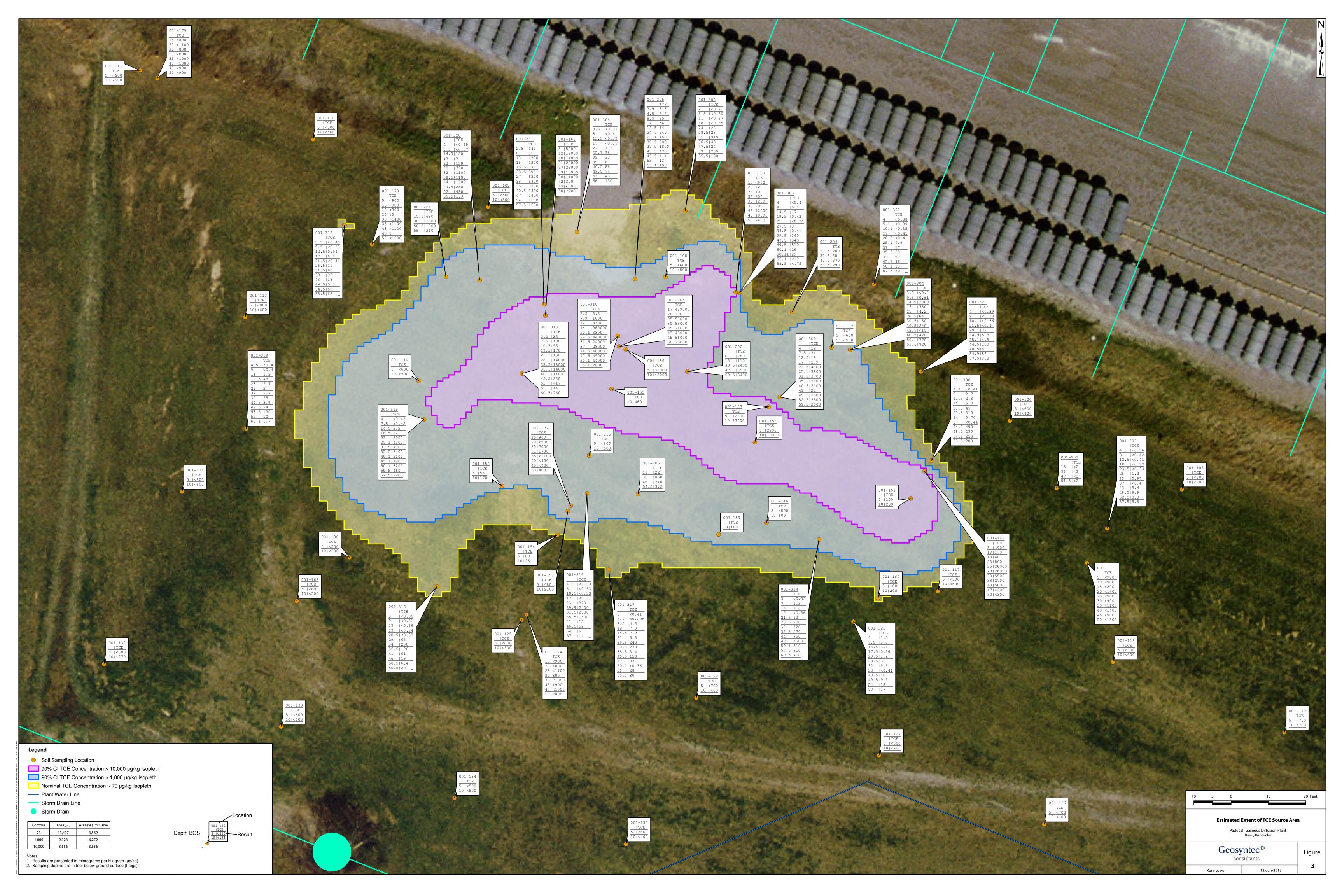
It is acknowledged that there are significant uncertainties associated with providing a mass estimate of dense nonaqueous-phase liquid (DNAPL) regardless of the interpolation technique; however, kriging is a useful and valid approach to estimating the extent of source area at various isoconcentration levels below the threshold of residual saturation. Kriging also provides insight about the mass distribution at differing isoconcentration levels. Uncertainty has been considered by estimating mass at different levels of statistical confidence. By kriging data at every node of the model, an average value along with a standard deviation is calculated, thus providing a range of estimated TCE concentrations and ultimately mass. A level of significance of 0.1 [i.e., 90% confidence interval (CI)] was used in modeling the geometry and mass of TCE above 1,000 and 10,000 μg/kg to address uncertainty in the estimates.

A one-layer geologic model was built focusing on the top 65 ft of soil for modeling soil analyte distribution. Chemical results collected during evaluation of the UCRS (1998 and 2004) and RDSI (2012) sampling of SWMU 1 soils completed within and immediately surrounding the defined SWMU 1 source area are shown in Figure 3.

Due to elevated detection limits at select locations (typically within the range of 500 to 900 μ g/kg compared to the SWMU 1 treatment standard for TCE of 73 μ g/kg), data from the historic 1998 and 2004 UCRS investigations were analyzed in EVS using 1 μ g/kg for the detection limit for nondetect results. This detection limit is consistent with the typical detection limits observed in the RDSI data.

Due to duplicate sampling results in the historical datasets (i.e., multiple TCE analytical results for a given sampling location and depth interval), a set of decision rules was developed to select the most appropriate result to use in the modeling. The following were the rules followed in selecting a value when duplicate results were available:





- For two detects, take the highest value.
- For two detects with qualifiers, take the value that has the lowest number of qualifiers.
- If both nondetect values are the same, use the data point with the lowest detection limit.
- If one data point is detect and the other is estimated, take the detected value.
- If one data point is nondetect and the other is estimated, take the estimated value.

With few exceptions, the EVS-ES modeling was performed using the typical software defaults. The model parameters are documented in a calculation package included as Appendix B. The horizontal/vertical anisotropy ratio parameter, which allows the model to take into consideration expected differences in fluid flow through the soil matrix, was set to 1 versus the default of 10. This value was set at 1 to best represent the anticipated distribution of chemicals, as well as resulting in more conservative estimates of chemical mass. The Octant Search method was used to determine which sample points are selected for inclusion in the kriging matrix. This method refines the data points used in the local kriging matrix and results in better performance with clustered data. An Octant is any of the eight parts into which three mutually perpendicular planes divide space. Using EVS Octant search, searching is performed for each of the eight Octants surrounding the point to be kriged. The octant search algorithm is performed for every interpolated node of the model. Within each octant, a maximum number of points (up to one-fourth of the total points) is selected. Then, points are taken sequentially from each octant to the maximum number of total points or until all octant points have been used. Preference is given to points that are proximal to the interpolation point. Theoretically, there could be small extents such that some analytical data never would be used in the interpolation, but that would occur only in locations with clustered data over a small extent. Given the data distribution, for all intents and purposes, all the available analytical data were used in the interpolation. The model used a soil density of 1.5 gram per cm³ and a chemical density of 1.46 gram per cm³. The model's mass calculations then were reviewed and compared to hand calculations of the mass. A compact disc, which includes the EVS-ES output files, is included as Appendix B.

Mass estimates were calculated using kriging, kriging using the 90% CI, IDW, and nearest neighbor. The results of the EVS-ES modeling using the historical results and the RDSI soil results are presented in Table 3.

From a mass distribution perspective, both the 90% CI kriging and nearest neighbor interpolation indicate that 96% of the estimated mass is located within the greater than 1,000 μ g/kg isocontour area. The EVS estimated weight calculated is lower than the weight estimated in the SI.

The horizontal extent of the 73 μ g/kg isocontour using nominal kriging interpolation is estimated to be approximately 13,500 ft². The 1,000 μ g/kg and 10,000 μ g/kg isocontours using the 90% CI kriging interpolation are estimated to be approximately 9,900 ft² and 3,700 ft², respectively. The isocontours are shown on Figure 3.

Table 3. Mass Estimates

	Kriging	90% CI Kriging	IDW	Nearest Neighbor
Isoconcentration Level µg/kg	Mass of TCE (gal)			
73	8.9	29.3	1.4	24.8
1,000	8.0	28.1	0.5	23.7
10,000	4.2	19.8	0.1	18.0

1.5 SEQUENCING WITH OTHER REMEDIES

This RA will be executed in coordination with the Soils Operable Unit (OU) remediation of surface (< 1 ft) and subsurface soil (> 1 ft and < 10 ft) contaminants, as appropriate. The Soils OU remediation currently is planned for implementation following the SWMU 1 groundwater VOC contaminant source RA. A review of contaminants that exceed the no action level (NAL), as contained in Soils OU RI, DOE/LX/07-0258&D2, (DOE 2012c) was performed. The evaluation contained in the remedial investigation report separated the soils into surface and subsurface. Surface soils are located < 1 ft in depth; subsurface soils are located > 1 ft in depth and less than 10 ft in depth.

The surface soils in the area to be mixed contain polychlorinated biphenyls (PCBs) and metals above the Industrial NAL (DOE 2012c). The expected maximum PCB and metal contaminant concentrations in the soil mixing area are as follows:

•	PCBs	3.4 mg/kg
•	Arsenic	6.3 mg/kg
•	Beryllium	0.7 mg/kg
•	Cadmium	6.4 mg/kg
•	Cobalt	13.7 mg/kg
•	Vanadium	24 mg/kg

No VOCs, radioactive compounds or semivolatile organic compound exceeded the NAL in the surface soils in the area to be soil mixed. To protect the aboveground treatment system from potential PCB contamination and to facilitate greater depths in soil mixing, prior to implementing the deep soil mixing RA, the top 2 ft of the treatment/source area soil to be mixed, as defined in Figure 4, will be removed, stockpiled adjacent to the mixing area on a synthetic liner and covered with a liner to prevent erosion, and respread in the excavation after soil mixing action is complete. The excavation of surface soil supports the soil mixing in the following ways:

- 1. PCBs contacting the mixing equipment or passing through the vapor of liquid treatment system could contaminate the equipment and prevent the release of the equipment.
- 2. The presence of the metals could result in their being solubilized and passing through the treatment equipment and resulting in excess metals in the treatment effluent.
- 3. The soil mixing equipment with the 8-ft augering system, combined and our soil conditions, is limited to a depth of 60 ft, and the excavation will assist in attaining mixing to the bottom of HU4 (see Section 2).

During excavation of the top 2 ft of soil, the exposed area to be soil mixed will be inspected visually and will be probed with hand tools to determine if engineered layers of gravel are present near the surface that could inhibit effective vacuum extraction through the soil mixing hood. If the presence of such engineered gravels is detected, the graveled areas will be excavated and stockpiled, with the upper 2 ft for spreading after the soil mixing operations have been completed.

Following completion of the mixing process, the excavated area will be backfilled with the excavated surface and subsurface soils (0 ft to 2 ft) to bring the ground surface back to grade with the surrounding unmixed area. Because soils in the mixing area will be disturbed, the surface soils in that area will require recharacterization for use in the Surface Soils OU. DOE will recharacterize those soils (0 ft to 2 ft) as part of the Soils OU at the appropriate time in the future prior to selecting an appropriate remedial measure. To provide for continuity among the OUs, DOE will insert a footnote in Appendix 5 of the FY 2014 Site

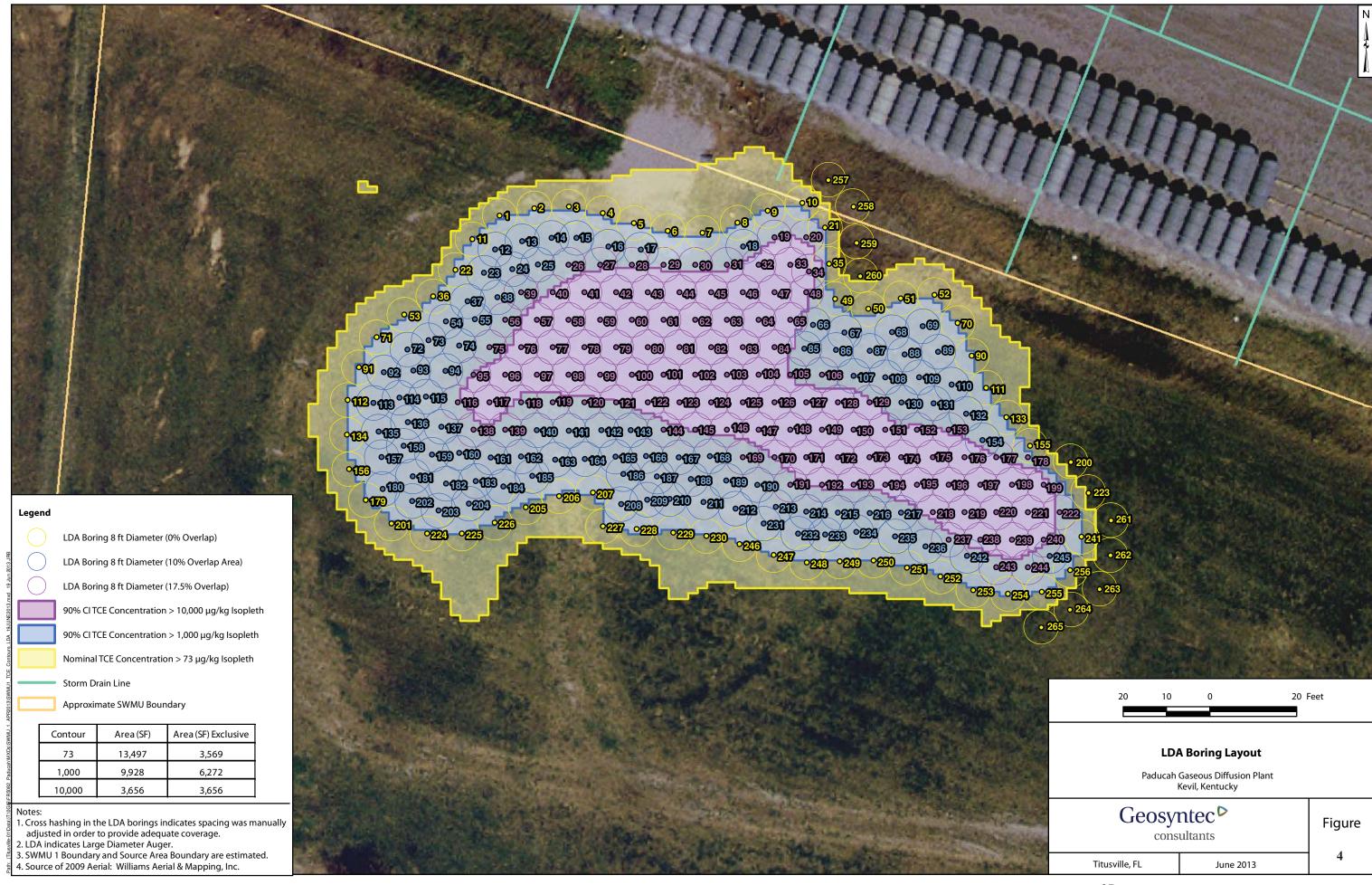
Management Plan stating that the D1 Feasibility for Soils OU Remedial Action 1 will evaluate VOC soil contamination at SWMU 1 that did not undergo active treatment (i.e., deep soil mixing). The surface soils located outside of the area to be soil mixed will be addressed, as appropriate, by the Soils OU at a later date. The replacement of the excavated soils is not expected to contaminate the subsurface UCRS soil at depth because the subsurface soils will be loaded with a minimum of 0.5% ZVI to provide for treatment of residual VOCs including those potentially migrating from the surface. PCBs in the replaced soil are not expected to become mobile after replacement because PCBs have a tendency to bind with soil. Until the completion of the Soils OU actions (0 ft to 10 ft), the interim LUCs to be instituted following completion of SWMU treatment by the Groundwater Operable Unit will serve to insure protectiveness of the worker until such time as the Soils OU can address remaining contaminants present in the 0-10 ft zone throughout the SWMU.

2. TREATMENT TECHNOLOGY

This RA will implement *in situ* source treatment using deep soil mixing with interim LUCs. The selected RA technology involves the utilization of LDAs combined with the introduction of hot air/steam for thermal volatilization and stripping of VOCs in soil and groundwater in the UCRS and upper RGA (hydrogeologically) soils to a depth of 62 ft bgs (takes into consideration the removal of the top 2 ft of soil prior to LDA implementation). To confirm the treatment of the UCRS and upper RGA (HU4) soils, the mapped source treatment area was placed over a kriging-based evaluation of the HU4/HU5 interface (Figure 4). This information, which is based upon the RDSI soil borings, documents that the HU4/HU5 interface is a maximum of 62 ft bgs within the treatment area. Accordingly, the proposed treatment depth of 62 ft bgs matches or exceeds the HU4/HU5 interface within the treatment area.

Granular ZVI in a guar gum solution also will be delivered to the subsurface via LDA injection as a polishing step to provide treatment of residual VOCs within the source area.





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A vapor treatment system will be utilized that includes real-time monitoring and provides a real-time indication of the level of contamination in specific zones being treated. Real-time monitoring will assist in controlling the process parameters to maximize VOC removal, control of operating treatment equipment, and support operation of the LDA and injection systems.

A more detailed description of the treatment technology and process is included in Section 4.

3. TREATMENT SYSTEM OBJECTIVES

As discussed in Section 2, design information, including contaminant levels, areas of soil VOC impacts and mass present in the treatment zone, was obtained during the RDSI. The RDSI information regarding the distribution of VOCs in the treatment zone is used in this design to optimize the LDA treatment area layout and auger boring overlap to provide effective VOC treatment and achieve project objectives. The following subsections provide discussions on the remedial action objectives and the key operational parameters of the mixing process to attain the objectives.

3.1 RA OBJECTIVES

The following remedial action objectives (RAOs) are defined in the ROD for the Southwest Plume source areas (DOE 2012a).

- (1) Treat and/or remove the principal threat waste consistent with the National Contingency Plan;
- (2a) Prevent exposure to VOC contamination in the source areas that will cause an unacceptable risk to excavation workers (< 10 ft);
- (2b) Prevent exposure to non-VOC contamination and residual VOC contamination through interim LUCs within the Southwest Plume source areas (i.e., SWMU 1, SWMU 211-A, and SWMU 211-B) pending remedy selection as part of the Soils OU and the Groundwater OU; and
- (3) Reduce VOC migration from contaminated subsurface soils in the treatment areas at the Oil Landfarm and the C-720 Northeast and Southeast Sites so that contaminants migrating from the treatment areas do not result in the exceedance of maximum contaminant levels in the underlying RGA groundwater.

3.2 OPERATIONAL PARAMETERS

The design will allow for operational parameters to be monitored during the treatment period. Operational parameters to be monitored and evaluated will include the following:

- LDA Operational Monitoring for
 - Depth penetration rate
 - Auger rotational rate
 - Applied torque
 - Down-hole temperature

- Temperature, flow rate, and injection pressure for
 - Injected steam
 - Compressed/heated air
 - ZVI slurry mixture
- Vapor recovery flow rate, temperature, and vacuum pressure
- Extracted VOC concentrations
- Treated vapor phase VOC concentrations

4. TECHNICAL DESIGN

4.1 TECHNICAL JUSTIFICATION FOR SELECTION OF REMEDIAL TECHNOLOGY

The selected RA technology for the Southwest Plume VOC Oil Landfarm source area involves the utilization of *in situ* soil mixing with LDA a projected (265) boring locations combined with the introduction of hot air/steam for thermal volatilization and stripping of VOCs in soil and groundwater within the target treatment zone. Additionally, granular ZVI in a guar gum solution will be delivered to the subsurface via LDA injection as a polishing step to provide additional treatment. Due to the significant operational flexibility provided by this technology, the actual number of LDA borings completed may change based on remedial team discussion (to include representatives from EPA, KDEP, DOE, and DOE design team representatives) that may occur during remedial implementation based on analysis of real-time field-collected data from the remedial equipment.

Prior to selecting the proposed RA, technology permutations considered included (1) LDA soil mixing with emulsified ZVI delivery, (2) LDA soil mixing with oxidant delivery, and (3) LDA soil mixing with ZVI and clay delivery. Based upon an evaluation of implementation approaches, the *in situ* LDA soil mixing with hot air/steam and ZVI injection offers (1) the highest anticipated level of mass reduction and potential to achieve objectives, (2) an implementation cost that falls within the range of the other technology permutations considered, and (3) demonstrated effectiveness for providing treatment of high levels of VOCs. Unique to the *in situ* LDA soil mixing with hot air/steam and ZVI injection technology, the mixing process and treatment application is adapted real-time based upon the monitoring of off-gas VOC concentrations (discussed in Sections 4.2 and 4.4.2.2). Accordingly, the selected RA has flexibility and can be actively adapted during individual borehole mixing to spend additional time, providing enhanced treatment to specific depth intervals and/or boreholes with higher levels of VOCs, as appropriate (discussed in Section 4.4.2.1).

4.2 CRITICAL PARAMETERS

Critical parameters for *in situ* LDA soil mixing with hot air/steam and ZVI injection are those operational parameters of the system and the physical and chemical parameters of the media being treated that have the greatest impact on the ability of the technology to meet the performance goals. These critical parameters are as follows.

Soil and Groundwater Temperature. The temperature of soil and groundwater throughout the treated volume must be raised sufficiently to achieve volatilization of the targeted contaminants. The target soil and groundwater temperature to achieve volatilization of identified VOCs in the treatment zone will be 170°F, which has been demonstrated to achieve volatilization of TCE and daughter products at other sites

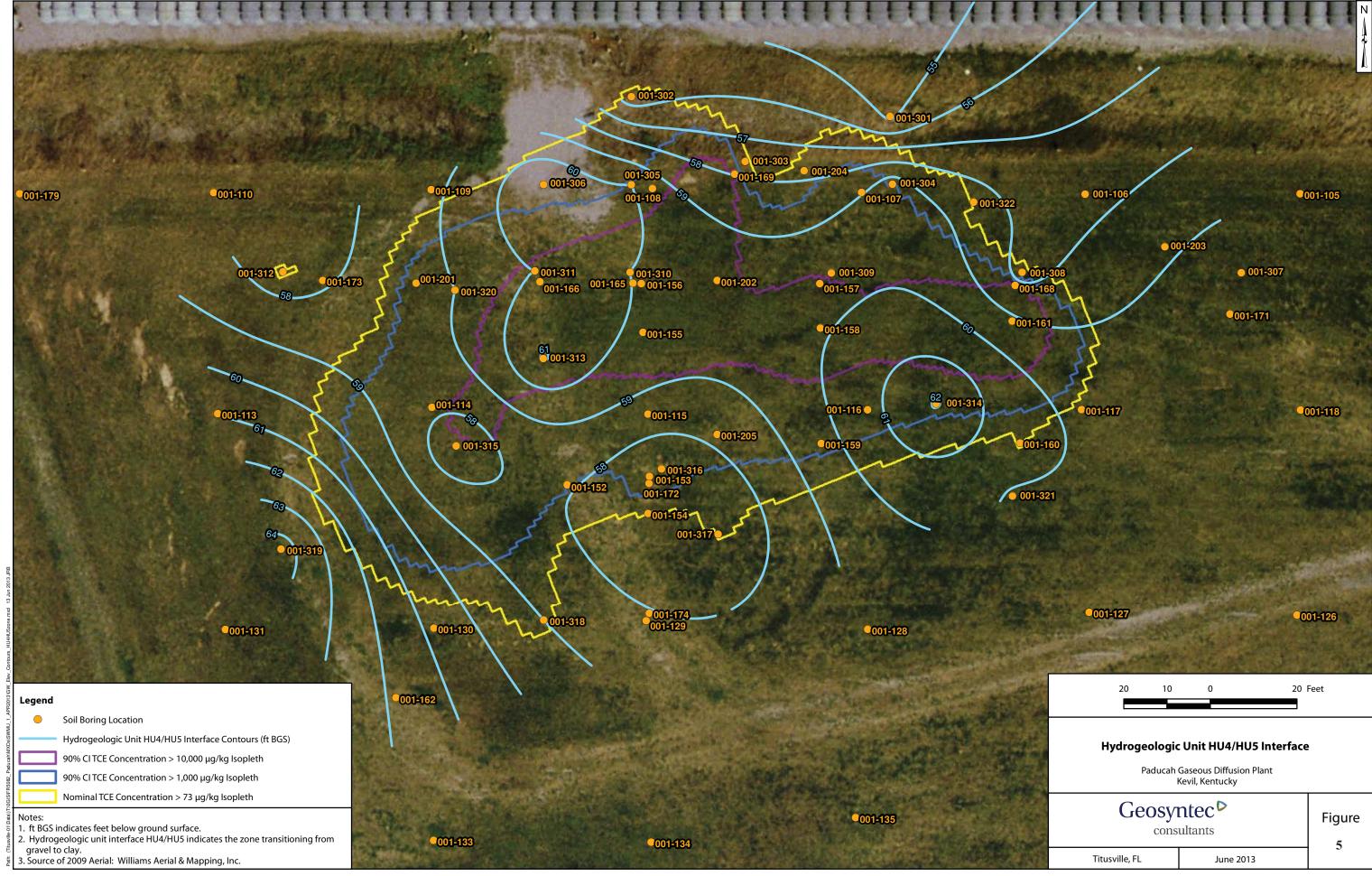
[e.g., Launch Complex 15, Ordnance Support Facility 1381 (USAF 2008), Security Police Confidence Course located at Cape Canaveral Air Force Station (USAF 2007); and Offutt Air Force Base, Nebraska (USACE 2012)] that have employed this remedial technology (the injected hot air/steam contacting the soil will have a temperature exceeding 200°F). A downhole thermocouple data logger, physically mounted to the LDA auger blade, will be used to monitor subsurface temperatures at the end of mixing operations for any given time period. The data logger will be retrieved from the LDA auger blade to download and view the data. The temperature of gas collection will be measured in the surficial shroud in real time. It has been established, based on experience at other sites (identified above) that, by adding a correction factor of 10°F to the shroud gas temperature, the resultant is representative of the downhole temperature. These studies were performed through installation of thermocouples posttreatment (at least 5 days) that indicated that subsurface temperatures typically were measured at approximately 10°F greater than the measured shroud temperature during mixing. It is noted that some cooling may have occurred during the lag time between treatment and posttreatment measurements; therefore, this correction factor is assumed to be conservative. Though it is noted that the downhole thermocouple may be slightly biased by the friction of auger rotation, this data measurement is offered to provide a singular line of evidence regarding downhole temperatures achieved through thermal treatment. Accordingly, a shroud gas temperature of 160°F will be utilized as a real-time indicator of adequate subsurface temperature for VOC volatilization.

Percentage of Auger Boring Overlap. The LDA borings will be established based upon three overlap spacing scenarios with slight variation in the three scenarios as needed to place circular soil mixing columns within the irregular geometric area. The fixed overlap scenarios are 0% (no overlap); 10% (some overlap for reduction of interstitial space between treatment cells/borings); or 17.5% (representing complete overlap with no interstitial space between treatment cells/borings). The overlap spacing is varied based upon on the average concentration of TCE in the RDSI soil borings. The LDA boring overlap consists of the following overlap scenarios:

- A 17.5% overlap will be provided in the area within the greater than 10,000 μ g/kg average TCE isoconcentration contour (928 ft² area).
- A 10% overlap will be provided in the area within the greater than 1,000 μ g/kg and less than 10,000 μ g/kg average TCE isoconcentration contours (4,163 ft² area).
- A 0% overlap (or greater to account for auger boring layout spacing) will be provided in the area within the greater than 73 μ g/kg and less than 1,000 μ g/kg average TCE isoconcentration contours (8,332 ft² area).

Due to transition issues among the three overlap scenarios and to resolve interference between borings in geometric placement, the overlap in some cases has been increased or decreased slightly. This slight modification in overlap allows the optimized placement of the soil mixing borings. The soil mixing borings which the slight modification incorporated are shown with cross-hatching in Figure 5. The slight modification in overlap is not expected to result in decreased effectiveness of the remedial action because, the LDA boring overlap scenario exceeds what has been used previously at other locations. The successful LDA technology implementation at the Security Police Confidence Course (Facility 18003) at Cape Canaveral Air Force Station, which used a 6% overlap throughout (USAF 2007); and the Ordnance Support Facility at Cape Canaveral Air Force Station, which used a 0% overlap throughout (USAF 2008). The referenced sites are located in a fully-saturated sand aquifer, which reflects a heating environment that is more difficult to steam volatilize VOCs than the soils present at SWMU 1. Additionally, the Offutt Air Force Base LDA soil mixing project was performed in a lithology-type (silty clay) similar to SWMU 1 and also achieved project objectives (USACE 2012). Figure 5 presents the LDA boring layout and up to





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265 proposed boring locations. Boring locations will be surveyed by a professional, licensed land surveyor prior to implementation of soil mixing. As previously noted, due to the significant operational flexibility provided by this technology, the actual number of LDA borings completed may change based on remedial team discussion (to include representatives from EPA, Kentucky Department for Environmental Protection (KDEP), DOE, and DOE design team representatives); these may occur during remedial implementation based on analysis of real-time field-collected data from the remedial equipment.

Soil Properties/Mixing Rate. Soil properties dictate the rate at which the LDA can penetrate the subsurface, appropriate angle of repose for the mixing blade, and considerations regarding the auger blade terminus. In consideration of the soil characteristics and consistency in the Oil Landfarm source area, which includes a hard layer identified in standard penetration test (SPT) borings in the site vicinity, it is anticipated that "rock teeth" will be required on the auger blades. For the *in situ* LDA soil mixing with hot air/steam and ZVI injection technology to be effective, no large boulders and/or large subsurface concrete structures can be present. No anomalies were identified during the RDSI. Previously, two anomalies were found through geophysical techniques and these were excavated. One was a large concrete pipe that did not appear to be associated with the former operations of the SWMU. The second anomaly was not identified, but was believed to have been a result of the presence of small metal objects such as drum lids, bungs, metal shavings, etc. Appendix C includes SPT blow count data and geotechnical data for soils anticipated to be encountered during LDA soil mixing for determination of penetration rate, angle of repose for the mixing blade/auger blade, and blade type selection by equipment vendors.

VOC Vapor Extraction Rate. The rate of air/vapor extraction from the vadose zone must be greater than the production of contaminant vapors to prevent vaporized contaminants from escaping to the atmosphere or from condensing in the vadose zone. The vapor extraction equipment will be capable of extracting vapors at a flow rate that is twice the maximum flow rate of the hot/air steam injection equipment, and field monitoring will ensure that vapor extraction is occurring at a rate not less than 50% greater than the concurrent hot air/steam injection flow rate. If field observations indicate that the measured vapor extraction rate is not at least 50% greater than the concurrent hot air/steam injection flow rate, then either the injection flow rate will be reduced and/or RAs will be ceased temporarily until the vapor extraction rate has been modified to achieve the design criteria. LDA soil mixing, thermal treatment, VCS, vapor treatment, and ZVI injection equipment will be operator-controlled by a workman experienced in the operation of this equipment (similar to previous applications of the technology). Due to the complexity of the equipment and because equipment operators maintain shutdown procedures specific to their equipment, it typically is inappropriate for alarm conditions to cause automatic shutdown of this remedial equipment. Alarm conditions are provided to alert the experienced operator of such conditions so that they can react accordingly. For example, a loss of vacuum in the collection shroud would result in a notification to the operator, which would trigger the operator to cease treatment operations until the alarm condition can be corrected. Additionally, workers will monitor the air in the worker breathing zone with an Organic Vapor Analyzer fitted with a flame ionization detector (FID)/photoionization detector (PID) (PID lamp 10.6 eV), after methane subtraction, to evaluate a condition where VOCs may escape the shroud pursuant to a project-specific health and safety plan (Section 8).

Concentration of VOCs in Extracted Vapor. The concentration of VOCs in the vapor extraction stream must be monitored in real time and balanced with the aboveground treatment system's ability to treat such concentrations. Gas samples from the process streams will be collected from the vapor extraction system for analysis by a PID/FID(after subtracting a methane value) and/or a gas chromatograph (GC). Regarding the subtraction of the methane value, the technique of flame ionization detection relies on the ionization of molecules during high temperature combustion in the reaction zone of the FID-flame to determine the total volatile organic concentration within a continuous gaseous sample (includes both methane and VOCs). The methane content of the continuous sample may be determined by directing the sample through a bed of activated carbon to remove VOCs (methane is not removed by the carbon) and

then into the FID. The methane concentration then may be subtracted from the total volatile organic concentration to obtain the difference, which represents the VOC concentration of the continuous gaseous sample. Note: It is not anticipated that significant methane concentrations exist in the subsurface at SWMU 1; however, the method of methane subtraction has been proposed to mitigate the potential that an FID measurement would be biased high due to the presence of methane, if present, in the subsurface.

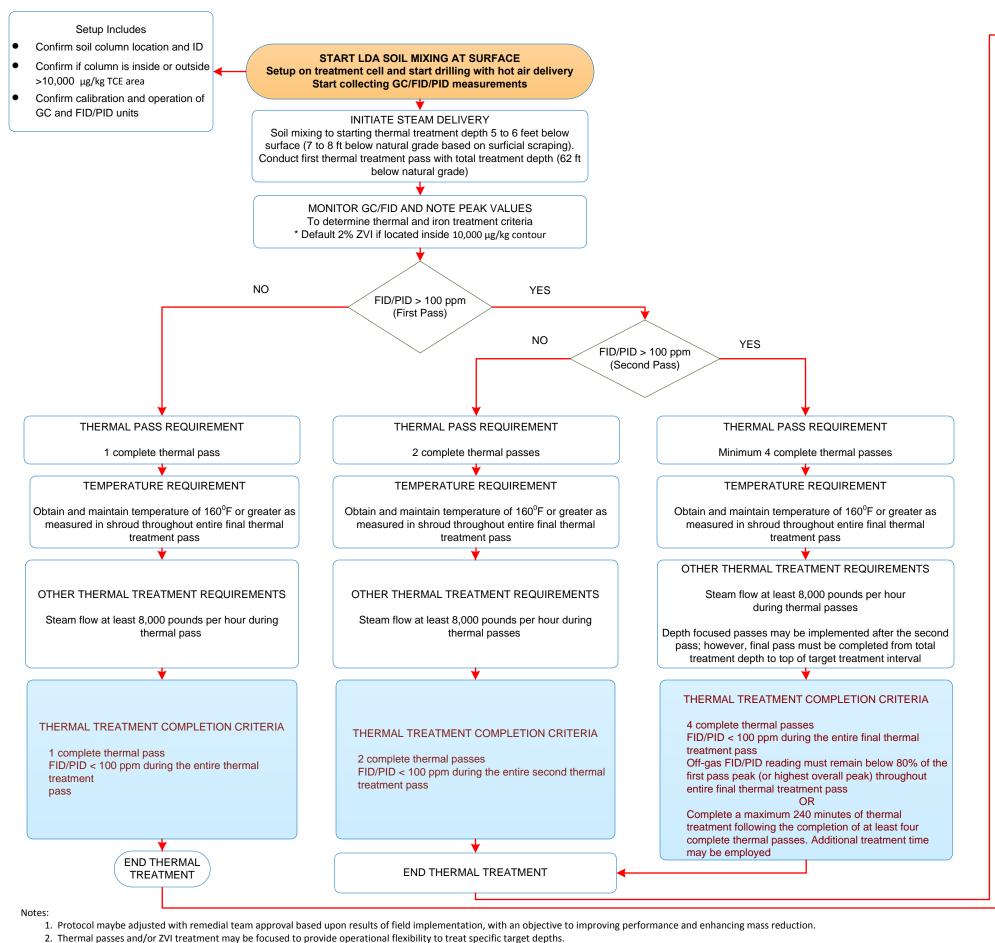
In the unlikely event the LDA soil mixing vendor-specific PID/FID and/or GC data monitoring equipment becomes saturated due to the presence of high VOC concentrations and/or DNAPLs present in the subsurface, LDA soil mixing will be paused until appropriate adjustments are made (adjustments will vary depending on specific equipment type) to allow resumption of vapor analysis. LDA soil mixing will be restarted when appropriate adjustments are made in the field (based upon vendor specific equipment) to compensate for the elevated concentrations by adjusting the ascent/descent rate of soil mixing, recalibration of the PID/FID equipment to a higher calibration standard to facilitate measurement, and/or introduction of additional bleed air to the system to provide for the adequate real-time monitoring of VOCs. The continuous monitoring of PID/FID and/or GC results in the vapor extraction stream is required at all times to effectively document mass removal rates per LDA soil mixing boring location.

ZVI Dosing Concentration. A slurry mixture consisting of granular ZVI, water, and guar gum (to facilitate ZVI injection into the soil) will be delivered based upon a percentage by weight application rate; field-based decisions based upon monitoring data collected during hot air/steam mixing phase will be used to adjust the ZVI dosing concentration. The amount of ZVI delivered to an LDA boring location will be established based on the observed PID/FID response value of VOCs, after subtraction of methane, from the first thermal treatment pass according to the following criteria:

- If a maximum PID/FID reading of 1,000 ppm or less (after subtracting the methane value) is observed on the first thermal treatment pass, an application of 0.5% ZVI will be applied.
- If a PID/FID reading of 1,000 to 5,000 ppm (after subtracting the methane value) is observed on the first thermal treatment pass, an application of 1.0% ZVI will be applied.
- If a PID/FID reading exceeding 5,000 ppm (after subtracting the methane value) is observed on the first thermal treatment pass, an application of 1.5% ZVI will be applied.
- Based upon RDSI soil sampling results, the area within the greater than 10,000 µg/kg TCE isoconcentration contour area will be treated with a default application of no less than 1.5%, but not greater than 2% ZVI regardless of PID/FID response. This range of concentration has been presented based on practical limitations to injection of 2% ZVI observed at other sites.

A graphical depiction of decision criteria associated with ZVI dosing is presented in Figure 6. The ZVI dosing concentration will be measured as a percentage by weight of the column of soil being treated. The ZVI dosing strategy is consistent with the LDA soil mixing projects successfully implemented to treat TCE/DNAPL source areas at Cape Canaveral Air Force Station (USAF 2007; USAF 2008) and former Offutt Air Force Base (USACE 2012).

LDA/STEAM/ZVI TREATMENT PROTOCOL



RETURN TO START DEPTH For iron treatment, treat from surface (2 ft below natural grade based on surficial scraping) to total treatment depth (62 ft below natural grade) IRON TREATMENT CRITERIA (Based Upon First Pass FID/PID reading) NO Located within YES >10,000 µg/kg TCE isocentrration contour FID/PID < 1,000 ppm YES NO FID/PID < 5,000 ppm 1.5% iron ≤ 2.0% iron* 0.5% iron 1% iron IRON TREATMENT Commence iron treatment pass WASHOUT IRON On final pass and while returning to surface for treatment cell completion **END TREATMENT**

- 3. * 2% represents maximum achievable ZVI dosage, actual applied is anticipated to range from 1.5-2.0 %.
- 4. During the collection of FID readings, methane corrected values shall be provided.
- 5. Remedial team includes representatives from EPA, KY DAQ, DOE, and DOE design team representatives.

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Impact to Surrounding Structures, Utilities, and Operations. It must be possible to implement the treatment technology at the Oil Landfarm source area and to operate it with limited interference to site personnel and other facility operations. No obstructions involving utilities, metal, or concrete were identified during the RDSI. A depiction of identified utilities is presented on the Estimated Extent of TCE Source Area, Figure 3, and the LDA Equipment Staging Layout, presented on Figure 8. Previously, two anomalies were found through geophysical techniques and these were excavated. One was a large concrete pipe that did not appear to be associated with the former operations of the SWMU. The second anomaly was not identified, but was believed to have been a result of the presence of small metal objects such as drum lids, bungs, metal shavings, etc.

Contaminants of Concern. The technology is designed specifically for the treatment of VOCs. Unacceptable concentrations of other contaminants will be addressed consistent with the details discussed previously in Section 1.5, Sequencing with Other Remedies. Monitoring of the previous non-target/non-VOC contaminants of concern will be conducted in the collected vapor condensate and the off-gas discharges from the treatment system within a representative subset of the remedial monitoring protocol to establish whether additional condensate treatment measures and/or equipment decontamination procedures will be necessary.

4.3 DESIGN REQUIREMENTS

The general input requirements for the *in situ* LDA soil mixing with hot air/steam and ZVI injection remediation design include the following:

- Site location and general site logistics, including nearby structures and site activity (See Section 1.2);
- Buried underground utilities and obstructions (See Section 4.2, Impact to Surrounding Structures, Utilities, and Operations, and Figures 3 and 8);
- Shape and depth of the treatment area (See Section 2 and Figure 5);
- Site geology (See Section 1.1);
- Site hydrogeology, including depth to groundwater and groundwater flow rate (See Section 1.1);
- Soil chemical characteristics, including percentage of organic carbon content (See Section 1.3);
- Contaminant-specific remediation goals, defined in the FFS (DOE 2010a) and listed in Table 4;
- Compliance with applicable or relevant and appropriate requirements (ARARs)(ROD DOE 2012a);
- Absence of low-volatility co-contaminants (at the time of LDA soil mixing within treatment area) (See Section 1.5);
- Options for wastewater disposal (See Section 4.4.1.4); and
- Selection of vapor treatment technology (See Section 4.4.1.5).

Table 4. Cleanup Levels for the Oil Landfarm Source Area RA

Contaminant of Concern	Cleanup Levels for the Oil Landfarm, mg/kg
TCE	7.30E-02
1,1-DCE	1.30E-01
cis-1,2-DCE	6.00E-01
trans-1,2-DCE	1.08E+00
Vinyl Chloride	3.40E-02

Note: Also see ROD Tables 17 and 18 for the UCRS Soil Cleanup Levels for VOCs (DOE 2012a).

4.4 PROCESS DESCRIPTION FOR *IN SITU* LDA SOIL MIXING WITH HOT AIR/STEAM TREATMENT AND ZVI AMENDMENT

In situ LDA soil mixing with hot air/steam and ZVI treatment technology consists of the following major elements: soil mixing, hot air/steam generation and delivery, vapor extraction and conditioning, recovered-liquid treatment and disposal, ZVI mixing and delivery, and vapor treatment. The treatment system includes a monitoring system for real-time data evaluation that assists in controlling the process parameters to maximize VOC removal and supports decision making for operation of the LDA and injection systems.

The mixing system will be equipped with an LDA that shears and mixes the soil as the auger is advanced below the ground surface, while concurrently injecting steam and hot air. This action causes thermal desorption and volatilization of the VOCs from soil particles, groundwater and interstitial spaces. The steam and hot air raises the temperature of the soil mass, increases the vapor pressure of the contaminants, volatilizes the compounds from the soil particles (through heat and air stripping), and allows them to be transported to the surface via the injected hot air/steam where they are collected in a shroud maintained under vacuum, covering the active treatment area. The shroud provides the ability to capture off-gases beyond the auger blades. The vapors then are transported from the shroud through the vapor conditioning system (VCS) to the VOC treatment system by a blower. VOC removal and treatment will then be enhanced via the placement of ZVI in the mixed soil column and aquifer material to enhance abiotic degradation of residual VOCs.

The VOC treatment system consists of a VCS and vapor treatment system. Vapor collected in the LDA shroud contains air, water, VOCs, and particulates. The VCS removes water and particulates from the vapor before being processed by the vapor treatment system. The VCS consists of a knockout tank, chiller, re-heater/heat exchanger, and particulate filter. The vapor from the VCS will then be processed in the vapor treatment system, which will consist of vapor-phase GAC placed in series to remove VOCs. If field-collected data during remedial implementation indicates that greater than anticipated volumes of vapor-phase GAC are required to achieve off-gas treatment, other treatment system components (such as a mobile thermal oxidation unit) may be incorporated to replace or supplement the GAC units. The need for other vapor treatment system components is considered highly unlikely, and specifics on this system have not been included in the design. The liquids from the VCS will be stored in frac tanks. The water in each frac tank will be analyzed for VOCs and nontarget/non-VOC contaminants, including polycyclic aromatic hydrocarbons (PAHs), PCBs, radionuclides, and heavy metals, consistent with the Memorandum of Agreement for the Southwest Plume FFS (DOE 2010c), to establish whether additional treatment measures will be necessary prior to discharge. If additional treatment is necessary, the water will be treated on-site via recirculation through the frac tank utilizing liquid-phase GAC and ion exchange resins (Purolite A530E or equivalent) for removal of VOCs and other contaminants, if present, prior to discharge at a PGDP outfall (e.g., Outfall 008).

Real-time data monitoring is an integral part of the treatment technology because it facilitates real-time decision making to enhance the efficiency of treatment and maximize the results (i.e., additional mixing hot air/steam injection at specific locations and/or discrete depth intervals based upon real-time monitoring results).

4.4.1 Equipment Summary

The general process flow diagram for the *in situ* LDA soil mixing with hot air/steam and ZVI injection system for the Oil Landfarm source area is provided in Figure 7. General unit processes shown in Figure 7, including LDA soil mixing; hot air/steam generation and delivery; vapor extraction and conditioning; recovered-liquid storage, treatment, and disposal; ZVI mixing and delivery; and vapor treatment are described in the following sections.

4.4.1.1 Soil mixing equipment

Major equipment and tools that are to be utilized for soil mixing will include a crane, LDA, kelly bar, and drill platform. The soil mixing rig will be comprised of a crawler-mounted lift crane (Manitowac 777, 200-ton crane or approved equivalent, with a minimum 75-ft long by 13.5 inch² diameter hollow drill stem (kelly bar) driven by a high-torque transmission (Hain turn-table or approved equivalent) capable of producing a range of torque of approximately 100,000 to 450,000 ft-lb of torque) and capable of achieving a design soil mix depth of 60 ft bgs (which will be 62 ft below the original land surface elevation based upon the excavation of the upper 2 ft of soil in the mixing area prior to implementation). Alternate heavy equipment (such as excavator-mounted soil mixing equipment) will be considered as an appropriate alternative to a crane if it is capable of meeting the afore-mentioned range of torque and achieving the required target depth.

A swivel assembly attached to the end of the crane boom cables serves as the connection point for the kelly bar, allowing the bar to rotate freely while drilling. In addition, the swivel will serve as the injection point of material into the kelly bar from flexible hosing connecting the hot air/steam and ZVI delivery system to the soil mixing equipment. A multi-bladed rotating mixing/injection tool (auger) with a minimum diameter of 8 ft will be located at the base of the kelly bar, which is capable of injecting the hot air, steam, and ZVI slurry into the soil to volatilize and treat VOCs. The mixing tool will include injection ports every 8 to 10 inches along the back side of the mixing blade (or approved equivalent) to achieve effective distribution of hot air/steam and injected ZVI throughout the mixed soil column. A spare mixing tool of similar diameter also will be maintained on-site. In consideration of the documented soil consistency [hard (greater than 100 blows per ft) at the approximate 20 to 25 ft below grade depth interval], it is anticipated that "rock teeth" will be required on the mixing tool to facilitate penetration. A spare mixing tool of similar diameter also will be maintained on-site. The mixing rig will be capable of reaching outward from the toe of the crawler tracks two rows of overlapped column locations. The mixing rig will operate on mats that will provide stability, maintain vertically plumb mixing, and minimize contamination of drill rig tracks. The mixing rig will be capable of reaching outward from the toe of the crawler tracks (crane front) up to two rows of overlapped column locations. Prior to initiating drilling activities for a given column, the Kelly bar will be checked for verticality utilizing a survey level. This check will be done in two perpendicular directions prior to proceeding with any drilling work and once during the first pass. Results will be logged. The kelly bar vertical alignment will be controlled by adjusting the crane mats, drill platform, or the cables that suspend the turntable and/or by slightly booming up or down as necessary. The soil mixing equipment will be capable of achieving an average LDA ascent/descent rate of 1 to 3 ft per minute and an auger rotational rate of 6 to 10 revolutions per minute within the medium soil consistency range documented in the treatment zone.



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4.4.1.2 Hot air/steam generation and delivery system

Hot air will be generated by drawing ambient air though two Sullair (or approved equal) electrically powered air compressors capable of providing an airflow of 750 actual cubic ft per minute (acfm). A filter bank will be utilized in-line to remove entrained oil from the generated air flow. The compressors will be capable of a turndown ratio greater than 75%. Injection pressure, temperature, and flow will be monitored and controlled during operations. Hot air will be delivered to the subsurface at flow rates ranging from 200 to 400 actual air compressor capacity (acfm) and minimum temperature of 385°F at a maximum operating pressure of 150 pounds per square inch gauge (psig), with higher flow rates applied to higher observed VOC concentrations based upon field-based PID/FID VOC measurements after subtracting the methane values. Flow rate will be measured with an orifice plate connected to a Rosemount delta P instrument and monitored by the data acquisition system or approved equivalent.

The steam generating system will be comprised of two 32 diesel-powered steam boilers (one 400-horsepower (HP) and one 250-HP or approved equivalent) with the capability of producing steam and/or hot air at a minimum temperature of 385°F from a facility-supplied water source that has been staged on-site in a minimum of two 21,000 gal frac tanks to provide time for residual chlorine to dissipate to a concentration of 0.03 mg/L or less (to be evaluated utilizing a Hach field chemistry test or equivalent), prior to utilization as makeup water for steam or ZVI injection. If residual chlorine concentrations remain elevated following a 24-hour stabilization period, an alternative approach to provide removal of residual chlorine, such as diffused aeration of the makeup water within the frac tank to assist in acceleration of the natural volatilization of residual chlorine, may be utilized. At the maximum operating capacity, the boilers are expected to output a minimum of 10 million British thermal units per hour (MBTU/hr). It is anticipated that a minimum of approximately 10,000 gal of water per day will be converted to steam for injection and steam will be injected at flow rates ranging from 8,000 to 14,000 pounds per hour (pph) at a maximum operating pressure of 135 psig, with higher flow rates applied to higher observed VOC concentrations based upon field-based PID/FID VOC measurements after subtracting the methane values. Braided steel and rubber hose will transfer the steam from the boilers to the manifold and rubber hose will be utilized to connect the manifold to the drill stem (kelly bar). Steam injection flow rate, pressure, and temperature will be monitored and controlled during operations.

Boilers may be subject to EPA area source Maximum Achievable Control Technologies (MACT) standards; however, 40 *CFR* Part 63, Subpart JJJJJJ (area source boiler MACT) 63.11195(h) indicates that temporary boilers are not subject to this subpart. Based on the definitions of a temporary boiler provided in 40 *CFR* Part 63, Subpart JJJJJJ (area 63.11237), it has been interpreted that the boilers used in this remediation process meet the definition of temporary boilers and will not be subject to this regulation. Regarding greenhouse gas emissions, we interpret that the remedial equipment would meet the definition of "portable equipment" under 40 *CFR* Part 98, Subpart A and, therefore, would be exempt from greenhouse gas reporting requirements under this regulation.

4.4.1.3 Off-gas extraction and vapor conditioning system

As the mixing blade rotates and hot air and steam are injected in the soils, VOCs will rise to the surface through the annulus created by the soil mixing process and associated pressure gradient. The contaminants will be collected within a minimum 12-ft diameter steel shroud to provide capture of VOCs. The shroud will cover the ground surface around the boring location that is penetrated by the rotating kelly bar providing a minimum 12-ft diameter radius of influence for vapor collection. The shroud will be set to penetrate the surface to approximately 1-ft bgs. The shroud provides the ability to capture off-gases beyond the diameter of the 8-ft diameter drilling blades. A blower connected to the shroud will provide a vacuum on the shroud for vapor recovery and transfer to the VCS. The blower connected to the shroud

will generate an anticipated air flow rate of 600 to 1,500 standard cubic feet per minute (scfm) at an approximate operating vacuum of 30 inches of water. An applied shroud vacuum of 1 to 5 inches of water will be established prior to soil mixing and maintained throughout soil mixing activities at each boring location. Establishment of the shroud vacuum prior to soil mixing provides a mechanism to confirm that the shroud provides an effective seal around the auger borehole location.

The VCS will consist of a blower, liquid-vapor knock-out (KO)/demister tank, air filter, chiller, transfer pumps, and reheater/heat exchanger or equivalent. The vapor entering the shroud from the borehole annulus is expected to be saturated with water; therefore, the vapors initially will flow through a liquid vapor KO tank to remove large dirt particles and moisture. The vapors then will flow from the KO tank into a chiller unit used to cool the gas (typically to a temperature of less than 90°F). General VCS equipment specifications are included as follows:

- **Blower**—A centrifugal pressure blower rated for 1,800 cubic ft per minute at 31 inches total static pressure @13.4 BHP using a 15 hp 230-460/3/60 VAC totally enclosed fan cooled premium efficiency motor [for use with a variable frequency drive (VFD)]. A damper will be employed to control the pressure variations at the shroud due to varying flow losses because of variable duct length from one treatment area to another. National Electrical Manufacturers Association 4 rated VFD motor speed control rated for a 15 hp motor and 460 VAC/3 phase input from a generator (or approved equivalent).
- **Knockout tank**—The KO tank will consist of a 44-inch diameter by 72-inch high steel vessel (or approved equivalent) with hose connections for processing air in and out, a sludge drain port with gate valve, and a connection for feeding to a transfer pump. The KO tank will include three float switches for pump on/off control and a high water alarm.
- Chiller—The chiller unit will consist of a TRANE 70T [840,000 British thermal units per hour (BTU)/hr]) air cooled water chiller using FREON 22 (or approved equivalent). This unit will be capable of cooling the gas flow temperature from approximately 160°F to less than 100°F at a flow rate of 1,300 scfm. The heat exchanger will be an Aerofin Type Rf coil 34.9 inch by 25 inch, six-row with copper fins on 5/8 inch copper tubing with a galvanized steel case. The housing for mounting the coil, inlet filters, inlet and outlet connections will be 14 gauge galvanized steel. The drain pan will be 304 stainless, 14 gauge, with a 3/4 inch national pipe thread drain connection.
- Particulate Filter—Included in the chiller unit housing will be a 25 inch by 16 inch by 2 inch stainless steel mesh filter (F-101) for particulates (or approved equivalent).
- Condensate Pump and Discharge Pump—These pumps will be commercial off-the-shelf, 1/2 hp water pumps (or approved equivalent) for pumping out the collected water from the knockout tank and chiller condensate to the VOC water holding tank and to the Outfall 008 discharge.
- **Reheater**—The reheat unit along with the blower heat of compression will raise the temperature more than 12°F and reduce the relative humidity to less than 80%. The coil is housed in the same housing as the chilled water heat exchanger and is designed to produce 150,000 BTU/hr maximum using 180°F water from the boiler preheat tank. A hand valve on the upstream side of the reheater will control the water flow and subsequent heat capacity.

Condensate water generated by the KO tank chiller will be transferred and stored in a 21,000-gal frac tank(s) and treated with liquid-phase GAC and ion exchange resins (Purolite A530E or equivalent) to remove constituents of concern prior to discharge to a PGDP outfall (e.g., Outfall 008), in accordance with ARARs. Additionally, recovered condensate water from each frac tank will be analyzed for VOCs

and non-target/non-VOC contaminants, including PAHs, PCBs, radionuclides, and heavy metals, consistent with the Memorandum of Agreement for the Southwest Plume FFS (DOE 2010c), to establish whether additional treatment measures will be necessary prior to discharge. Cooled vapor will enter a reheater/heat exchanger to raise the off-gas temperature in order to reduce the off-gas relative humidity to less than 80% (thereby increasing the efficiency of the vapor-phase carbon adsorption system). Vapor then will flow through an air filter to remove fine particulates prior to entering vapor-phase GAC treatment systems. The VCS will be monitored and controlled during operations. Data that will be recorded from monitoring instruments on the VCS include pressure drop over the chiller/heat exchange unit, vapor temperature after chiller, and vapor temperature and relative humidity after the reheater.

4.4.1.4 Liquid treatment system (liquid-phase carbon adsorption and ion exchange)

Condensate water generated by the KO tank chiller will be transferred and stored in a 21,000-gal fractionation tank(s), which will be filled to a capacity not greater than 18,000-gal. The frac tanks will be enclosed and vents will be covered with vapor-phase carbon filters to prevent fugitive VOC emissions. It is anticipated that condensate water may contain VOCs and/or some non-target/non-VOC contaminants (such as PAHs, PCBs, radionuclides, and heavy metals), which will require treatment prior to discharge. The collected condensate water will be treated in a closed-loop recirculation treatment system consisting of 2 liquid-phase GAC and 2 ion exchange resin columns connected in series to remove constituents of concern prior to discharge to a PGDP outfall (e.g., Outfall 008) (in accordance with ARARs). The liquidphase carbon vessels will be utilized primarily for removal of VOCs, PAHs. and PCBs, if present in the condensate water. The ion exchange resin (Purolite A530E) will be utilized for removal/recovery of metals and radionuclides, if present in the condensate water. The GAC vessels will provide a total holding capacity of a maximum of 4,000 lb of virgin, liquid-phase GAC. The ion exchange resin columns will hold a maximum of 4,000 lb of Purolite A530E resin. Each vessel will be capable of treating a flow range of 40 to 60 gpm. Condensate water will be pumped via submersible pump capable of producing a flow rate of 50 gpm placed in the frac tank. Condensate water will be recirculated through the treatment system for a minimum of 24 hours (equal to four treatment volumes of collected condensate water). Following a 24-hour treatment period and prior to discharge, treated condensate water from each frac tank will be analyzed for VOCs and non-target/non-VOC contaminants, including PAHs, PCBs, radionuclides, and heavy metals, by the on-site laboratory facility on a 48-hour turnaround time basis. Laboratory analysis will establish whether additional treatment measures will be necessary or discharge may occur. If the treated condensate water has met the established treatment criteria for a PGDP outfall (e.g., Outfall 008), the treated effluent will be discharged accordingly. While laboratory results are pending, additional condensate water produced by the treatment system will be collected in a separate frac tank. The condensate water treatment system will be utilized for treating condensate water collected within other frac tanks while laboratory results are pending. The effectiveness of the treatment system will be evaluated based on the treatment performance data reported by the laboratory prior to discharge. If necessary, based on the findings of the laboratory data, the treatment system may be amended or modified, and spent media will be changed out to ensure that treatment objectives are being met prior to discharge to a PGDP outfall (e.g., Outfall 008).

4.4.1.5 Vapor treatment system (vapor-phase carbon adsorption)

Conditioned vapors exiting the VCS will be treated on-site utilizing a minimum of three 3,000-vapor-phase GAC adsorption vessels connected in series. At least one additional vessel will be maintained at the site in standby mode. The GAC vessels will provide a total holding capacity of a minimum of 9,000 lb of virgin, vapor-phase GAC and will be capable of treating an airflow range of 600 to 1,500 scfm. To monitor the GAC for breakthrough, the effluent from each GAC vessel will be monitored a minimum of twice daily during active operations using a PID, FID, or Draeger-Tubes. GAC vessel change out, if required, will occur when GAC breakthrough is documented, as indicated by an increase in initial GAC

vessel exhaust concentration to a level that is within 50% of the influent concentration, indicating that breakthrough has occurred in the initial GAC vessel. If an air exhaust measurement of approximately 50% of the influent measurement is detected, planning will begin for carbon replacement.

The results of the EVS-ES modeling using the RDSI soil results revealed a potential range of TCE mass within the source area of 1.4 gal to 29.3 gal. Based on a conservative range of total VOC contaminant mass in the SWMU 1 area ranging from 100 to up to 1,000 lb, and an assumed carbon adsorptive capacity and usage rate of 20% (20 lb VOCs/100 lb GAC) for an influent GAC relative humidity of 80%, the total mass of vapor-phase carbon to be utilized for off-gas treatment is estimated to be approximately 500 to 5,000 lb (indicating that the 9,000 lb or greater of vapor-phase GAC vessels in series provides adequate capacity).

For design purposes, it is assumed that 100% mass removal will be extracted in the vapor phase. Off-gas from the vapor-phase polishing system will be discharged to the atmosphere through a 15-ft tall by 6-inch diameter stack. Off-gas emissions will be monitored by a photoacoustic analyzer. The analyzer will communicate with a control system to notify operations personnel in the event of an exceedance of discharge criteria. The analyzer utilized will be an Innova 1412 or equivalent that is capable of measuring over 300 different gases including the 5 VOCs mentioned here. The Innova can measure up to 5 gas components and water vapor in each air sample. The analyzer will be calibrated and equipped with optical filters for speciation of the five contaminants of concern expected at SWMU 1(TCE, vinyl chloride, cis-1,2 DCE, trans-1,2 DCE, and 1,1 DCE) or as recommended by the analyzer manufacturer or authorized representative. The optical filters will supply a maximum detection limit of less than 1 ppm for each gas with a minimum sample integration time of 5 seconds. The analyzer will alarm at the control system panel to notify operations personnel in the event of an exceedance of discharge criteria and to discontinue mixing and vacuum operations. The air dispersion modeling results included in Appendix D indicate that a maximum exhaust pollutant concentrations (with an applied safety factor of 1.5) results in property boundary concentrations that are significantly lower than the off-site limits; thus, the system will be shut down manually before emissions reach the quantities that will exceed acceptable risk levels.

4.4.1.6 ZVI mixing and delivery system

A slurry mixture consisting of granular ZVI, water, and guar gum (to facilitate ZVI injection into the soil) will be prepared on-site and delivered on the final pass of the LDA at each boring location. Based upon a review of LDA soil mixing with hot air/steam and ZVI injection applications at Cape Canaveral Air Force Station, Florida, and former Offutt Air Force Base, Nebraska, it is anticipated that granular ZVI particle size will range from approximately 50 micron to 300 micron in diameter. To create this slurry mixture, ZVI will be suspended in the slurry at a rate of approximately 5 to 7 lb of ZVI per gal of water, and guar gum will be mixed at a rate of approximately 60 to 80 lb per 1,000 gal of water. The actual quantity of guar gum and water may be adjusted (within the range provided), during field preparation to create a site-specific mixture, which adequately suspends the ZVI and achieves the optimal pumping viscosity. ZVI preparation and delivery equipment will consist of mixing tanks of a minimum of 500 gal each, a high-shear slurry mixer (5 yd³ High Shear Lightning Mixer or approved equivalent), a progressive cavity pump (L-12 Moyno pump or approved equivalent), and a high viscosity flow meter (Halliburton Turbine Water flow meter or approved equivalent). It is anticipated that up to approximately 2,000 gal of water per day will be utilized in the preparation of the ZVI/guar slurry.

4.4.1.7 Real-time data collection and monitoring system

The effective application of the *in situ* LDA soil mixing with hot air/steam and ZVI injection system involves real-time data collection and monitoring to allow for field-based decision processes regarding the following:

- Depth penetration rate, auger rotational rate, torque, and down-hole temperature of LDA soil mixing;
- Injection temperature, pressure, and flow rate of hot air and steam;
- Temperature, pressure, flow rate, relative humidity, and VOC concentrations in the vapor extraction and conditioning systems;
- Injection temperature, pressure, and flow rate of the ZVI slurry injection system; and
- VOC concentration of the vapor-phase treatment system effluent.

Operational parameters (frequencies of data collection, monitoring, and associated reporting) of the previously mentioned monitoring protocol are discussed throughout applicable portions of Section 4. Gas samples from the process streams will be collected from the vapor extraction system for analysis by a PID/FID, after methane subtraction and/or a GC. GCs will be used to detect, speciate, and quantify target analytes from the treatment process off-gas. PIDs/FIDs will be used to continuously monitor the vapors produced by the treatment process. If the PID/FID data monitoring equipment becomes saturated due to the presence of high VOC concentrations and/or DNAPLs present in the subsurface, adjustments will be made in the field to compensate by adjusting the ascent/descent rate of soil mixing, recalibration of the PID/FID equipment to a higher calibration standard to facilitate measurement, and/or introduction of additional bleed air to the system to provide for the adequate real-time monitoring of VOCs. Data from the PIDs/FIDs and GCs will be utilized to evaluate VOC trends in depth, concentration, and location of contamination mass requiring focused treatment (i.e., additional mixing time, higher application of ZVI slurry mixture within a specific interval, etc.). Real-time monitoring of the point of atmospheric emission will be monitored with a photoacoustic analyzer. This monitoring will trigger an alarm notification to the equipment operator, which will trigger a manual shutdown of remedial equipment.

The Data Acquisition System will consist of the two SRI GCs 8610, and field instruments served by three Automation Direct 205 programmable logic controllers that provide data input to a personal computer (PC) (or approved equivalent). The data will be monitored and recorded in real time. The data will be displayed and recorded in engineering units in real time. PC application software will display, in real time, selected parameters and will record at a selected rate of 6 times a minute. The recorded data will be viewed and saved in a Microsoft Excel spreadsheet.

4.4.2 Implementation Sequence

The LDA borings will be established based upon an overlap spacing ranging from 0% to 17.5% (representing complete overlap with no interstitial space) overlap. Figure 5 presents the LDA boring layout. The protocol for establishing overlap spacing is discussed in greater detail in Section 4.2 [generally, reduced overlap spacing will be employed around the periphery of the treatment cell (concurrent with lower VOC concentrations), and increased overlap spacing (concurrent with higher VOC concentrations) will be employed internal to the treatment cell]. Prior to full active remedial implementation, at least two test cells will be performed during implementation in the SWMU 1 treatment area to simulate active remediation, to ensure the system is functioning efficiently as designed, and to troubleshoot problems or issues that developed prior to active remediation. The test treatment cells will be conducted in an area of highest detected concentration and in an exterior cell of anticipated lowest concentrations at the site. The information collected during the conduct of test cells will be used to discuss potential modifications to treatment decision criteria, if needed. Following test cell implementation, the test cell evaluation will include testing of the vapor condensate and off-gas discharges to help ensure that these are being handled appropriately. The sequencing of soil mixing and

treatment locations will be conducted such that the perimeter cells are treated first and subsequent locations will move inward in concentric circles, generally targeting lower concentration areas prior to targeting higher concentration areas and creating a perimeter ZVI slurry enhanced ring, which would provide treatment as a best management practice to potential groundwater displaced outward during implementation.

4.4.2.1 Description of soil mixing and hot air/steam delivery procedure

Soil mixing with hot air/steam delivery will be conducted at each cell location in treatment passes (a pass is considered to be one movement of auger through the entire thermal treatment depth of the cell in one direction, up or down). The thermal treatment depth will begin approximately 5 to 6 ft below the surface (2 ft below natural grade based on surficial scraping) for worker safety purposes and will continue to the base of the treatment cell [60 ft below the surface (2 ft below natural grade based on surficial soil removal)]. Data collected from off-gas analysis from the PIDs/FIDs and GCs during the first hot air/steam treatment pass will be monitored to aid in the real-time decision making process and to evaluate results against treatment criteria, completion criteria, and iron dosage quantities presented in Figure 6.

The hot air/steam treatment pass will be initiated when the auger is drilled from the ground surface to the starting thermal treatment depth for the zone of treatment at a typical descent rate of 1 to 3 ft per minute and 6 to 10 revolutions per minute. Additionally, if warranted based on field conditions, a drilling mud (EZ Mud® or approved equivalent) may be utilized as a cutting fluid to assist in auger advancement in the formation, to provide flexibility to the LDA contractor in case the drilling penetration is impeded based on soil conditions. A field condition that could warrant using the drilling mud would be encountering, while drilling, a very dense layer or soils with a high friction coefficient where the injection of a drilling mud could assist in achieving LDA penetration. The drilling mud has no negative effect on thermal treatment processes. The drilling mud also has no impact on the ZVI injection process because the mixing blade provides the mechanism for distribution within the soil column. It is noted that drilling mud was applied in the remedial implementation at the Offutt Site, and a negative impact on the overall project performance at that Site was not observed or perceived. The GCs will process samples continuously at a frequency of approximately every 2 minutes for analysis; however, this sample processing rate may be reduced if the auger ascension/descension rate is reduced to less than 1 ft/min.

The PIDs/FIDs continuously will analyze and process the off-gas total VOC concentration. Once the auger reaches the target starting depth (anticipated to be 5 to 6 ft bgs), the steam valve will be opened, steam will enter the treatment column, and the auger will continue descent to the desired finishing depth, which is anticipated to be 60 ft bgs (62 ft below original land surface because the upper 2 ft will be excavated prior to LDA operations). The protocol for evaluating the number of treatment passes which will be completed at each treatment cell will be based on the peak TCE concentration in UCRS soils and in the upper RGA (HU4) evaluated by the data collection system during the first treatment pass. Once the peak off-gas VOC values are collected from the first treatment pass, the cell treatment protocol will be characterized into one of three categories, which are described as follows.

- (1) Low VOC concentration target threshold (less than 100 ppm response)—Requires a minimum of one complete thermal pass; a shroud temperature of 160°F maintained throughout the treatment pass; and monitoring of VOC concentrations to ensure that they are below the established low target threshold.
- (2) Greater than the low target on the first treatment pass, but less than the low target treatment threshold on second treatment pass—Requires a minimum of two complete thermal passes; a shroud temperature of 160°F maintained throughout the complete final pass; and monitoring of VOC concentrations to ensure that they are below the established low target threshold.

(3) Greater than the low target on the first and second treatment passes—Requires a minimum of four complete thermal passes and a shroud temperature of 160°F maintained throughout the entire complete final pass. Depth-focused passes could be implemented after the second pass; however, the final pass must have been completed from total treatment depth to top of target treatment interval, and to obtain completion criteria of an FID concentration, after subtracting the methane value, less than 80% of the highest peak FID value obtained during the first pass, or VOC concentrations less than low target threshold, or reach a maximum hot air/steam treatment time of 240 minutes following the completion of at least four complete thermal passes. Additional treatment time may be employed.

The LDA/steam/ZVI treatment protocol is presented graphically in Figure 6. Please note that the intention of the LDA/steam/ZVI treatment protocol depicted in Figure 6 has not been presented with the intention to provide a rigid framework that will apply to each and every case that may be encountered during field implementation, but rather to describe the general protocol and procedures for what are anticipated to be representative of the most likely scenarios encountered during implementation. The field team and equipment operator will reserve the flexibility of field-based judgment to alter the Treatment Protocol only for the overall benefit and success of project implementation. If alterations to the treatment protocol are to be made during project implementation that result in relaxed treatment criteria from those described above, they will be discussed first with the remedial team (to include representatives from EPA, Kentucky KDEP, DOE, and DOE design team representatives). If residual VOCs remain following the thermal treatment protocol, they will be addressed further through the introduction of the ZVI slurry mixture, which will be concentration weighted based on PID/FID data, as described in Section 4.4.2.2. The low VOC concentration target threshold value is based upon the field-screening PID response data from the RDSI boring locations generally corresponding to low VOC concentrations in soil (less than 70 μ g/kg TCE).

4.4.2.2 Description of ZVI dosing

A slurry mixture consisting of granular ZVI, water, and guar gum (to facilitate ZVI injection into the soil) will be delivered based upon a percentage mass of ZVI to mass of soil application. Decisions will be based upon monitoring data collected during hot air/steam mixing phase will be used to adjust the ZVI dosing concentration. The amount of ZVI delivered to an LDA boring location will be established based on the observed PID/FID response value of VOCs from the first thermal treatment pass according to the following criteria:

- If a maximum PID/FID reading of 1,000 ppm or less (after subtracting the methane value) is observed on the first thermal treatment pass, an application of 0.5% ZVI will be applied.
- If a PID/FID reading of 1,000 to 5,000 ppm (after subtracting the methane value) is observed on the first thermal treatment pass, an application of 1.0% ZVI will be applied.
- If a PID/FID reading exceeding 5,000 ppm (after subtracting the methane value) is observed on the first thermal treatment pass, an application of 1.5% ZVI will be applied.
- Based upon RDSI soil sampling results, the area within the greater than 10,000 µg/kg TCE isoconcentration contour area will be treated with a default application of no less than 1.5%, but not greater than 2% ZVI, regardless of PID/FID response. This range of concentration has been presented based on practical limitations to injection of 2% ZVI observed at other sites.

The ZVI dosing concentration will be measured as a percentage by weight of the column of soil being treated. The ZVI dosing strategy is consistent with the LDA soil mixing projects successfully

implemented to treat TCE/DNAPL source areas at Cape Canaveral Air Force Station and former Offutt Air Force Base. The LDA/Steam/ZVI Treatment Protocol is presented graphically in Figure 6. Please note that the intention of the LDA/Steam/ZVI Treatment Protocol depicted in Figure 6 has not been presented with the intention of providing a rigid framework that will apply to each and every case that may be encountered during field implementation, but rather to describe the general protocol and procedures for what is anticipated to be representative of the most likely scenarios encountered during implementation. The field team and equipment operator will reserve the flexibility of field-based judgment to alter the Treatment Protocol only for the overall benefit and success of project implementation. If alterations to the treatment protocol are to be made during project implementation that result in relaxed treatment criteria from those described above, they will be discussed first with the remedial team (to include representatives from EPA, KDEP, DOE, and DOE design team representatives).

During the LDA ZVI slurry injection pass, the desired quantity of ZVI-guar slurry mixture for each cell will be transferred to the soil mixing auger by a pump. The slurry then will travel down the kelly bar and will be injected into the subsurface at a flow rate of approximately 25 gal per minute (gpm) through the rotating auger to distribute the iron throughout the column. Water will be used to flush the iron-guar slurry from the injection plumbing into the column during the final pass to ensure that the entire quantity of iron required is injected into the column. The vertical treatment of ZVI application will extend from the surface of the treatment cell (approximately 2 ft below natural grade based on surficial scraping) to the base of the treatment cell depth (approximately 62 ft below natural grade). This will not coincide with thermal treatment, which will commence at a depth of 5 to 6 ft bgs (7 to 8 ft below natural grade based on surficial scraping) which is a necessary measure for worker safety.

5. CONSTRUCTION REQUIREMENTS

5.1 CONSTRUCTION EQUIPMENT

Construction-type equipment will be required to deliver and stage equipment on-site and to perform *in situ* LDA soil mixing with hot air/steam and ZVI soil mixing and treatment activities. These likely will include, but not be limited to, these items:

- Crawler crane (200-ton crawler crane such as a Manitowac 777 or approved equivalent) or heavy equipment capable of delivering required torque and soil mixing requirements to achieve target depth
- Flatbed truck
- Storage units (e.g., Conex boxes/Sealand containers)
- Drill turntable (Hain or approved equivalent)
- Excavator (CAT 322 or approved equivalent)
- Loader (Cat 928 or approved equivalent)
- High reach man lift (High Reach-Bil Jax 45XA—4WD or approved equivalent)
- 21,000-gal frac tank(s) for supply water staging and KO vessel water storage (Adler 21,000 closed top frac tank or approved equivalent)

- Telescopic forklift (CAT 3RN01724 or approved equivalent)
- Equipment storage trailer

The mixing rig will be mobilized to the site with multiple tractor-trailer components, as necessitated by the vendor-specific equipment. A crane will be required to unload the tractor-trailers and place the component parts of the mixing rig in the site staging area for rig assembly.

5.2 *IN SITU* DEEP SOIL MIXING WITH HOT AIR AND STEAM TREATMENT AND ZVI AMENDMENT SYSTEM EQUIPMENT

Following is a list of typical equipment required for the extraction and treatment systems. The equipment required to achieve project objectives shall be based upon vendor-specific components proposed to achieve project objectives. Typical equipment includes the following:

- Mixer
- Liquid mixing tanks
- 400- hp or equivalent boiler generating steam at 385°F
- Liquid transfer pumps
- Hollow kelly bar (70-ft long) and swivel
- 8 ft auger
- Containment shroud (minimum 12-ft diameter)
- Vapor conditioning system, 70-ton chiller, or equivalent, with blower unit
- Process knockout tank
- Heat exchanger
- SVE Blower capable of 600 to 1,500 scfm at an approximate operating vacuum of 30 inches of water
- Data acquisition system
- Three 3,000 lb or equivalent vapor-phase carbon adsorption vessels
- Power generators

Additional detail related to equipment specification or approved equivalents is provided in Section 4.4.1, Equipment Summary, and associated subsections.

5.3 ELECTRICAL REQUIREMENTS

Electrical components needed for the in situ soil mixing and treatment system will require 3-phase power for the operation of air compressor, pumps and blowers, mixing equipment, instrument panels and controls, electronic instruments, and thermocouples, etc. Approximately 750 kilovolt amperes (kVA) will be required to operate the *in situ* LDA soil mixing with hot air/steam and ZVI injection system (this may vary depending on contractor-specific equipment utilized to achieve the site treatment objectives), which will be obtained through an on-site generator to be supplied by the remediation vendor.

5.4 WATER REQUIREMENTS

It is anticipated that at least 12,000 gal of water will be utilized by the *in situ* soil mixing and treatment system per day of operation. Water will be utilized for the generation of steam (approximately 10,000 gal per day) and for mixing the ZVI slurry (approximately 2,000 gal per day). Water will be

obtained from the fire hydrant located at the southeast intersection of 4th Street and Tennessee St. (see Figure 8) and will be hard piped to the treatment area via culverts that run beneath the streets and railroad tracks. Water will be collected and staged on-site in a minimum of two 21,000-gal frac tanks to provide time for residual chlorine to dissipate to a concentration of 0.03 mg/L or less (to be evaluated utilizing a Hach field chemistry test or equivalent) prior to utilization as makeup water for steam or ZVI injection. If residual chlorine concentrations remain elevated following a 24-hour stabilization period, an alternative approach to provide removal of residual chlorine may be utilized. Additionally, Water entering steam boiler units may require conditioning using water softening ion exchange units to prevent scaling of the units. If needed, water will be recirculated through weak acid cation exchange units (Marlo, Inc., MGT-300-2 Twin Alternating Softener System or approved equivalent) until field measurements of the water hardness (based on Hach field chemistry) achieve limits acceptable to the remediation equipment vendor. The need for water softening units will be determined by the LDA soil mixing contractor based upon operations at other sites and experience with the steam boiler units owned and operated by the contractor.

5.5 SITE PREPARATION

Site preparation also may include siting of an operations trailer, site surveying, utility locating, clearing and grubbing, grading, and leveling. Additional activities for site preparations will include, but are not limited to, removing the top 2 ft of surface soil to remove potential contaminants that may be present and to facilitate soil mixing to desired depth, stockpiling the excavated soil, and then respreading the excavated soils after mixing is complete. These nonvolatile contaminants will not be treated by the soil mixing technology and will be addressed consistent with the approach discussed previously in Section 1.5, "Sequencing with Other Remedies." Liner material such as polyethylene or Hypalon[®] will be placed under and over the stockpiled soil until completion of the RA. Figure 8 presents a conceptual LDA equipment layout that includes the stockpiling area. During excavation of the top 2 ft of soil, water sprays will be used as needed to prevent the generation of fugitive dust.

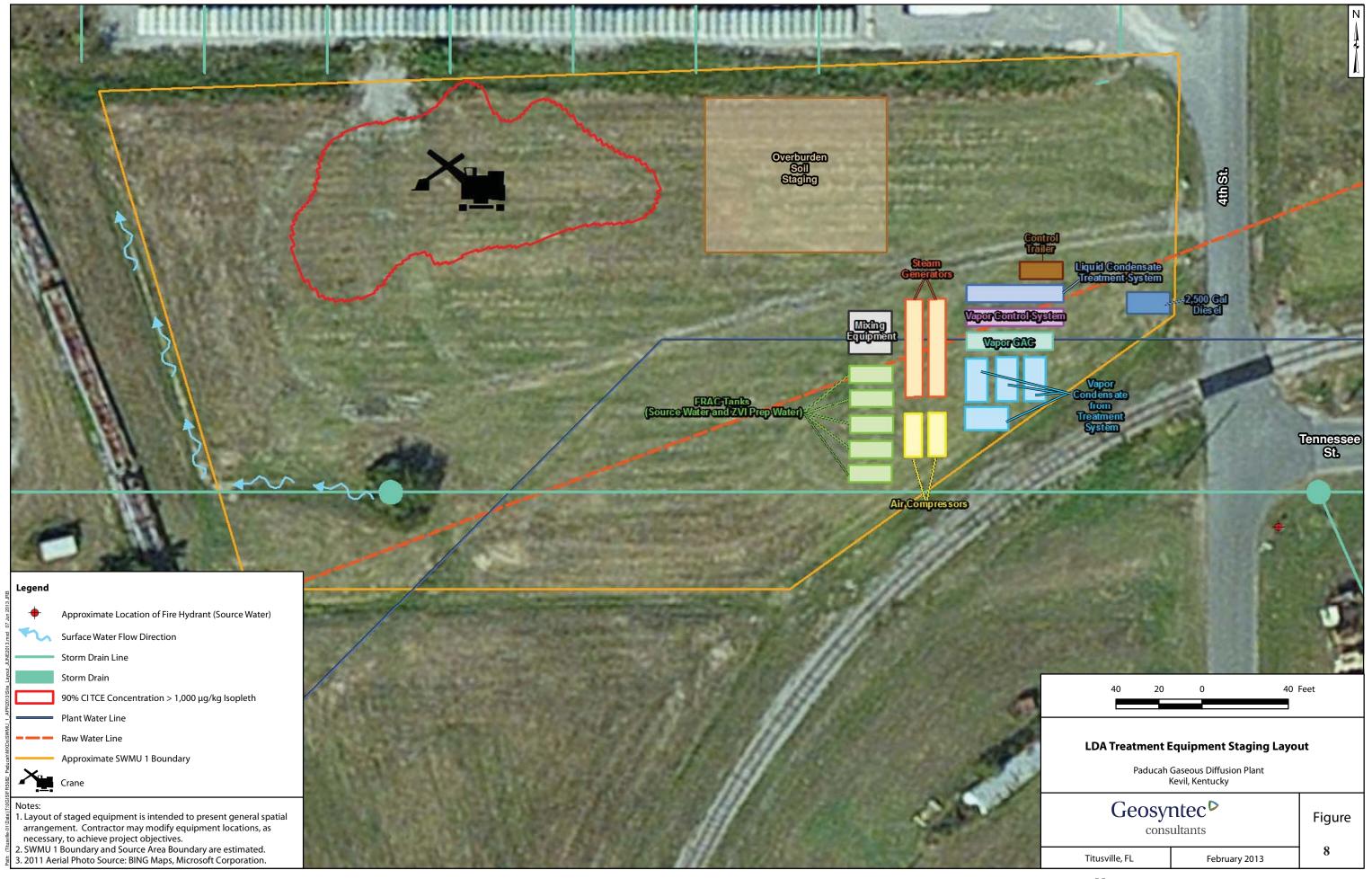
The excavated soil will be respread on the area that has been soil mixed. The replacement of the soil will be performed within one year of completion of the soil mixing operation. The soil placement will be delayed for two reasons:

- 1. The soil will be more stable to heavy equipment traffic, which will be the most efficient way of placing the soil, and
- 2. The one-year window will allow the performance of the postremedial soil monitoring to be performed without having to push direct-push technology tooling through the extra 2 ft of soil.

A layer of Visqueen or similar material will be placed at the base of the replaced soils to provide a marker bed between the mixed soil and the unmixed soil. If remedial efforts for the Soils OU have progressed in the selection of a remedial measure prior to soil replacement, and it is determined that use of the Visqueen will be detrimental to the potential Soils OU RA, the placement of the Visqueen will not be performed. Should the placement be cancelled, the FFA parties will be notified of the change to the in design to support the future Soils OU actions.

5.6 PERMITTING

Site-specific permits will be required for the implementation of the RA utilizing the selected *in situ* soil mixing and treatment system. Applicable site-specific permits include the following:



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- Excavation/penetration permits
- Lockout/tagout permits
- Hot work permits

The use of best management practices related to storm water management is required for the construction within the SWMU 1 area because PGDP has a Kentucky Pollutant Discharge Elimination System permit. Accordingly, it is anticipated that silt fence will be installed in the site construction area as a component of a site-specific stormwater best management practice.

6. SAMPLING AND MONITORING

6.1 SAMPLING AND MONITORING DURING SOIL MIXING

During operation, on-site personnel will monitor the soil mixing and treatment system activities to assess the performance and progress of the remedial action. Systems will be designed to accommodate operational sampling and real-time monitoring for parameters, such as the following:

- **Subsurface Temperatures.** Monitored continuously using a combination of evaluation of vapor shroud off-gas temperature and daily review of auger mixing blade thermocouple data. Subsurface temperatures will be documented for each soil mixing location.
- **VOC Concentrations in Recovered Vapor.** Monitored continuously during soil mixing at each boring location with PID/FID recorded continuously with depth. GCs will continuously process samples at a frequency of approximately every 2 to 5 minutes for analysis during soil mixing activities. Documentation of PID/FID response with depth (per treatment pass) and GC data (every 2 to 5 minutes) will be collected for each soil mixing location.
- VOC Concentrations in the Worker Breathing Zone. Due to the concentrations of VOCs present and the potential for release into the breathing zone as a result of the soil mixing activities, real-time air monitoring will be conducted during the course of all intrusive work associated with soil mixing consistent with the requirements of the project-specific Health and Safety Plan for the remedial action.
- Shroud Extraction Vacuum, Temperature, and Flow Rate. Continuous monitoring and recording of shroud vacuum at each boring location to document vacuum requirements achieved. Continuous monitoring of shroud temperature and air flow rate and documentation at each boring location that temperatures meet criteria and that flow rate from shroud exceeds air injection rate, as required.
- Compressed Heated Air/Steam Delivery Pressure, Temperature and Flow Rate. Continuous monitoring at each auger location to document heated air/steam delivery pressure, temperature and flow rate. Documentation at each boring location to include information on quantities delivered, confirmation of compressed heated air/steam and documentation at each boring location to document vacuum requirements achieved. Continuous monitoring of shroud temperature and air flow rate and documentation at each boring location that temperatures meet criteria and that flow rate from shroud exceeds air injection rate, as required.
- **ZVI Injection Quantity, Temperature, Pressure, and Flow Rate.** Continuous monitoring at each auger location to document ZVI mass applied, temperature, pressure, and flow rate. Documentation at

each boring location to include information on quantities delivered, temperature, pressure, and flow rate during delivery.

- Vapor-Phase Effluent Discharge Flow Rate and VOC Concentration. Monitoring of vapor phase flowrate and VOC concentration and monitoring of vapor-phase carbon for efficiency and loading.
- VOC Concentration in Condensed Liquids from the Vapor Stream. Fluid sampling of condensed liquids.
- PCB, PAH, Radionuclide, and Heavy Metals. Concentration in a subset of condensed liquids from the vapor stream and vapor-phase effluent for each frac tank prior to release.
- Heat Exchanger Air Temperatures and Relative Humidity. Recorded and documented for each auger boring location.
- Vapor-Phase Effluent Discharge Temperature, Flow Rate, and CVOC Concentration. Monitor vapor phase flow rate and VOC concentration and monitoring of vapor-phase carbon for efficiency and loading. Measurements of discharge temperature and flow rate will be recorded by the Data Acquisition System at a rate of 6 times per minute. To monitor the GAC for breakthrough, the effluent from each GAC vessel will be monitored daily during active operations using a PID or FID, after methane subtraction. Additionally, off-gas emissions will be monitored by a photoacoustic analyzer. The analyzer will communicate with a control system to notify operation personnel in the event of an exceedance of discharge criteria. The set point at the stack that will cause the vapor extraction and treatment system to shut down will be the maximum exhaust pollutant concentrations (with an applied safety factor of 1.5) as presented in Appendix D, Table D.4.

6.2 SAMPLING AND MONITORING POSTREMEDIAL ACTION

Following the cessation of active remedial operations with *in situ* soil mixing with hot air/steam and ZVI injection, postremedial performance monitoring and sampling will be conducted to assess the performance of the remedial action and to support the five-year assessment period to evaluate remedial performance against the established objectives. Given the potential that residual TCE contamination may remain following soil mixing with steam injection, the addition of ZVI is used as polishing measure. The residual contaminant concentrations are expected to persist until such time that movement (based upon flow and/or diffusion) facilitates contact between the contaminant and the ZVI, thereby allowing the contamination to undergo chemical reduction. Field conditions also will have changed as a result of the soil mixing and injections. The field conditions following the treatment are expected to be as follows:

- Soil will be unstable due to mixing operations and destruction of soil structure,
- Increased water content resulting from hot air/steam injection may result in decreased density and soil strength, and
- Soil temperatures will be elevated due to injection of steam/hot air which will increase worker health and safety concerns.

Because of these field conditions and subsurface conditions, the implementation of postremedial sampling and monitoring will be delayed by six months following the completion of soil mixing. The requirements for the postremedial work will be documented in a Postremedial Sampling and Analysis section of the Remedial Action Work Plan (RAWP) with specifics on boring approach, locations, sampling,

contaminant analysis, and the collection of information necessary to complete the required five-year assessments. The areas to be evaluated generally will include the following:

- Postremedial soil sampling for VOCs and levels and distribution profiles in mixed and unmixed areas:
- Installation of postremedial MWs to monitor the progress of contaminant reduction in the RGA groundwater following the mixing process and placement of the ZVI;
- Postremedial soil temperature evaluation; and
- Postremedial evaluation of soil homogeneity and ZVI distribution.

Following completion of the soil mixing process, the previously excavated surface soils will be respread to bring the ground surface back to grade with the surrounding unmixed area. The soils from the surface to a depth of 10 ft contained in the mixing area will require recharacterization due to being disturbed by the mixing process. DOE intends to recharacterize those soils as part of the Soils OU at the appropriate time in the future.

6.2.1 Posttreatment Sampling and Analysis

Following cessation of active remedial operations with *in situ* soil mixing with hot air/steam and ZVI injection, monitoring will be conducted to assess the near-term performance of the RA and to support the required CERCLA Five-Year Reviews.

Posttreatment sampling and analysis are intended to achieve three main goals:

- 1. Assessment of the heating of the subsurface,
- 2. Assessment of the placement of ZVI for continued VOC reduction, and
- 3. Assessment of the success of deep soil mixing to achieve the primary project goal of reduction of VOC concentrations to the RA cleanup levels in the treated source zone.

In addition, posttreatment actions will include the installation of upper RGA wells at the perimeter of the treated source zone to monitor the progress of contaminant reduction in the RGA groundwater following soil mixing. It is expected that a reduction in the VOC contaminant concentrations in the RGA groundwater over time after the RA is indicative of supporting Goal 3.

In the area of the treated source zone, soil temperatures may be significantly elevated due to injection of steam/hot air. In addition, the soil may be inherently unstable because soil mixing will destroy soil structure and hot air/steam injection may result in decreased soil density and strength. These subsurface conditions require that the implementation of posttreatment sampling and installation of MWs will be delayed by six months following the completion of soil mixing. The delay is advantageous because contaminant concentrations may remain elevated until the guar carrier for the ZVI degrades, allowing the VOC contamination to be reduced by the ZVI.

¹ The VOCs of interest to this remedial action are 1,1-DCE; *cis*-1,2-DCE; *trans*-1,2-DCE; TCE; and vinyl chloride. VOC samples will be analyzed using EPA SW-846 Method 8260.

6.2.2 Soil Sampling

The RDSI for SWMU 1 included soil sampling and VOC analysis in 22 locations to determine the areal extent and depth of the source zone. These VOC analyses along with other SWMU subsurface soil VOC analysis provide a baseline for evaluating the effectiveness of the remedial action in reducing the VOC concentrations in the treated areas to the cleanup levels. The posttreatment characterization fieldwork will duplicate the collection of VOC contaminant concentrations in the UCRS soils by twinning the boring locations and collecting samples. The samples will be collected using the same approach used in the RDSI. The project then will be able to evaluate how effective the soil mixing for remedial action was at reducing the VOC contaminant concentrations in the treatment area. The posttreatment characterization fieldwork will include continuous logging of soil conductivity and temperature and sampling of soil borings to the total depth of mixing in 11 of the original RDSI soil boring locations (Figure 9). Eight of the soil borings will be located within the treated source zone, and 3 of the soil borings will be located on the perimeter. These locations (see Table 5) are representative of both the range of VOC contamination and the areal extent of the treated source zone.

A direct push technology rig equipped with an electrical conductivity probe and a thermocouple will provide the continuous logs of electrical conductivity and temperature of the soil column throughout the depth of the treated source zone. These logs will support assessments of the vertical distribution of ZVI and the residual heat in the treated source zone. The soil sampling to support the posttreatment assessment will remain consistent with the data quality objectives (DQOs) and Quality Assurance Project Plan (QAPP) developed for the RDSI. The direct push technology rig will be used to sample soils within the treated source zone and at perimeter locations, with similar methods used during the RDSI. Analyses of these soil samples will support an assessment of the reduction of VOC levels within the treated source zone and verify the distribution of ZVI.

² ZVI is significantly more electrically conducted than native soil. Any significant inhomogeneity of ZVI distribution will be apparent on the electrical conductivity log.

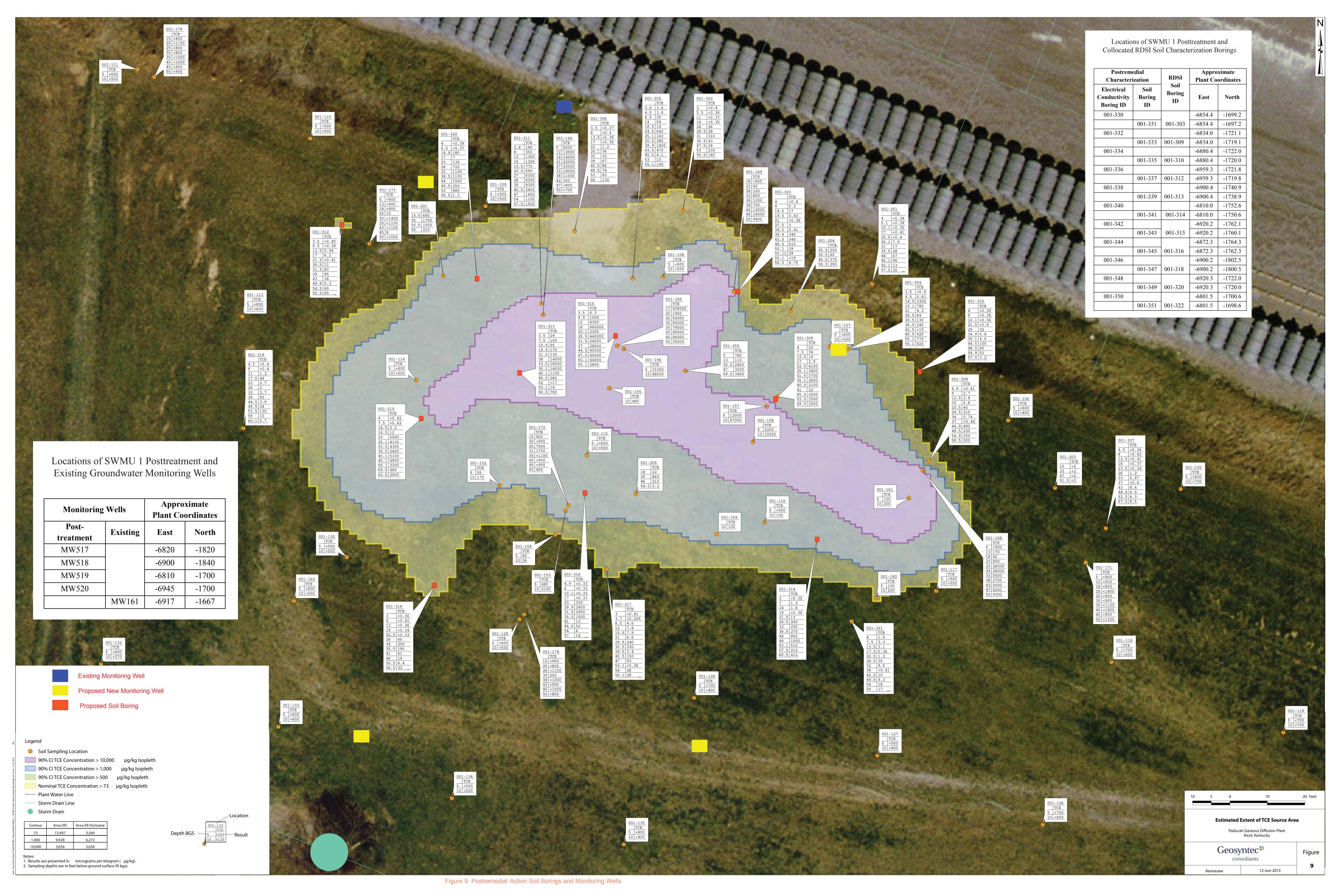


Table 5. Locations of SWMU 1 Posttreatment and Collocated RDSI Soil Characterization Borings

Postremo Characteri		RDSI		ximate ordinates
Electrical Conductivity Boring ID	Soil Boring ID	Soil Boring ID	East	North
001-330		001-303	-6854.4	-1699.2
	001-331	001-303	-6854.4	-1697.2
001-332		001-309	-6834.0	-1721.1
	001-333	001-309	-6834.0	-1719.1
001-334		001-310	-6880.4	-1722.0
	001-335	001-310	-6880.4	-1720.0
001-336		001-312	-6959.3	-1721.8
	001-337	001-312	-6959.3	-1719.8
001-338		001-313	-6900.4	-1740.9
	001-339	001-313	-6900.4	-1738.9
001-340		001-314	-6810.0	-1752.6
	001-341	001-314	-6810.0	-1750.6
001-342		001-315	-6920.2	-1762.1
	001-343	001-313	-6920.2	-1760.1
001-344		001-316	-6872.3	-1764.3
	001-345	001-310	-6872.3	-1762.3
001-346		001-318	-6900.2	-1802.5
	001-347	001-318	-6900.2	-1800.5
001-348		001 220	-6920.3	-1722.0
	001-349	001-320	-6920.3	-1720.0
001-350		001-322	-6801.5	-1700.6
	001-351	001-322	-6801.5	-1698.6

6.2.3 Monitoring Well Construction and Sampling

Placement and Construction of RGA Monitoring Wells: MW161 is an RGA MW located immediately downgradient of the treated source zone, screened over the interval 78–83 ft bgs (elevation 289 to 294 ft amsl). (The HU5 gravel interval of the RGA extends over the approximate elevations of 270 to 310 ft amsl.) Previous sampling and analysis of MW161 documents dissolved TCE levels between 1,000 and 2,000 μ g/L since 2005. This RA is expected to reduce the transport of dissolved VOCs to the RGA and to result in declining TCE levels in MW161.

To provide for a broader and continuing assessment of future dissolved VOC levels in the area of the treated source zone, four MWs will be installed in the top of the HU5 gravel interval of the RGA as part of the posttreatment field sampling efforts (two upgradient of the treated source zone and two downgradient) (Figure 9). Table 6 provides the geographic location for the MWs to be installed. The four

MWs will be constructed with 5-ft length screen (screened approximately 65–70 ft below the original average soil grade; well screen elevations of 302.5 to 307.5 ft amsl). Each of these wells will be equipped with dedicated sampling pumps. Trends in dissolved VOC levels in MW161 and the four wells to be installed will be criteria for future assessment of this SWMU 1 RA until cleanup levels are met in the UCRS soils.

Sampling Analysis and Schedule: The RDSI for SWMU 1 included groundwater sampling and analysis in MW161 to assess preremediation VOC levels and indicators of VOC biodegradation activity. The focus of near-term monitoring as part of the posttreatment action will be to assess the decline in dissolved VOC levels directly resulting from soil mixing and the degradation of VOCs associated with the injection of steam/hot air and ZVI. Groundwater sampling to support the posttreatment assessment will remain consistent with the DQOs and QAPP developed for the RDSI. An assessment of the level of biodegradation activity may be of interest in the future, if follow-on RA is required.

To assess the potential near-term decline in VOC levels in the MWs, groundwater samples will be collected for VOC analysis on a quarterly basis for a one-year term following construction of the MWs and will be collected semiannually during the second year. Subsequent monitoring frequencies will be dictated by the site's Environmental Monitoring Plan, which is updated annually in compliance with DOE Order 450.1A. The continued sampling under the Environmental Monitoring Plan also will provide the necessary data to support the preparation of five-year reviews required under CERCLA.

Table 6. Locations of SWMU 1 Posttreatment and Existing Groundwater Monitoring Wells

Monitoring	Approximate Plant Coordinates		
Posttreatment	Existing	East	North
MW517		-6820	-1820
MW518		-6900	-1840
MW519		-6810	-1700
MW520		-6945	-1700
	MW161	-6917	-1667

7. DATA MANAGEMENT

A project-specific data management and implementation plan will be included in the RAWP.

8. HEALTH AND SAFETY

A general health and safety plan overview will be included in the RAWP and a project-specific health and safety plan will be developed for field implementation.

9. WASTE MANAGEMENT

The sitewide Waste Management Plan (PAD-PLA-ENV-001) will be the basis for all waste management activities. Any deviations from this sitewide plan will be documented in the project-specific RAWP.

10. REFERENCES

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- DOE 2010b. Remedial Design Support Investigation Characterization Plan for the C-747-C Oil Landfarm and C-720 Northeast and Southeast Sites at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky (Draft in Progress), U.S. Department of Energy, Paducah, KY, July.
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- DOE 2012b. Remedial Design Work Plan for Solid Waste Management Units 1, 211-A, and 211-B Volatile Organic Compound Sources for the Southwest Groundwater Plume at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky, DOE/LX/07-1268&D2/R1, U.S. Department of Energy, Paducah, KY, April.

- DOE 2012c. Soils Operable Unit Remedial Investigation Report at the Paducah Gaseous Diffusion Plant, Paducah, Kentucky, DOE/LX/07-0258&D2, U.S. Department of Energy, Paducah, KY, September.
- Krige, D.G. 1951. "A Statistical Approach to Some Basic Mine Valuation Problems on the Witwatersand," Journal of Chemical Metallurgical and Mining, South Africa.
- USAF 2007. Corrective Measures Implementation Report Security Police Confidence Course (Facility 18003) Solid Waste Management Unit C091, Cape Canaveral Air Force Station, Florida, U.S. Air Force Space Command, Volume 1, May.
- USAF 2008. Corrective Measures Implementation Report Ordnance Support Facility (Facility 1381) Solid Waste Management Unit C021, Cape Canaveral Air Force Station, Florida, U.S. Air Force Space Command, Volume 1, May.
- USACE 2012. *In Situ* Thermal Treatment Using Large Diameter Auger Soil Mixing and Zero-Valent Iron Results, Launch Service Building 2, Flame Pit Area, U.S. Army Corps of Engineers, September.

APPENDIX A SWMU 1 SOURCE AREA EXISTING ANALYTICAL DATA



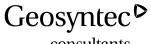
Appendix A information included on CD (see back cover).



APPENDIX B

ENVIRONMENTAL VISUALIZATION SOFTWARE EVALUATION AND VOC MASS ESTIMATE





Page

consultants

of

Written by:	Raphael Siebenmann	Date:	6/13/2013	Reviewed by:			Date:		
Client: Pa	ducah	Project:	SWMU 1 TCE	Mass Estimate	Project/ Proposal No.:	FR5082	Phase No.:	01	

DRAFT SWMU 1 TCE Extent and Mass Estimate

PURPOSE

Utilizing the results of LATA-provided soil sampling data, Geosyntec has developed estimates of the extent and mass of trichloroethene (TCE) in soils above the Regional Gravel Aguifer (RGA) at solid waste management unit 1 (SWMU 1), using C Tech's Environmental Visualization Software (EVS). Provided soil sampling data was collected during evaluation of the Upper Continental Recharge System (UCRS) (1998 and 2004) and Remedial Design Support Investigation (RDSI) (2012) sampling of SWMU 1 soils completed within and immediately surrounding the defined SWMU 1 source area to a maximum depth of 64.1 feet below land surface (ft bls). The purpose of this calculation package is to document the methods used in the calculation of the TCE extent and mass

METHODS

Several interpolation techniques, including kriging, kriging using the 90% confidence interval (CI) about the data, inverse distance weighting (IDW), and nearest neighbor were evaluated, with kriging ultimately being selected as the primary interpolation technique. The techniques are further described below:

- Kriging is a stochastic technique similar to inverse distance weighted averaging in that it uses a linear combination of weights at known points to estimate the value at the grid nodes. Kriging is named after D.L. Krige, who used kriging's underlying theory to estimate ore content. Kriging uses a variogram (a.k.a. semivariogram) which is a representation of the spatial and data differences between some or all possible "pairs" of points in the measured data set. The variogram then describes the weighting factors that will be applied for the interpolation.
- IDW is a method of interpolation that estimates values by averaging the values of sample data points in the neighborhood of each data point. The closer a point is to the center of the cell being estimated, the more influence, or weight, it has in the averaging process. With IDW, the significance of known points on the interpolated values is controlled based on their distance from the output point. A power of two is most commonly used with IDW and is the default.
- Nearest neighbor interpolation is a simple method of interpolation which assigns a value based on the nearest given point.

It is acknowledged that there are significant uncertainties associated with providing a mass estimate of DNAPL using kriging. However, using kriging is still a useful and valid approach to estimate the extent of the source area at various isoconcentration levels below the threshold of residual saturation. Kriging also provides insight about the mass distribution at differing isoconcentration levels. Uncertainty has been considered by estimating mass at different levels of statistical confidence. By kriging data at every node of the model, an average value along with a standard deviation is calculated, thus providing a range of estimated TCE concentrations and ultimately mass. A level of significance of 0.1, the i.e. 90% confidence interval (CI), was used in modeling the geometry and mass of TCE in order to address uncertainty in the estimates.

Due to elevated detection limits at select locations (typically within the range of 500 to 900 µg/kg compared to the SWMU 1 treatment standard for TCE of 73 µg/kg), data from the historic 1998 and 2004 UCRS investigations were analyzed in EVS using 1 µg/kg for the detection limit for non-detect (ND) results. This detection limit is consistent with the typical detection limits observed in the RDSI data.



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Written by:	Raphael Siebenmann	Date:	6/13/2013	Reviewed by:			Date	»:		
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Due to duplicate sampling results in the historical datasets, i.e. multiple TCE analytical results for a given sampling locations and depth interval, a set of decision rules were develop to select the most appropriate result to use in the modeling. The following were the rules followed in selecting a value when duplicate results were available:

- For two detects take the highest value
- For two detects with qualifiers, take the value that has the lowest number of qualifiers
- If both non-detect values are the same, use the data point with the lowest detection limit.
- If one data point is detect and the other is estimated, take the detected value.
- If one data point is non-detect and the other is estimated, take the estimated value

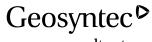
ABOUT EVS

EVS is a software suite for the earth sciences that provides analysis and visualization tools for a wide range of applications. One of the main functions of the software is to interpolate data in both three and four dimensions.

C Tech's software is used by government agencies, universities and companies around the world. Customers include the United Nations, U.S. Environmental Protection Agency (USEPA), Environment Canada, U.S. Geological Survey, British Geological Survey, U.S. Army Corps of Engineers, U.S. Department of Energy (DOE) Laboratories, U.S. Nuclear Regulatory Commission, U.S. Department of Transportation, and the majority of the world's largest engineering and environmental consulting firms (C Tech, 2013).

EVS employs an expert system variogram analysis procedure that examines the spatial distribution and number of points in the input data set, and calculates a variogram that is a best fit to the data under the constraints imposed upon it by the user. In all of EVS's variogram algorithms, if a parameter has a default value of 0 and the user does not change it, then no constraints are being placed on the procedure and the algorithm will calculate, use, and return those parameters which provide the best fit of the variogram to the data (C Tech, 2013).

EVS is similar to other Environmental Decision Support Software (DSS), such as SitePro and Spatial Analysis and Decision Assistance (SADA), and was evaluated by USEPA and DOE in 1998 alongside five other DSS packages. EVS underwent an environmental technology verification report in March, 2000 (USEPA, 2000) that concluded that "the main strengths of EVS-PRO are its outstanding 3-D visualization capabilities and its capability to rapidly process, analyze and visualize data" and "the demonstration showed the EVS-PRO software can be used to generate reliable and useful analyses for evaluating environmental contamination problems."



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MODEL INPUT PARAMETERS

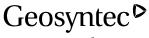
The following model input parameters were used.

Parameter ¹	Default (Yes/No) ²	Value/Setting	Description/Explanation ³
Geology Setup			
Search Distance	Yes	0	The search distance (reach) field defines the radial distance (in user units - ft in this case) from any given model node that the kriging module will look for data points to be included in the estimation of the model parameter at that node. The default value of reach is 0, which results in the module calculating a reach value, which is approximately two-thirds of the longest distance between any two data points in the data set.
Points	Yes	20	The Points parameter defines the maximum number of data points (within the specified reach) that will be considered for the parameter estimation at a model node. The default value for points is 20, which generally provides reasonably smooth modeled parameter distributions.
Quadrant Search	Yes	Disabled	The Quadrant Search toggle changes the method by which data sample points are selected for inclusion in the kriging matrix. If this is on, the "Points" parameter switches to "Max Points in Quadrant". The geology was modeled as one unit, therefore quadrant search was disabled.
X Res/ Y Res	Yes	81 / 81 (results in approx. 4.2 ft ² grid)	The X Res and Y Res parameters specify the number of grid nodes that will be included within the model domain.
Convex Hull Offset	Yes	10%	The Boundary Offset parameter sets the distance that the convex hull for the kriging domain will be set outside of the actual convex hull of the data. This parameter allows the user to specify the distance outside of the actual data in which the parameter values will be extrapolated. The distance is a percentage of the diagonal extent in the X-Y plane.
Geology Model Semivariogram C	Output Parameters		1
Range	Yes	65 ft	Range - the approximate distance at which spatial autocorrelation between data point pairs ceases or the distance at which the difference between the semivariogram and the sill is negligible.
Sill	Yes	0.05 ft^2	Sill - the semivariance value at which the variogram model levels out (plateau).

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Page Written by: Raphael Date: 6/13/2013 Reviewed by: Date: Siebenmann Phase Client: **Paducah SWMU 1 TCE Mass Estimate** Project/ Proposal No.: FR5082 No.: 01 Project: Nugget - the intercept of the semivariance model. EVS uses a nugget of zero, which forces the estimated value to be 0 ft equal to the known value of data points that fall exactly on a Nugget Yes grid point in the modeled domain, thus honoring actual data points. **Chemistry Setup** The X / Y / Z resolution parameters specify the number of X / Y / Z Resolution Yes 71 grid nodes that will be included within the model domain. Adaptive Gridding refines the grid automatically to place grid nodes at all of the measured data points. The adaptive Adaptive Gridding Yes Active grid will result in a kriged parameter distribution that honors all of the measured data points exactly. Proportional gridding results in the number of nodes specified for the Z Resolution will be distributed (proportionately) over the geologic layers in a manner that is Proportional Gridding Yes Active approximately proportional to the fractional thickness of each layer relative to the total thickness of the geologic domain. Min Cells per layer - establishes a minimum number of cells 2 Min Cells Per Layer / Units Yes (in the Z direction) per layer. Minimum layer thickness forces layers thinner than the 0.00001 Min Layer Thickness Yes specified value to have a minimum thickness and therefore not pinch out completely. TCE concentrations in soil were kriged in the model domain. Krig 3D Chemistry Input 1 μg/kg was used for non-detect results. TCE Statistical Method Yes Ordinary Kriging An Octant is any of the eight parts into which three mutually perpendicular planes divide space. Octant search - a maximum of N points (defined by user) in each of the eight octants surrounding the interpolation point are used in the calculations. This method results in better performance with clustered data. The Octant Search toggle changes the method by which data sample points are selected for inclusion in the kriging matrix. If this is on, the "Points" Octant Search No Enable parameter switches to "Max Points in Octant". Searching is performed for each of the eight Octants surrounding the point to be kriged. Within each octant a maximum number of points (up to one-fourth of the total points) are selected. Then, points are taken sequentially from each octant up to the maximum number of total points or until all octant's points have been used.



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Written by:	Raphael Siebenmann	Date:	6/13/2013	Reviewed by:		I	Date:	
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Anisotropy			No ⁴	1	The Horiz./Vert. Anisotropy model to consider the effects conductivity of soil matrices geologic materials are deposi oriented horizontally, and the saturated and unsaturated zor direction than in the horizont deposition can occur along he fracture systems. Chemical c with flowing fluids may there spreading in one or the other Anisotropy Ratio allows the language model node. The defau which allows data points in a model node to influence the times more than data points a vertical direction. When the related to fluid flow or other by matrix anisotropy, then the isotropic.	of anisotropy to fluid flow. ited with platy us flow of wat ne can be slow tal direction. A constituents be efore show a l direction. The kriging algorited to apply bi vertical direct tilt value for fluid horizontal direct property bein processes that	in the In most case clay minera er in both the er in the ver also, ore ertical fault or ing transport arger degree e Horiz./Verthm to specifiased weightions away fruid flow is 10 rection away at that node ice away in a g modeled is might be affi	es, ls e tical or eed of 'y a ng on om a 0, from 10 t not fected
Chemistry N	Model Semivariogra	am Output	Parameters					
Range			Yes	106 ft	Range - the approximate dist autocorrelation between data distance at which the differer and the sill is negligible.	point pairs ce	ases or the	gram
Sill			Yes	3 ft2	Sill - the semivariance value levels out (plateau).	at which the v	ariogram mo	odel
Nugget			Yes	0 ft	Nugget - the intercept of the a nugget of zero, which force equal to the known value of a grid point in the modeled dor points.	es the estimate data points tha	d value to be t fall exactly	on a
Volumetric Pa	rameters		l l		•			
Soil Density			No	1.50 g/cc	Soil density of the soil matrix	x in which the	chemicals re	esides.
Chemical De	ensity		No	1.46 g/cc	Chemical density at (20 °C)			

Notes:

 $1. \ \ Input parameters for kriging software (Environmental Visualization System - Premier 9.82, C-Tech Corporation).$



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- 2. Indicates whether value used is the software default.
- 3. Parameter descriptions adapted from "C Tech Help System for EVS & MVS 9.8" by C Tech Development Corp.
- 4. Software default assumes fluid flow. 1 is the software's suggested value for vadose zone modeling.

RESULTS

As shown below, the interpolation of the 2012 RDSI investigation estimates that 40.7 kg of TCE is present is SWMU 1 soils.

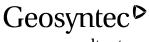
Mass estimates were calculated using kriging, kriging using the 90% CI, IDW, and nearest neighbor. The results of the EVS-ES modeling using the historical results and the RDSI soil results are presented below.

	Kriging	90% CI Kriging	IDW	Nearest Neighbor
Isoconcentration Level µg/kg		Mass o	of TCE (gal)	
73	8.9	29.3	1.4	24.8
1,000	8.0	28.1	0.5	23.7
10,000	4.2	19.8	0.1	18.0

From a mass distribution perspective, both the 90% CI kriging and nearest neighbor interpolation indicate that 96% of the estimated mass is located within the greater than 1,000 μ g/kg isocontour area. The EVS estimated weight calculated is less than the weight estimated in the SI.

The horizontal extent of the 73 μ g/kg isocontour using nominal kriging interpolation is estimated to be approximately 13,500 square ft. The 1,000 μ g/kg and 10,000 μ g/kg isocontours using the 90% CI kriging interpolation are estimated to be approximately 9,900 square ft and 3,700 square ft respectively.

Modeling results have been included in this calculation package as "4DIM files", which are freely rotatable 3D model. Key screenshots of the model are presented below:



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Project/ Proposal No.:

Written by:	Raphael Siebenmann	Date:	6/13/2013	Reviewed by:	Date:
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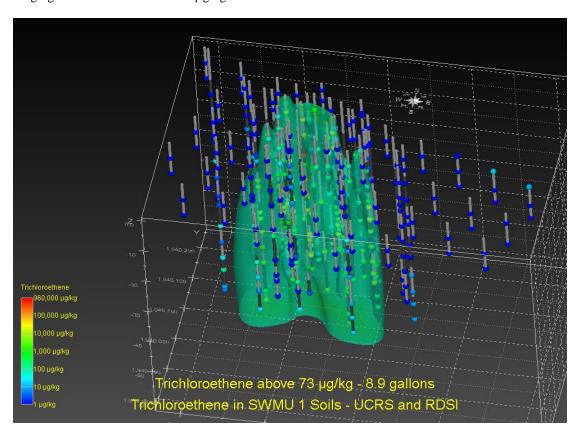
Phase No.: **01**

Kriging results for TCE above 73 $\mu g/kg$

Project:

Paducah

Client:

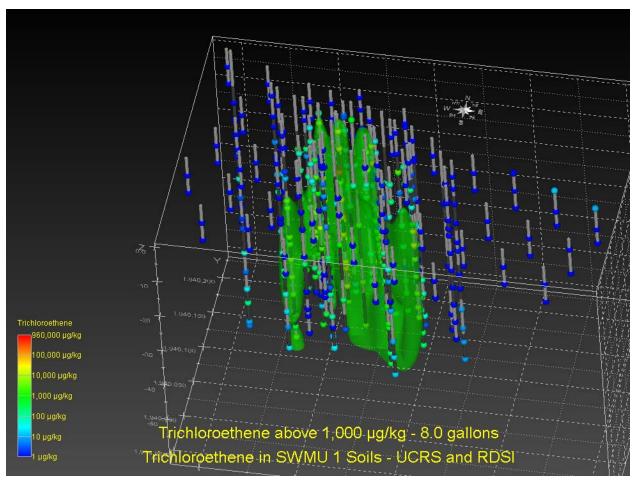


SWMU 1 TCE Mass Estimate



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Written by:	Raphael Siebenmann	Date:	6/13/2013	Reviewed by:			Date	:		
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Kriging results for TCE above 1,000 μ g/kg



Kriging results for TCE above 1,000 µg/kg using 90% CI

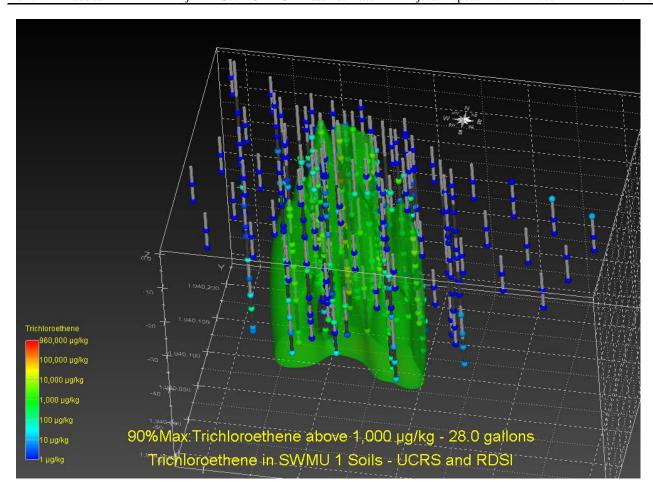


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Written by: Raphael Date: 6/13/2013 Reviewed by: Date: Siebenmann

Phase

Client: Paducah Project: SWMU 1 TCE Mass Estimate Project/ Proposal No.: FR5082 No.: 01



REFERENCES

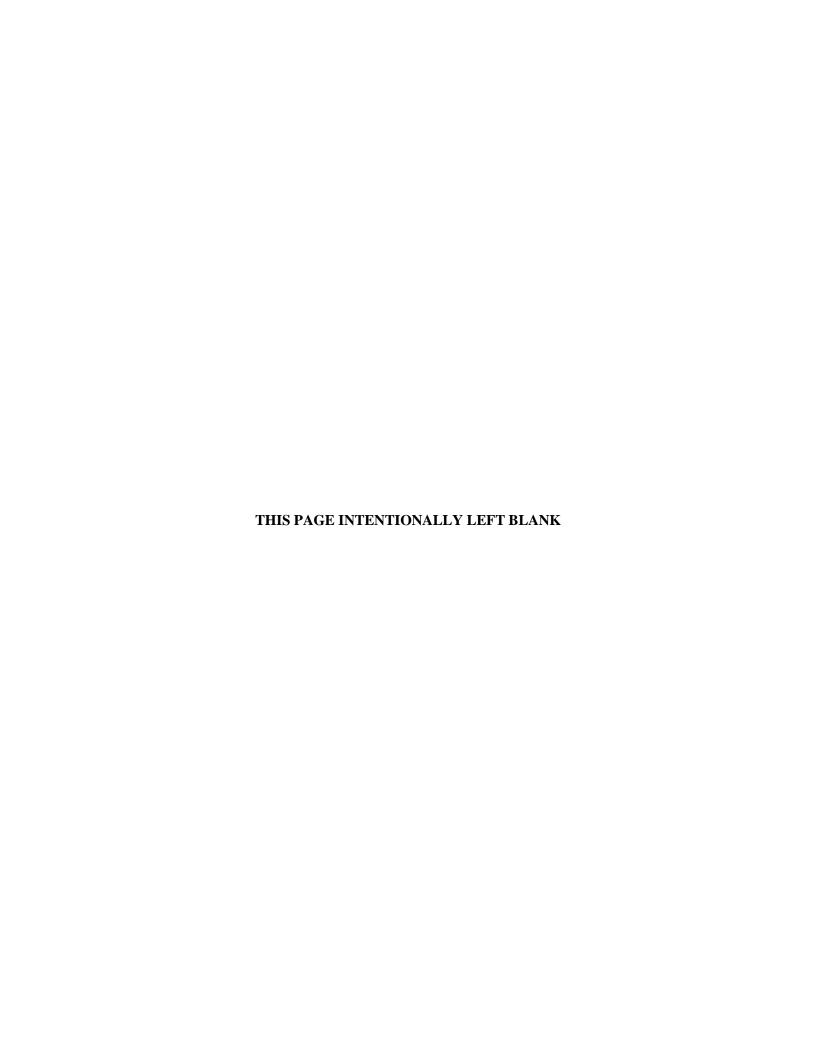
C Tech Development Corporation. Web. 4 February 2013. http://www.ctech.com

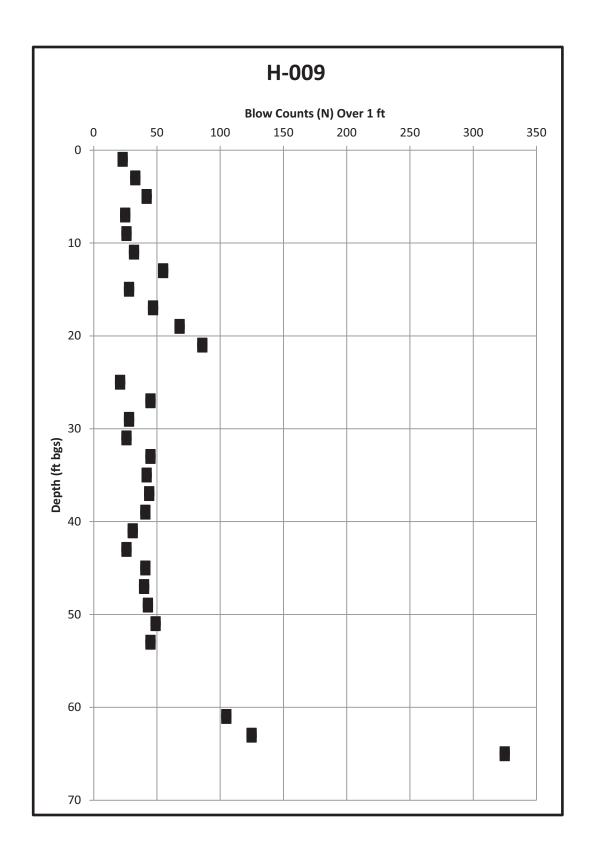
USEPA, March 2000. "Environmental Technology Verification Report. Environmental Decision Support Software. C Tech Development Corporation. Environmental Visualization System Pro (EVS-PRO). EPA/600/R-00/047.

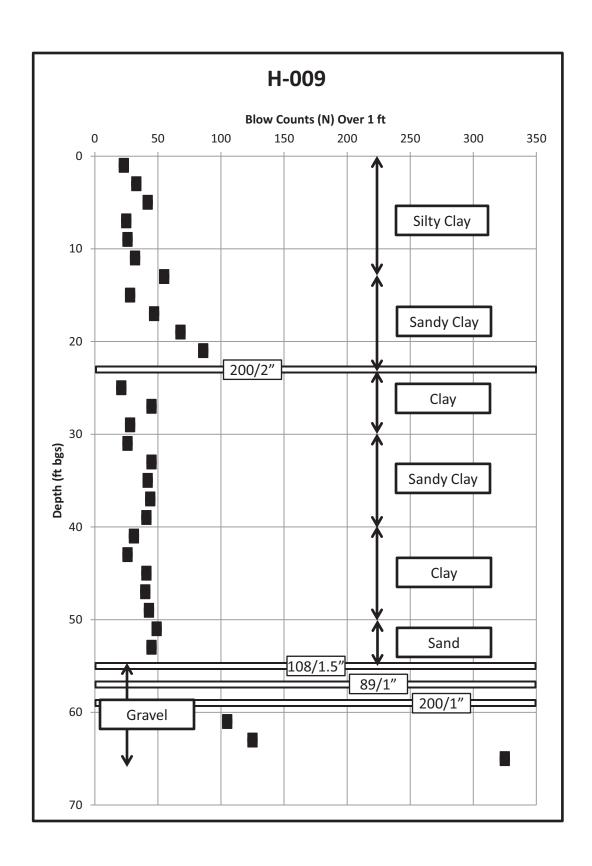
Appendix B information included on CD (see back cover).

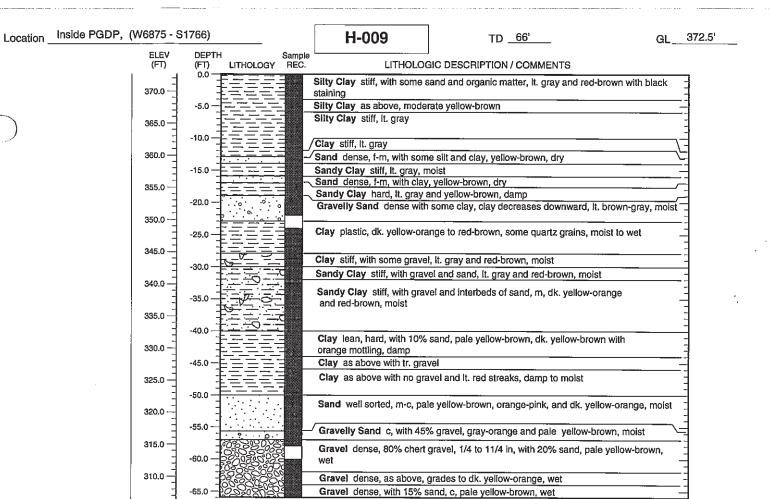
APPENDIX C

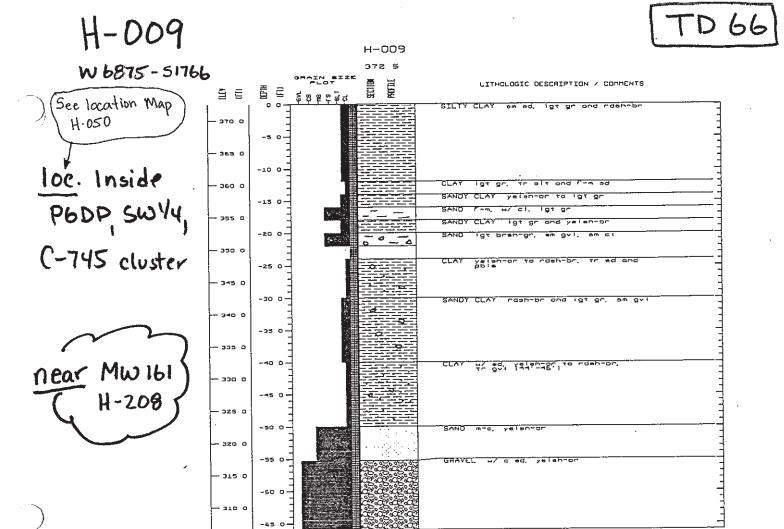
STANDARD PENETRATION TEST RESULTS SUMMARY AND GEOTECHNICAL DATA











MAPD

Detailed Loc. Map CH2MHill Phase I, Vol. 2, Fig 4-2

PROJECT NUMBER SED28178.FS BORING NUMBER

H-009 SHEET 1 OF 3

SOIL BORING LOG

PROJE	PROJECT PGDP Phase I Site Investigation LOCATION WMU 1, Oil Landfarm								
ELEVA						Engineering			
				DUIPMENT	Mobile B-53, Hollow Stem Auger	7110000			
WATER	LEVE	L AND	DATE_	CTANDARO	START1/6/90FINISH	1/10/90 LOGGER Bill Cocke			
	5	SAMPL	E	PENETRATION	SOIL DESCRIPTION	COMMENTS			
DEPTH BELOW SURFACE (FT)	NTERVAL	TYPE AND NUMBER	RECOVERY (FT)	TEST RESULTS 6" -6" -6" (N)	SOIL NAME, COLOR, MOISTURE CONTENT, RELATIVE DENSITY OR CONSISTENCY, SOIL STRUCTURE, MINERALOGY, USCS GROUP SYMBOL	DEPTH OF CASING, DRILLING RATE, DRILLING FLUID LOSS. TESTS AND			
필공	~	FZ	品币	(11)	_	INSTRUMENTATION			
2 -	0-2		0.75	9-11-12-12 (23)	SILTY CLAY WITH SAND, VERY LIGHT GRAY (NB) WITH IRON STAINING, MODERATE REDDISH BROWN (10 YR 46) AND BLACK ORGANIC STAINING, DAMP, LOW PLASTICITY, VERY — STIFF, SOME VEGETABLE MATTER, (CL)	BACKGROUND RAD-40-45 CPM HNU-0 PPM SAMPLE HNU-0 PPM RAD-160 CPM			
4 -	2-4	4213		14-14-19-30 (33)	SAME AS ABOVE, BUT WITHOUT VEGETABLE MATTER, HARD, (CL)	HNU-0.3 PPM RAD-40-45 CPM —			
	4-6		1.0'	30-24-18-30 (42)	SAME AS ABOVE, COLOR CHANGING TO MODERATE YELLOWISH BROWN (10 YR 5/4), HARD, (CL)	HNU-20 PPM (IN SPOON) RAD-40 CPM COMPOSITED SAMPLE 4213 AT 1500			
6 -	6-8		1.25	13-12-13-14 (25)	SAME AS ABOVE, COLOR CHANGING BACK TO GRAY (N8), VERY STIFF, (CL)	HNUL18 PPM (IN SPOON) RAD-40 CPM			
	8-10	4214	1.5	11-12-14-18 (26)	SAME AS ABOVE, COLOR GRAY (NB) AND YELLOWISH BROWN (10 YR 54), VERY STIFF, (CL)	HNU-30 PPM (IN SPOON) RAD-40 CPM			
12 —	10-12		2.0'	13-13-19-19 (32)	SAME AS ABOVE, VERY LIGHT GRAY (NS), HARD, (CL)	HNU-30 PPM (IN SPCON) RAD-45 CPM COMPOSITED SAMPLE 4214 AT 1520			
14 —	12-14		2.0	13-19-36-48 (55)	CLAY (CH), VERY LIGHT GRAY (N8), MOIST, HARD, PLASTIC, CHANGING TO WELL GRADED SAND, WITH SOME SILT AND CLAY, MODERATE YELLOWISH BROWN (10 YR 54), DRY, VERY DENSE, FINE-MEDIUM, (SW-SC)	HNU-31 PPM RAD-45 CPM			
_	14-16	4215	2.0	6-14-14-15 (28)	SANDY CLAY, VERY LIGHT GRAY AND MODERATE YELLOWISH BROWN (NB AND 10 YR 54), MOIST, VERY STIFF, (CL)	HNU=0.2 PPM RAD=45 CPM			
16	16-18		1.5'	19-20-27-30 (47)	WELL GRADED SAND, WITH CLAY, LIGHT GRAY (N7), MOIST, DENSE, FINE-MEDIUM, (SW), CHANGING TO SANDY CLAY, LIGHT GRAY (N7), AND YELLOWISH BROWN (10 YR 54), DAMP, HARD, (CL)	HNUL85 PPM RAD-40 CPM COMPOSITED 4215 AT 1800			
20	18-20			26-32-36-48 (68)	SANDY CLAY SAME AS ABOVE, (CL), CHANGING TO WELL- GRACED SAND, LIGHT BROWNISH GRAY (5 YR 61), VERY DENSE, DAMP-HOIST, COARSE PEBBLES AND SOME CLAY, (SW)	HNU-16 PPM RAD-0 CPM			
22 -	20-22	4216		26-40-46-50 (86)	WELL GRADED SAND AS ABOVE, MOIST, VERY DENSE, VERY LITTLE CLAY WITH LENSES OF GRAVEL (SW)	HNU- 14.5 PPM			
_	22-24			200/2*	NO SAMPLE				
24	24-26		2.0°	7-7-14-19 (21)	CLAY, DARK YELLOWISH ORANGE (10 YR 66), MOIST, VERYSTIFF, PLASTIC, (CH)	HNU-20 PPM RAD-35-40 CPM COMPOSITED SAMPLE 4216 AT 0825			
28	26-28	10.0	1,8*	14-18-27-30 (45)	CLAY SAME AS ABOVE, COLOR CHANGING TO MODERATE RECOISH BROWN (10 R 46), MOIST-WET, HARD, SOME COARSE SAND GRAINS, (CH)	HNU-31 PPM RAD-40 CPM			
-	28-30	4218	2.0'	15-15-13-14 (28)	CLAY SAME AS ABOVE, MODERATE REDDISH BROWN AND LIGHT GRAY (10 R 46 AND N7), MOIST, VERY STIFF, LOW PUASTICITY, SOME LARGE PEBBLES, (CL)	HNUL-25 PPM RAD-40-45 CPM AUGER TO 30', STOP TO SET CASING			

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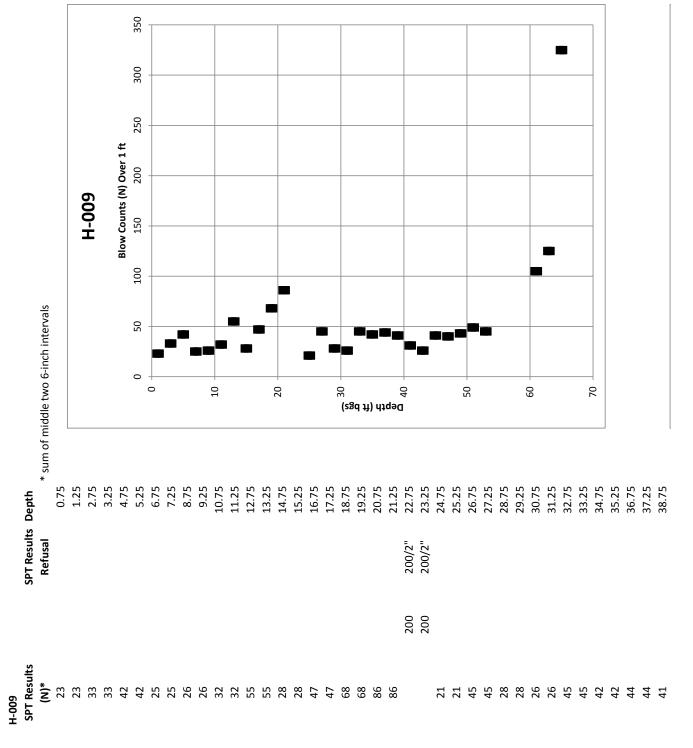
SOIL BORING LOG

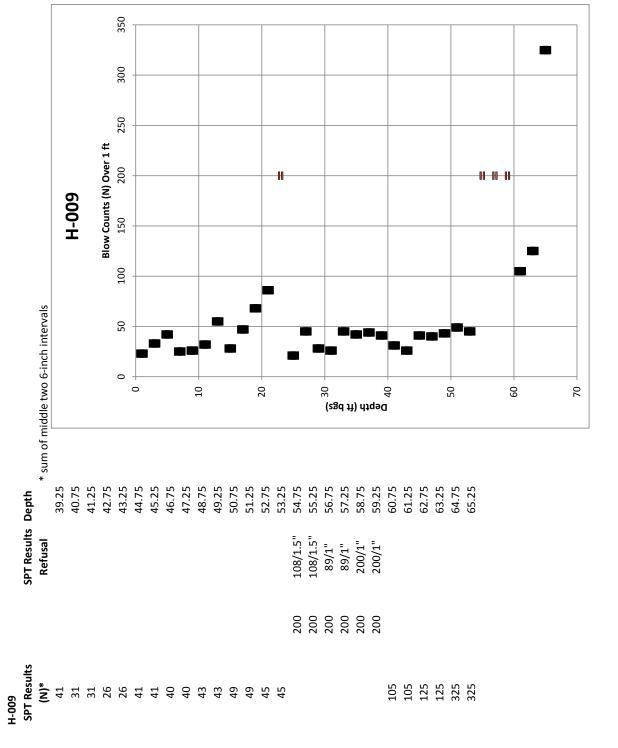
rROJE	ст <u>Р</u> С	DP Ph	ase I S	Site Investiga	ation Location WMU			
ELEAY.	TION		UD 5011	IDMENT Mob	DRILLING CONTRACTOR Geotek Engi	neering		
		HOD AI		IPMENT_IVIQU	START 1/6/90 FINISH 1	/10/90 LOGGER Bill Cocke		
117.121		AMPLE		STANDARD ENETRATION	SOIL DESCRIPTION	COMMENTS		
SURFACE (FT) INTERVAL TYPE AND NUMBER RECOVERY (FT)				TEST RESULTS 6" -6" -6" (N)	SOIL NAME, COLOR, MOISTURE CONTENT, RELATIVE DENSITY OR CONSISTENCY, SOIL STRUCTURE, MINERALOGY, USCS GROUP SYMBOL	DEPTH OF CASING, DRILLING RATE, DRILLING FLUID LOSS. TESTS AND INSTRUMENTATION		
-30 '-	30-32	4218	2.0'	6-9-17-29 (26)	SANDY CLAY, MODERATE REDDISH BROWN AND LIGHT GRAY (10 R 46 AND N7), MOIST, VERY STIFF, LOW PLASTIC- ITY, WITH GRAVEL SOME LARGE PEBBLES, (CL)	HNU-0.2 PPM RAD-40-45 CPM RESUMED SAMPLING 1/9/90, COMPOSITED SAMPLE 4218 AT 1345		
32 — —	32-34		2.0"	17-19-26-21 (45)	SANDY CLAY, SAME AS ABOVE, MODERATE REDOISH BROWN AND DARK YELLOWISH ORANGE (10 YR 66), HARD. WITH GRAVEL, (CL)	HNU-0 PPM RAD-40-45 CPM		
34 —	34-36	4219	2.0'	17-17-25-29 (42)	SANDY CLAY, SAME AS ABOVE, MODERATE REDOISH BROWN, HARD, WITH GRAVEL AND LAYERS OF MEDIUM SAND, (CL)	HNU=0.2 PPM RAD=40 CPM		
36 -	36-38		2.0'	18-18-26-27 (44)	SANDY CLAY SAME AS ABOVE	HNU-3.0 PPM RAD-40 CPM COMPOSITED SAMPLE 4219 AT 1420		
38 -	38-40		2.0°	16-17-24-26 (41)	CLAY SAME AS ABOVE	HNU-0 PPM		
40	40-42	4220	2.0'	13-13-18-21 (31)	LEAN CLAY WITH SAND, PALE YELLOWISH BROWN (10 YR 62) WITH DARK YELLOWISH DRANGE (10 YR 66) STREAKING, SOME MOTTLING WITH DRANGE, DARK DISCOLORATION, DAMP, HARD, <10% FINE SAND, (CL.)	RESUMED SAMPLING 1/10/90 AT 1000 HNU-0 PPM RAD-40 CPM		
42 -	42-44	-	2.0	13-13-13-14 (26)	LEAN CLAY WITH SAND SAME AS ABOVE, VERY STEF, =15% SAND IN LOWER =0.3" OF SPOON, (CL)	HNU-0 PPM RAD-45 CPM		
44 -	44-46		2.0'	18-17-24-26 (41)	LEAN CLAY WITH SAND SAME AS ABOVE, HARD, MODERATE RED STREAKS (5 R 5/4), 2 SMALL (-<1° DIAMETER) PIECES OF GRAVEL, (CL.)	HNU-0.2 PPM RAD-45 CPM		
46 -	46-48	4221	2.0°	18-18-22-25 (40)	LEAN CLAY WITH SAND SAME AS ABOVE, HARD, NO GRAVEL, (CL)	HNU-02 PPM RAD-45 CPM		
48 -	48-50		2.0'	18-18-25-26 (43)	LEAN CLAY WITH SAND, PALE YELLOWISH BROWN (10 YR 6/2) WITH DARK YELLOWISH ORANGE (10 YR 6/6) AND LIGHT RED (5 R 6/6) STREAKS, DAMP-MOIST, HARD, 1 PEBBLE, COAL LENSES, (CL.)	HNU=0.2 PPM RAD=45 CPM COMPOSITED SAMPLE 4221 AT 0900		
50	50-52		1.75	18-23-26-27 (49)	POORLY GRADED SAND. PALE YELLOWISH BROWN (10 YR 6' 2), SLIGHT MODERATE ORANGE PINK (10 R 7/4) AND DARK YELLOWISH ORANGE (10 YR 66) STREAKS, MOIST, DENSE, MEDIUM GRAINED, NO GRAVEL (SP)	HNU=0.2 PPM — RAD=45CPM —		
52	52-54	4223	2.0'	25-18-27-28 (45)	SAND SAME AS ABOVE, (SP)	HNU-0.8 PPM - RAD-52-54 CPM		
54	54-5	- · 6	1.7	108/1.5	POORLY GRADED SAND, PALE YELLOWISH BROWN (10 YR 5 2), SOME MODERATE ORANGE PINK (10 R 74) AND DARK YELLOWISH ORANGE (10 YR 66) STREAKS, MOIST, VERY DENSE, MEDIUM-COARSE GRANED, GRAVEL IN LOWER =0.4 (SP)	HNU-0.8 PPM		
56	56-5	7	0.8	89/1"	WE'L GRADED SAND, COARSE SAND WITH '45% GRAVEL, QUARTZ CRYSTALS, PALE YELLOWISH BROWN (10 YR 62) WITH GRAYISH ORANGE (10 R 7/4) STREAKS, WET, VERY	HNU=0 PPM		
58	57-5	8	1.2	200/1*	DENSE, GRAVEL (GW)			
	58-6	4224		SAMPLE TAKE	N Co	_		

PROJECT NUMBER	BORING NUM	ABER				
SED28178.FS	H-009	SHEET	3	OF	3	
		,				

SOIL	B	OR	ING	LOG
	_	~		

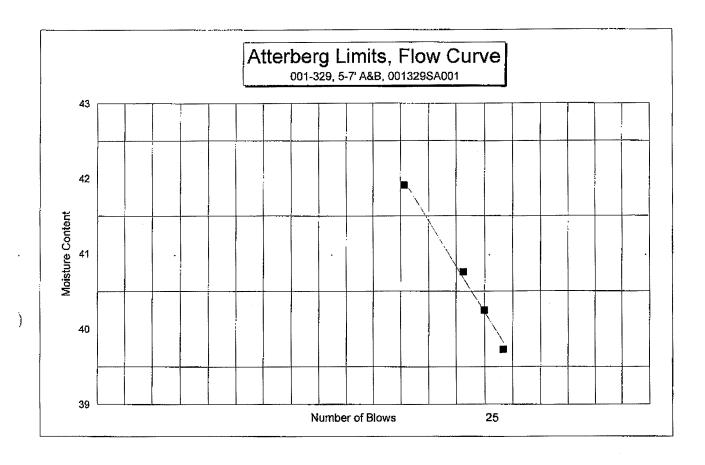
, ROJE	ROJECT PGDP Phase I Site Investigation LOCATION WMU 1, Oil Landfarm									
ELEVA"	TION	THOD	AND EC	DUBMENT M	DRILLING CONTRACTOR Geotek Enobile B-53, Hollow Stem Auger	gineering				
		L AND		ZOIFMENT		1/10/90 LOGGER Bill Cocke				
		SAMPLI	Ę	STANDARD PENETRATION	SOIL DESCRIPTION	COMMENTS				
SDEPTH BELOW SURFACE (FT)	INTERVAL.	TYPE AND NUMBER	RECOVERY (FT)	TEST RESULTS 6" -6" -6" (N)	SOIL NAME, COLOR, MOISTURE CONTENT, RELATIVE DENSITY OR CONSISTENCY, SOIL STRUCTURE, MINERALOGY, USCS GROUP SYMBOL	DEPTH OF CASING, DRILLING RATE, DRILLING FLUID LOSS. TESTS AND INSTRUMENTATION				
62 —	60-62	4224	0.5	60-40-65-100 (105)	WELL GRADED GRAVEL WITH SAND, PALE YELLOWISH BROWN (10 YR 62), SAND =20%, WET, VERY DENSE, SAND =20%, GRAVELS =14" TO 1-14" DIAMETER, QUARTZ, CHERT, (GW)	HNUL-O PPM RAD40 CPM				
64	62-64	4224	1.5	60-65-60-74 (125)	WELL GRADED GRAVEL WITH SAND, PALE YELLOWISH BROWN (10 YR 6/2), GRADES INTO DARK YELLOWISH CRANGE (10 YR 6/6), WET, VERY DENSE, GRAVELS *14'>1/2' DIAMETER; QUARTZ, CHERT, (GW)	HNU-0 PPM RAD-40 CPM COMPOSITED SAMPLE 4224 AT 1215, (56-58' AND 60-64' NO SAMPLE AT 58-60')				
	64-66	4225	1.7"	135-160-165-175 (325)	WEIL GRADED GRAVEL WET, VERY DENSE, GRAVEL =14-2" DIAMETER, MOSTLY CHERT, SOME SAND =15%, COARSE GRANED, PALE YELLOWISH BROWN (10 YR 6/2), (GW)	HNU-0 PPM RAD-30-40 CPM COMPLETED SAMPLE 4225 AT 1606 (64-66) TD OF BORING, 66.0'				
66 —										
68 _										
00 -	i İ				_					
)70			ļ i.							
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72						_				
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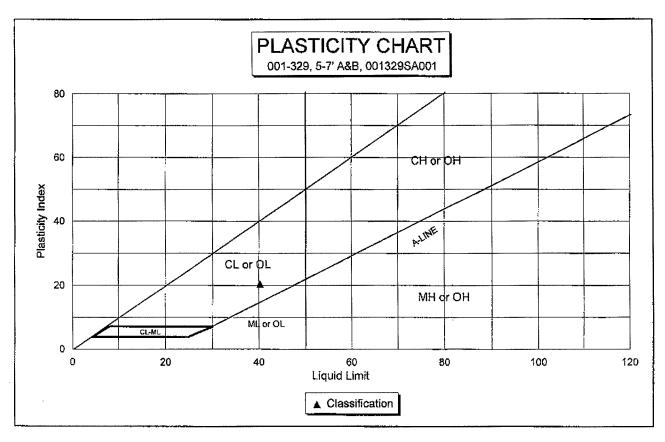


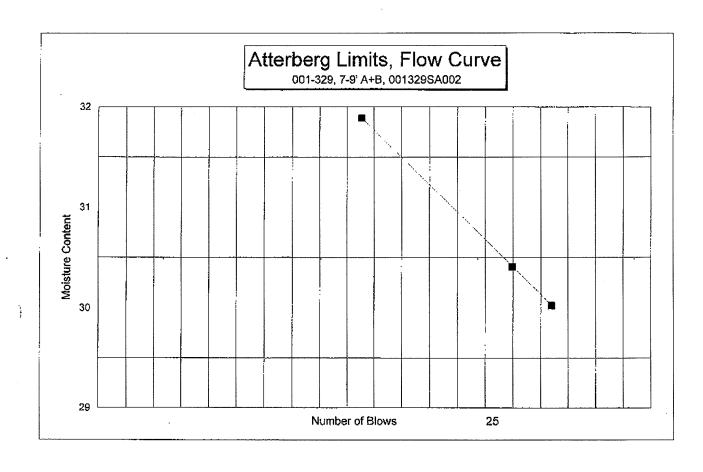


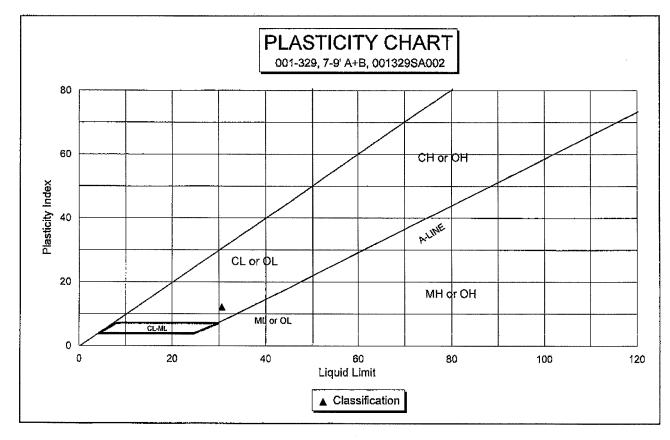
Geotechnical Soil Data Soil Boring: 001-239 SWMU 1: C-746-C Oil Landfarm

Sample	Depth	Moisture Content	рН	Liquid Limit	Plastic Limit	Plasticity Index	Atterberg Classificatiion	Fraction of Organic Carbon
	(ft)	(%)	(Std Units)					(mg/Kg)
001329SA001	5.0-7.0	22.8	5.54	40.2	19.9	20.4	CL	
001329SA002	7.0-9.0	23.3	7.15	30.7	18.6	12.1	CL	
001329SA003	10.0-12.0	21.4	6.63	30.1	15.2	15.0	CL	
001329SA004	16.5-17.5	15.8	6.97	24.3	14.2	10.1	CL	
001329SA005	18.5-19.5	8.2	7.49	30.1	12.4	17.7	CL	
001329SA006	20.5-21.5	12.2	7.42	36.6	11.1	25.6	CL	
001329SA007	30.0-32.0	19.6	7.51	25.3	10.5	14.8	CL	
001329SA008	40.0-42.0	14.2	7.08	18.7	13.6	5.1	CL-ML	
001329SA009	50.0-50.9	17.9	7.53	20.7	11.8	8.9	CL	
001304FOC1	14.9							5,900
001304FOC2	26.5							430
001304FOC3	42.5							230
001307FOC1	12.5							740
001307FOC2	23.5							680
001307FOC3	33							360
001318FOC1	13							290
001318FOC2	20.5							240
001318FOC3	41							920

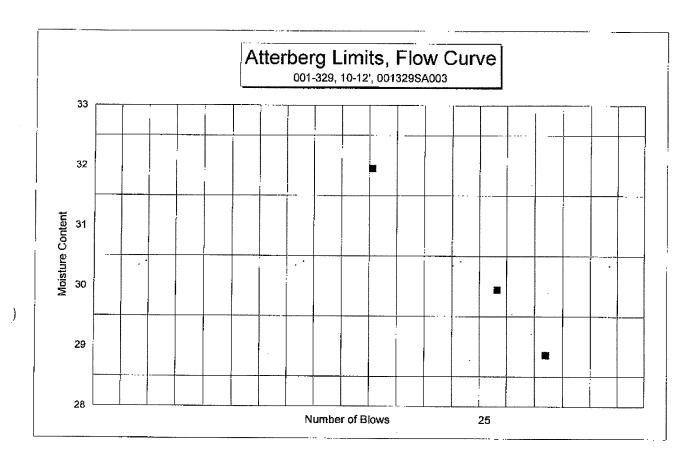


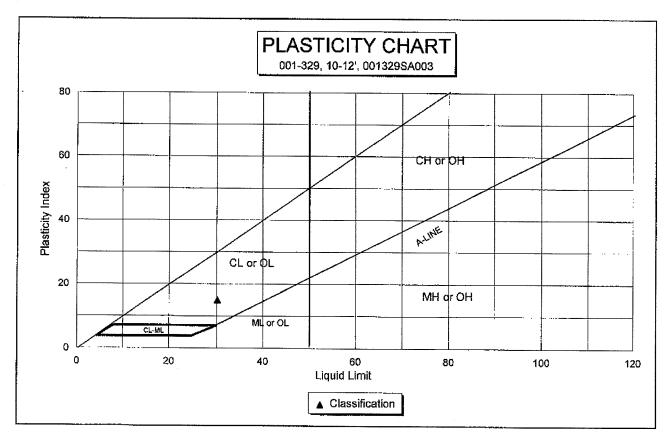


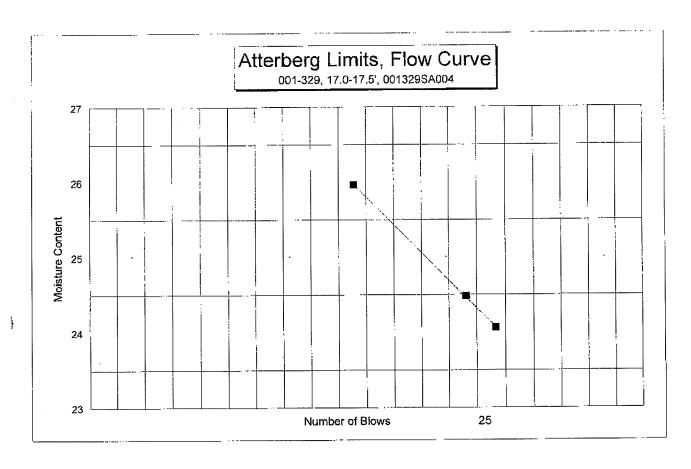


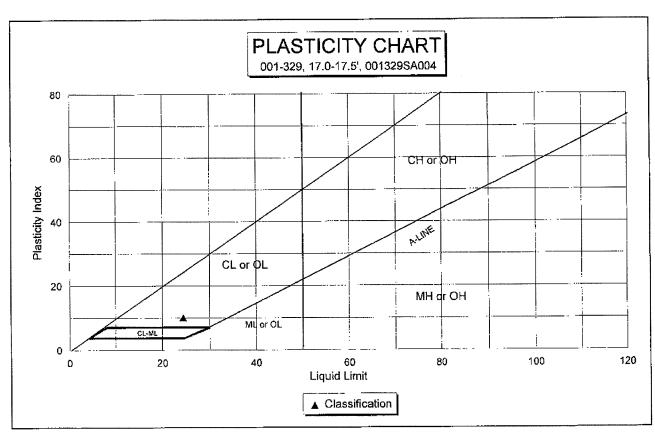


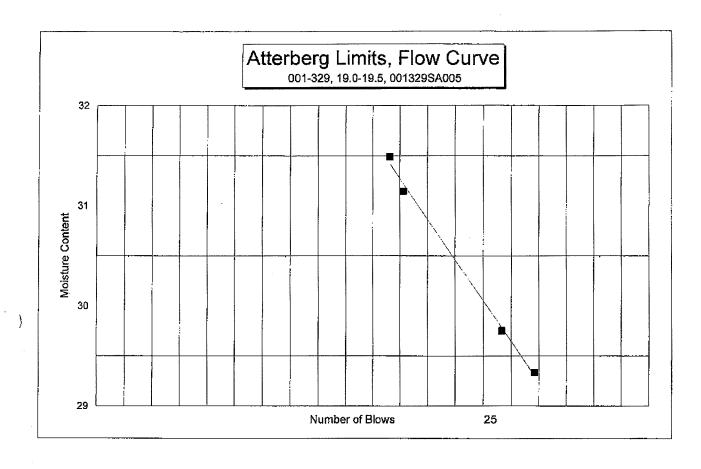
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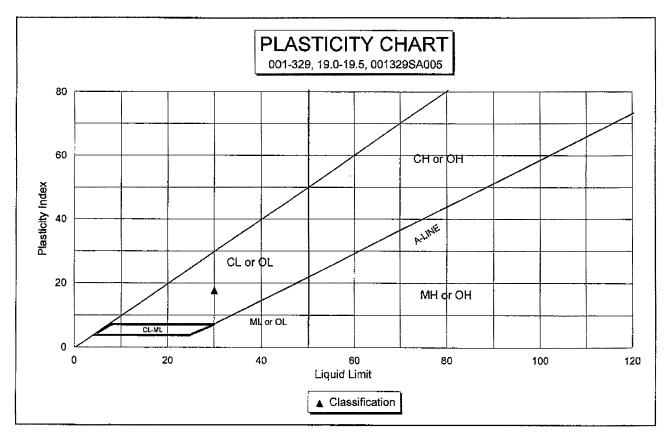


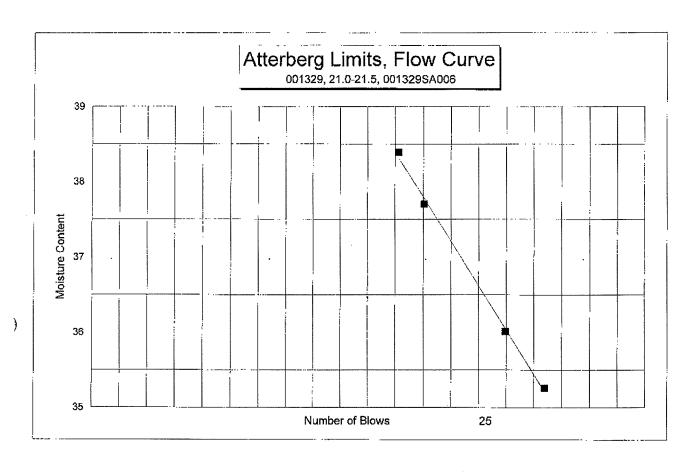


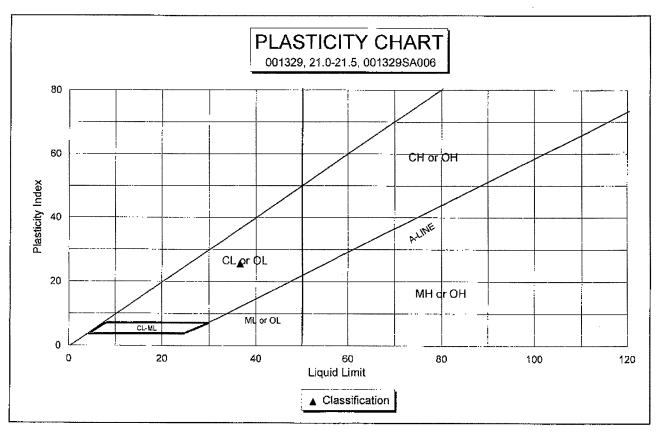


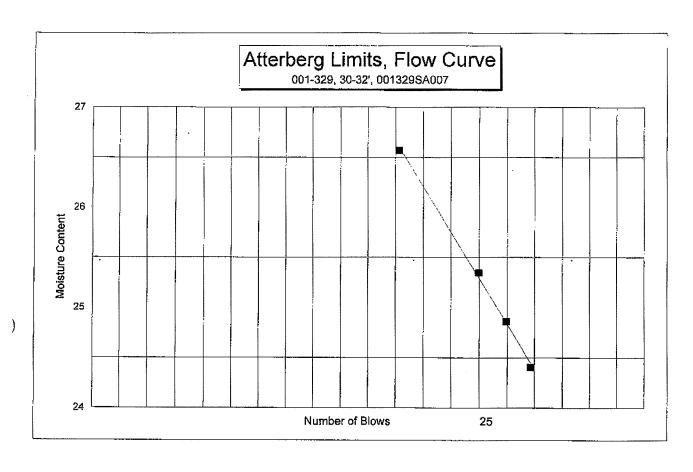


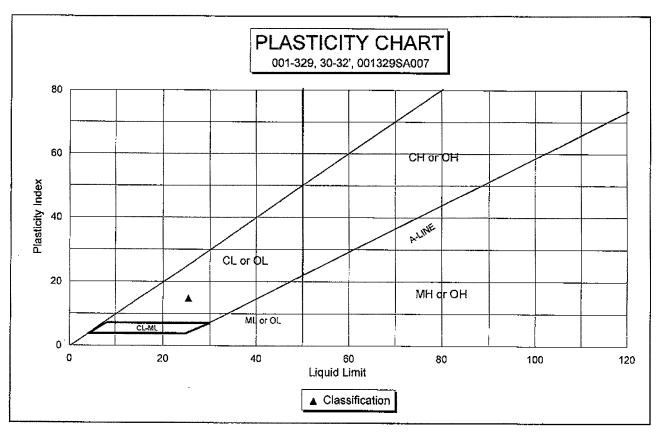


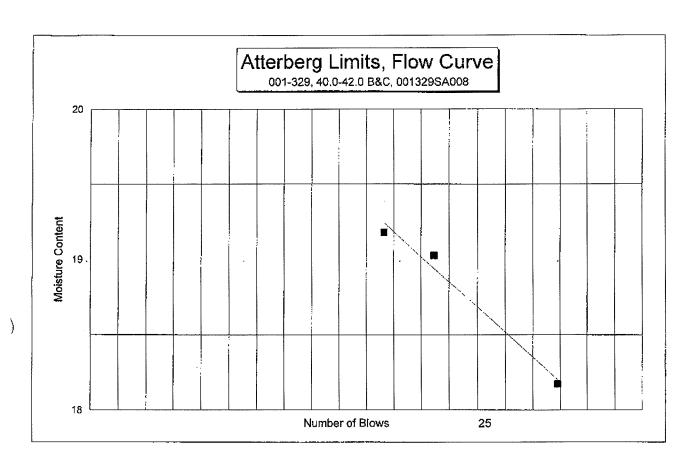


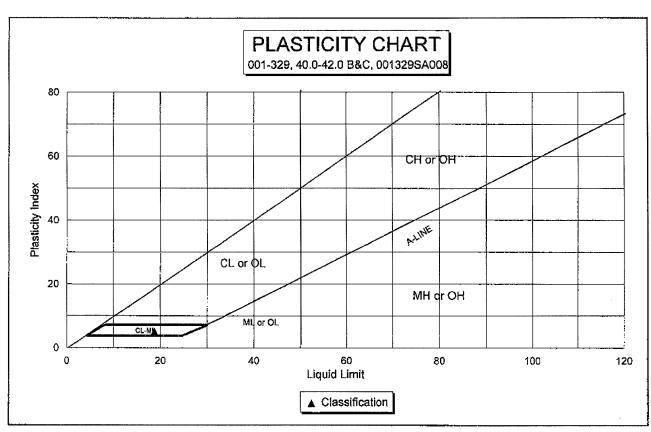


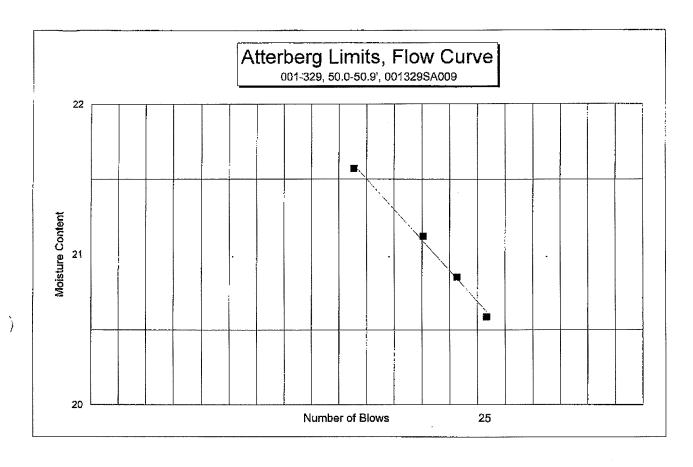


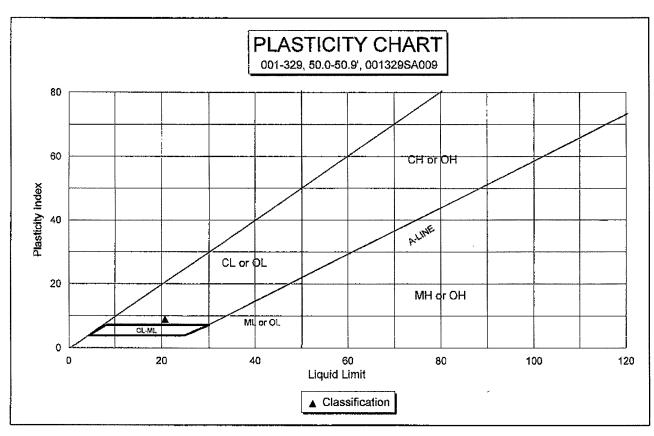


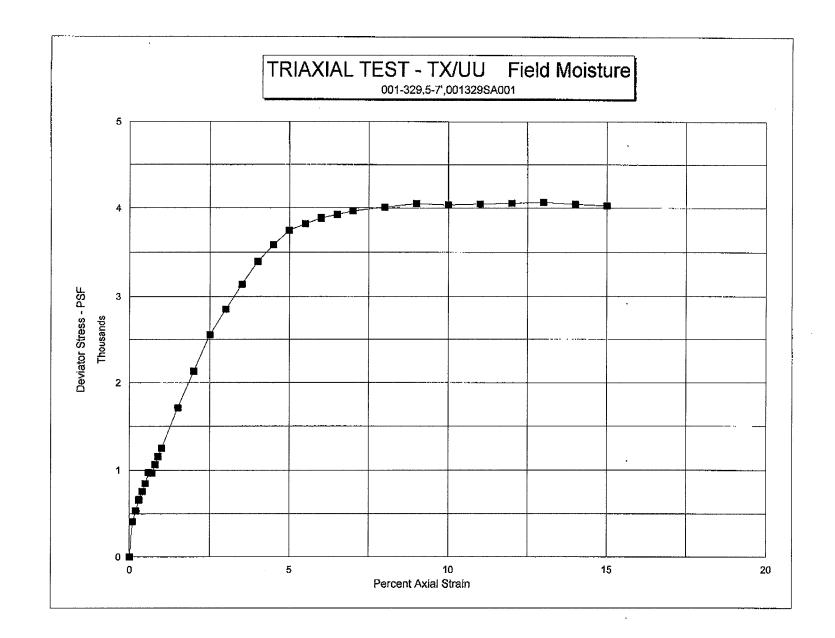


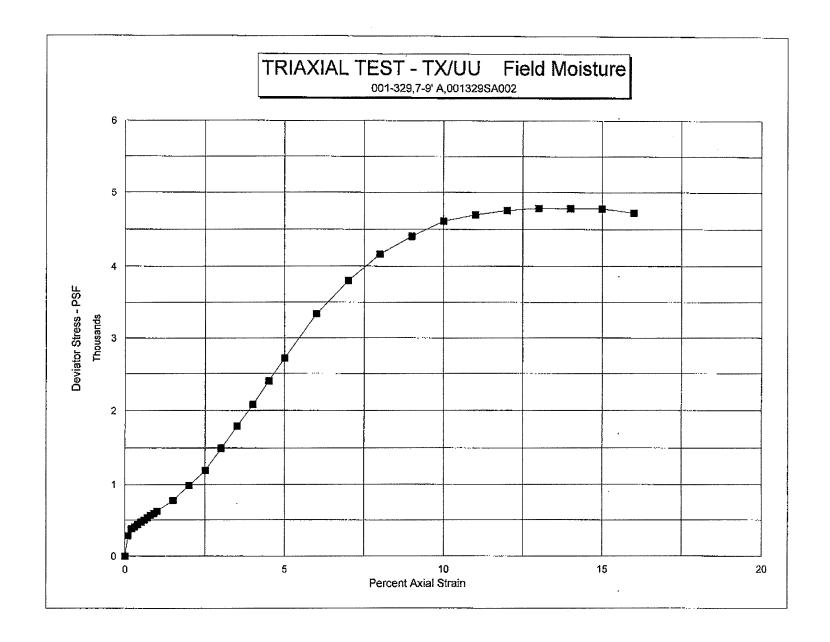


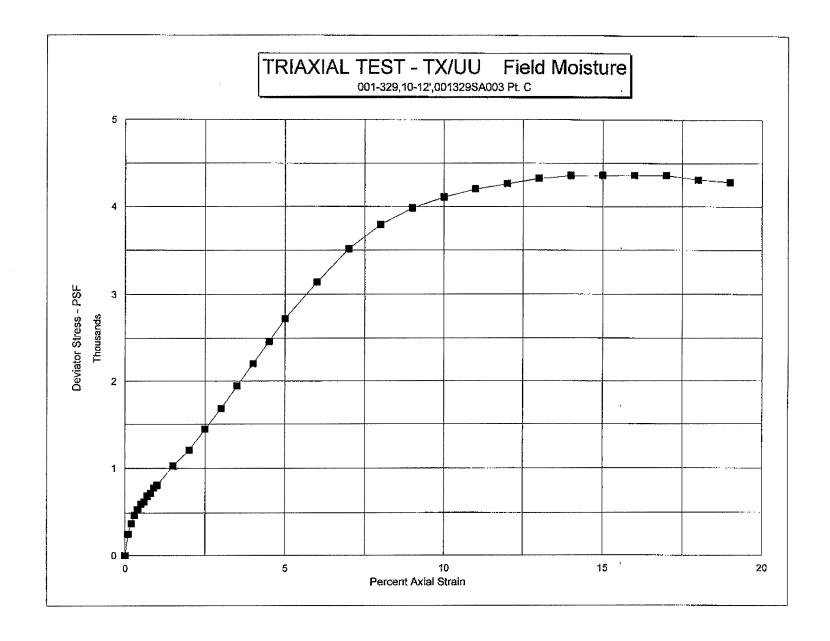


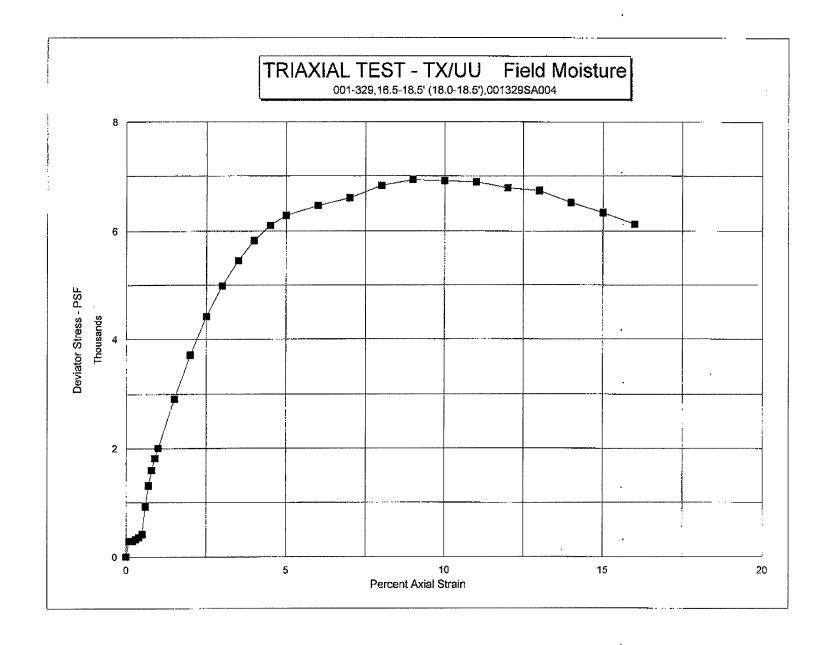


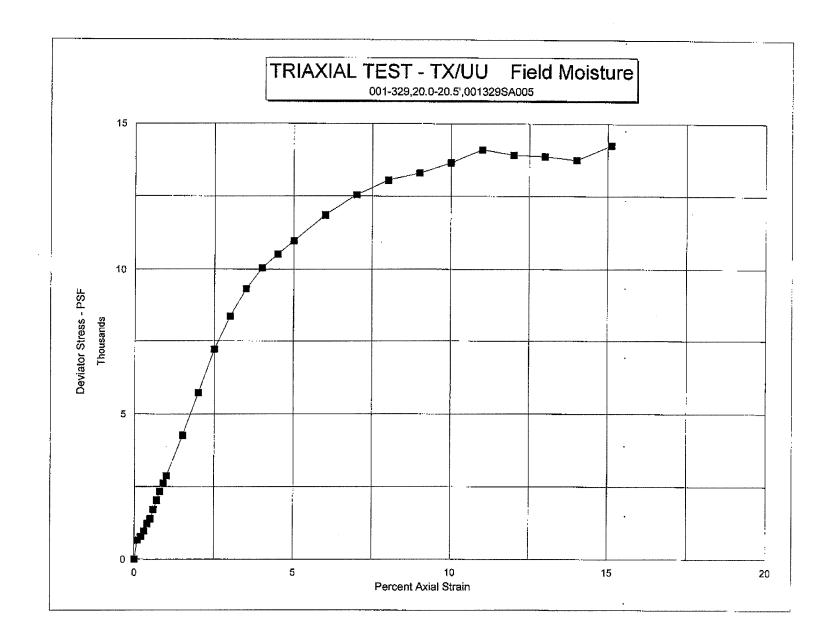


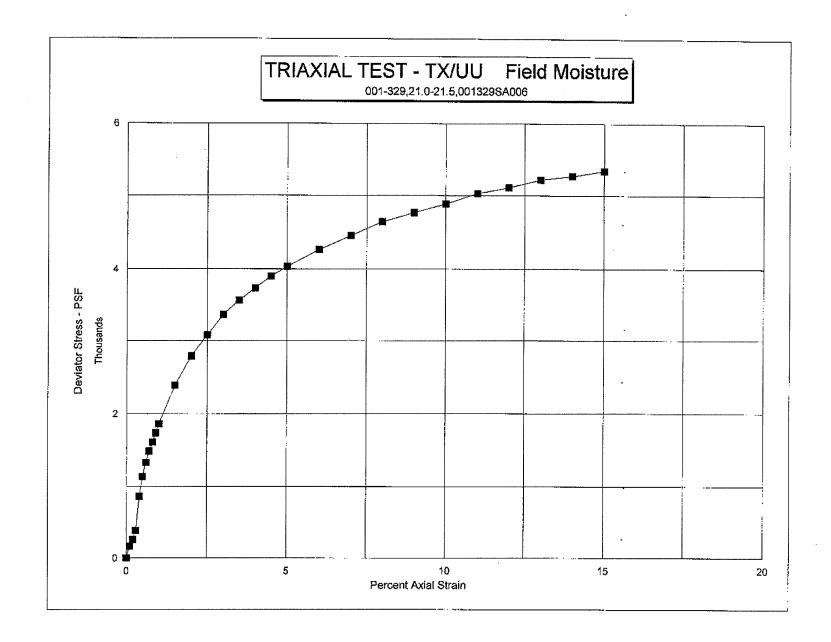


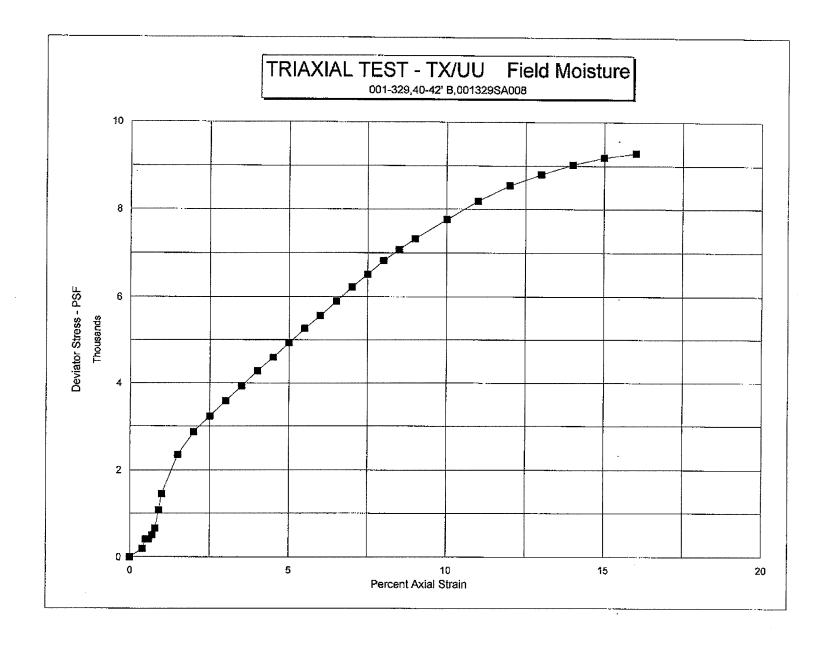


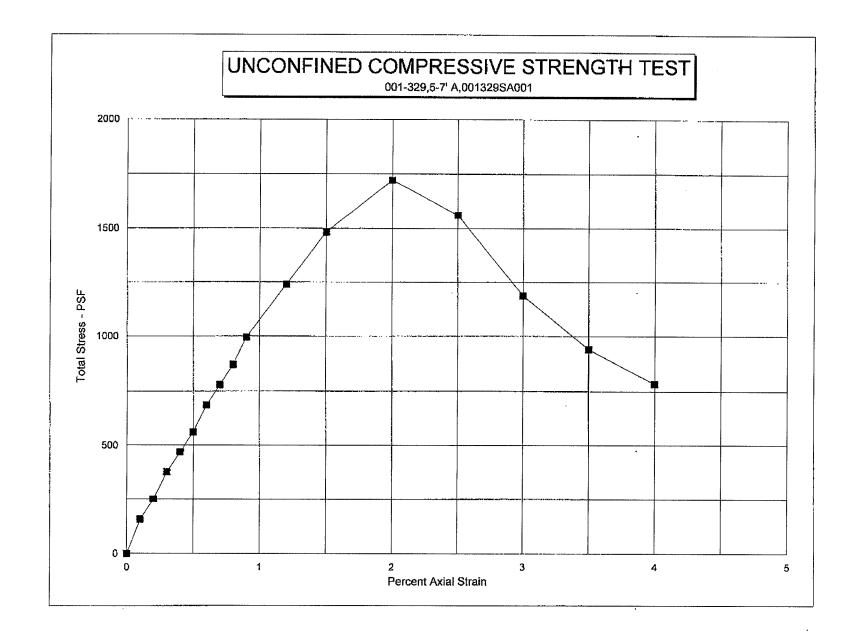


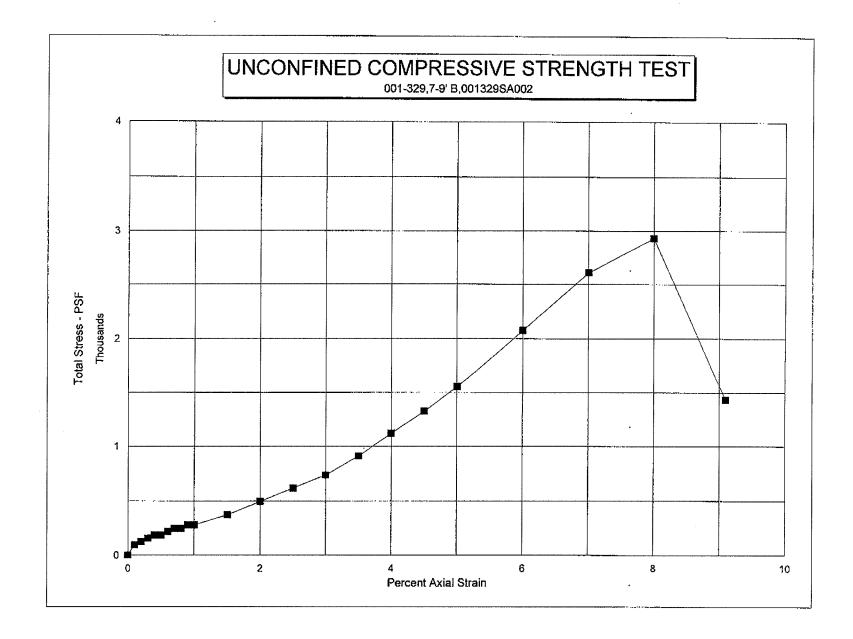


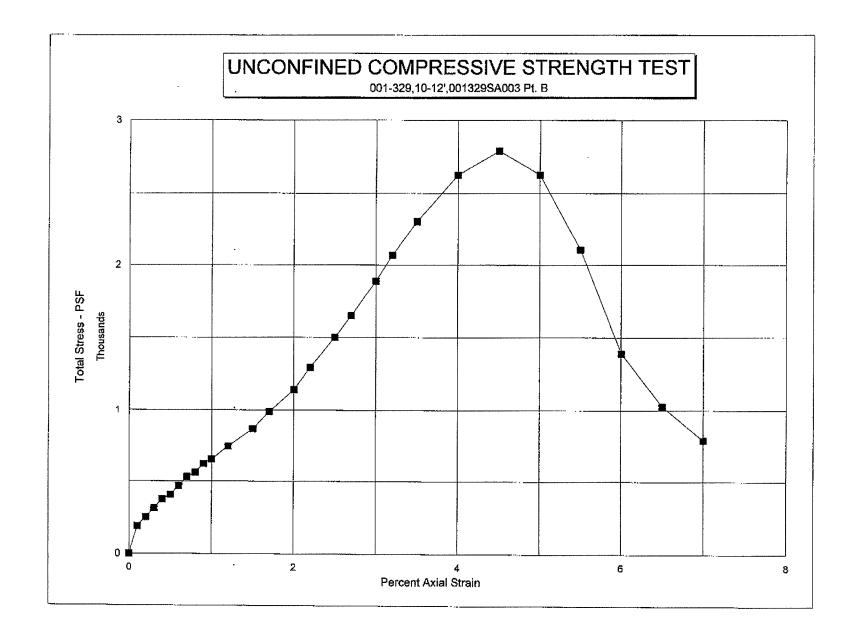


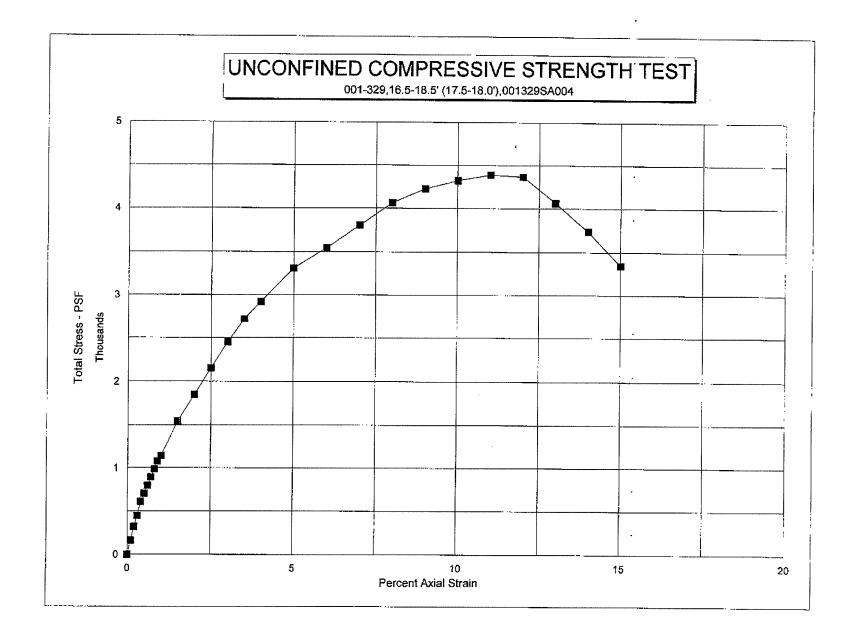


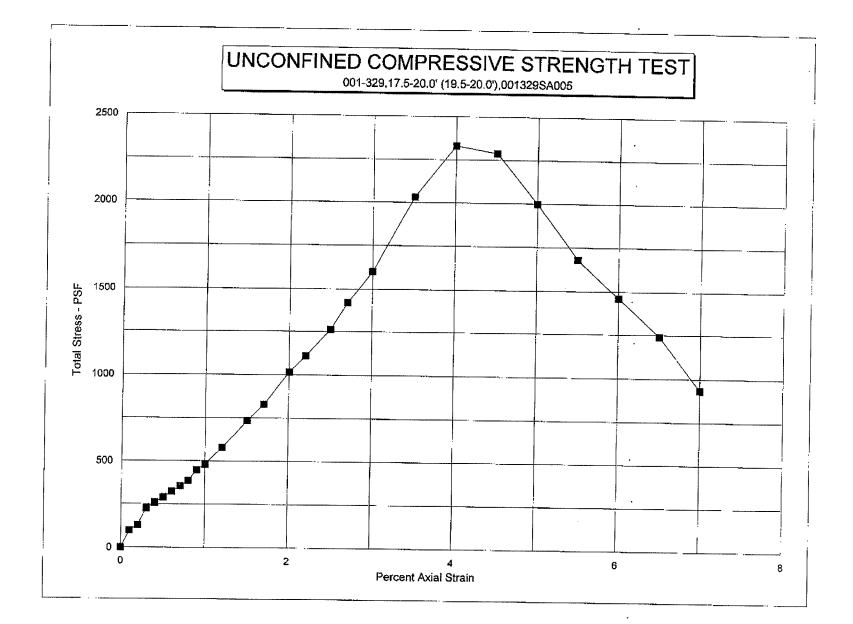


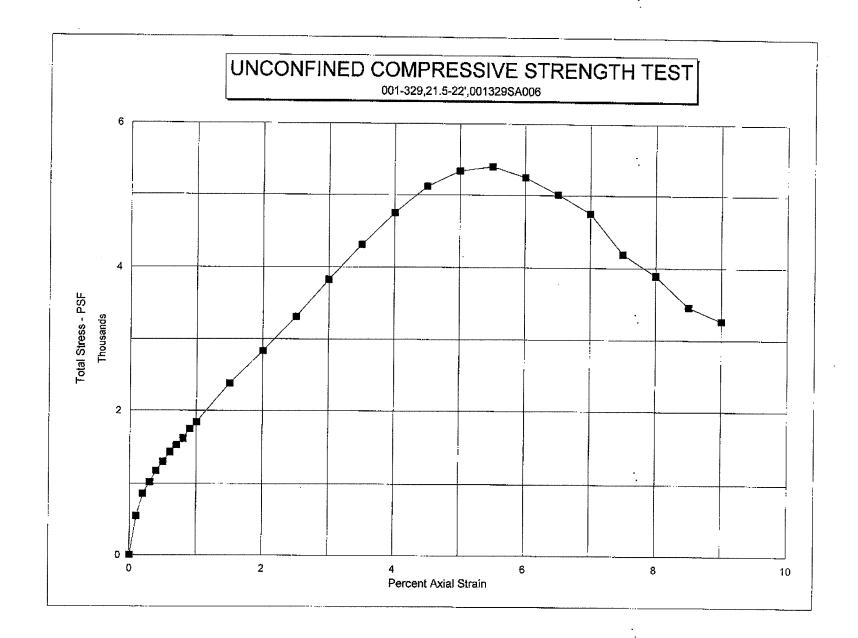


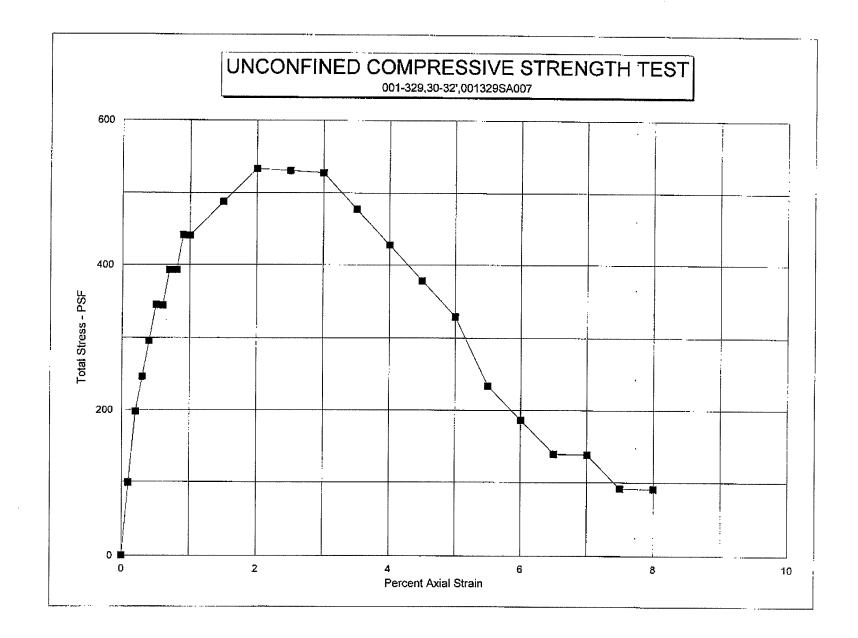


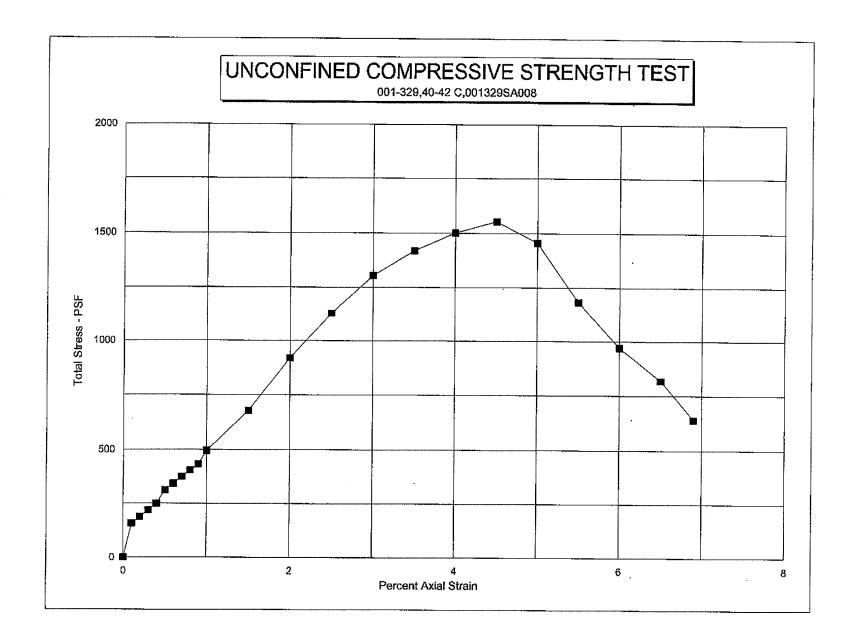


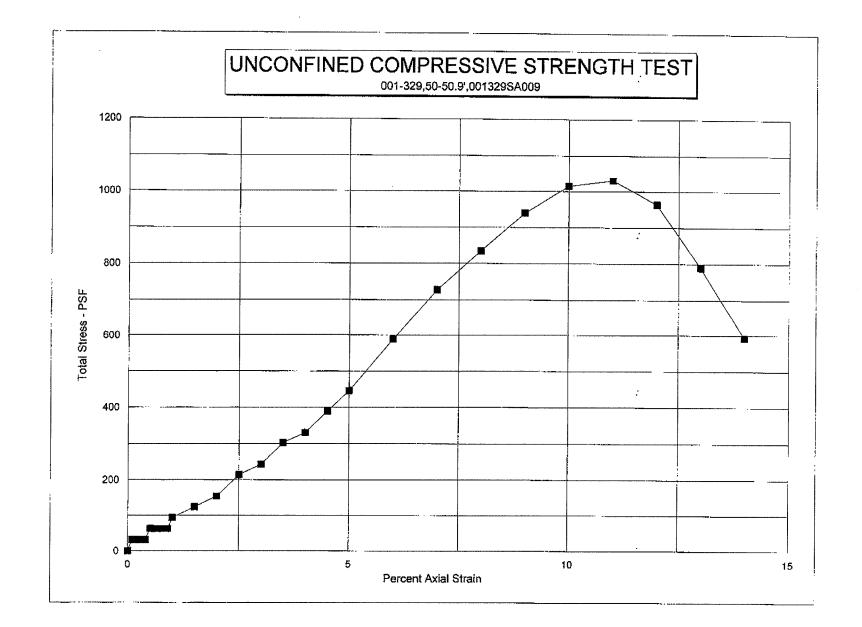


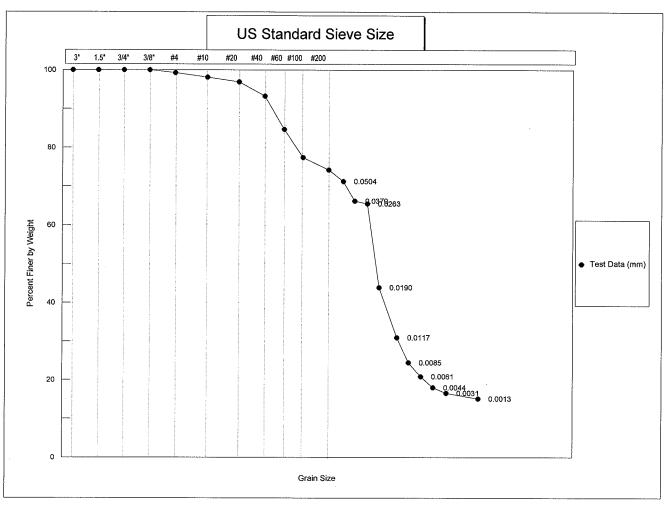












COBBLES	GF	RAVEL			SAND			SILT OR CLAY (mm)		
	COARSE	FI	NE (CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE C	RAVE	-	SA	AND		SILT	CLAY	
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORTH

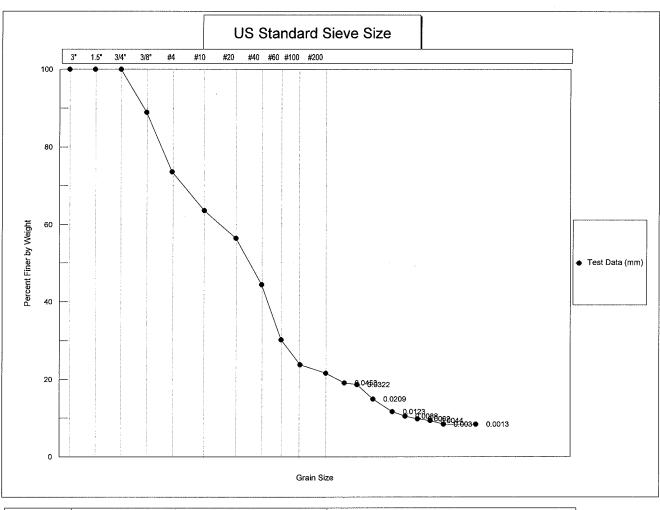
Classification:

LATA Kentucky

Depth:

Boring No.: 001-306

10-13' **Classification Not Performed** Sample No.: 001306GRNSZ1



COBBLES	GF	AVEL			SAND			SILT O]	
	COARSE	FII	NE (CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE (GRAVEL	_	SA	ND		SILT	CLAY	WENTWORTH
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORTH

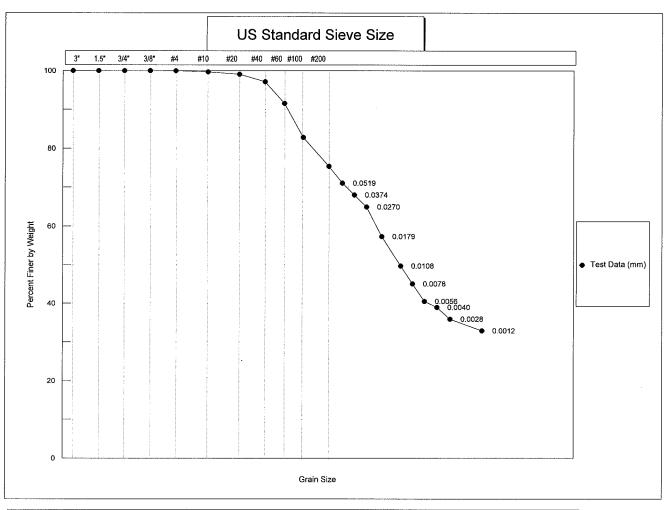
Classification:

LATA Kentucky

Boring No.: 001-306

Depth: 15-20'
Classification Not Performed

Sample No.: 001306GRNSZ2



COBBLES	GR	GRAVEL			SAND			SILT O		
	COARSE	FINI	E C	CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE GF	RAVEL	-	SA	ND		SILT	CLAY	
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORTH

Classification:

LATA Kentucky

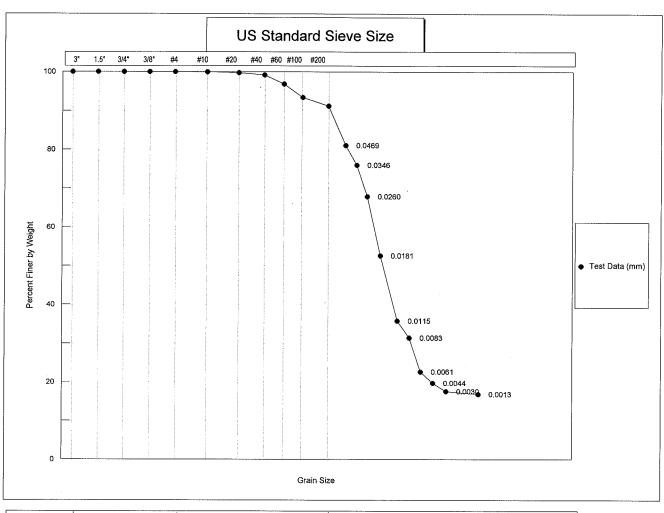
Boring No.: 001-306

Depth:

32.7-34.0'

Classification Not Performed

Sample No.: 001306GRNSZ3

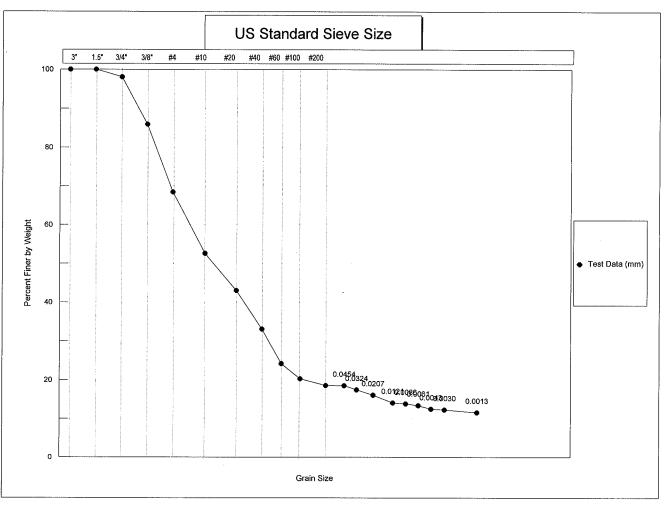


COBBLES	GR	AVEL			SAND			SILT OR CLAY (mm)		
	COARSE	FII	NE	CRS	MEDIUM	FINE	3	•		USCS
COBBLES	PE	BBLE C	RAVE	L	SA	ND		SILT	CLAY	
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORTH

Client: LATA Kentucky
Job Number: 2855-01
Classification: Cla

Boring No.: 001-307 Depth: 12.5-14.6'

Sample No.: 001307GRNSZ1



COBBLES	GRAVEL				SAND			SILT O		
	COARSE	FI	NE	CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE C	RAVE		Si	AND		SILT	CLAY	
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORTH

Client:

LATA Kentucky

Boring No.: 001-307

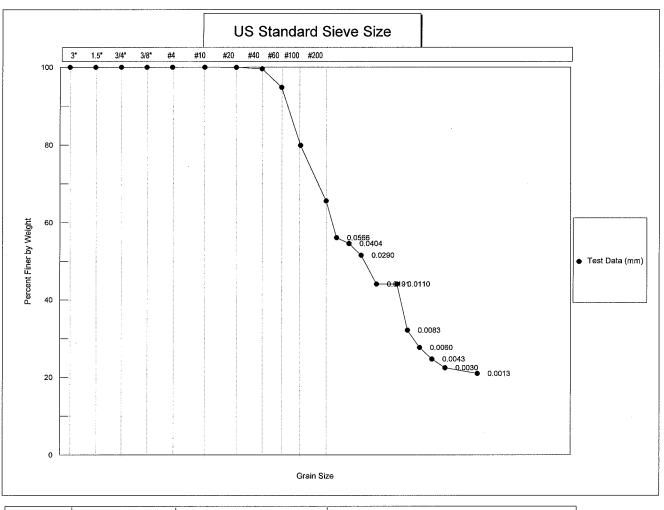
Depth:

Sample No.: 001307GRNSZ2

Job Number: 2855-01

19.4-21.9'

Classification:



COBBLES	GF	RAVEL			SAND			SILT OF	R CLAY (mm)		
	COARSE	FII	NE (CRS	MEDIUM	FINE				USCS	
COBBLES	PE	BBLE G		L	SA	ND		SILT	CLAY	WENTWORTH	
TO BOULDERS	COARSE	MED	l .	GRAN	COARSE	MED	FINE			WENTWORTH	

Sample No.: 001307GRNSZ3

Client:

LATA Kentucky

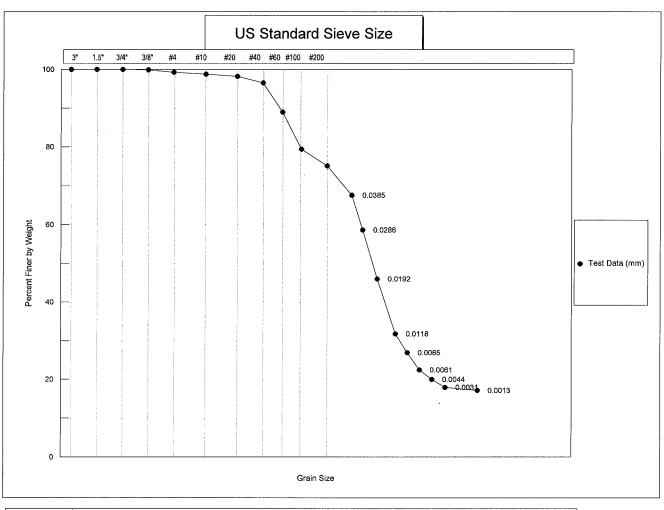
Boring No.: 001-307

Job Number: 2855-01

Depth:

30.0-33.7'

Classification:



COBBLES	GF	RAVEL			SAND			SILT O	R CLAY (mm)	
	COARSE	Fil	NE	CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE (RAVE	L,	SA	ND		SILT	CLAY)
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORTH

Classification:

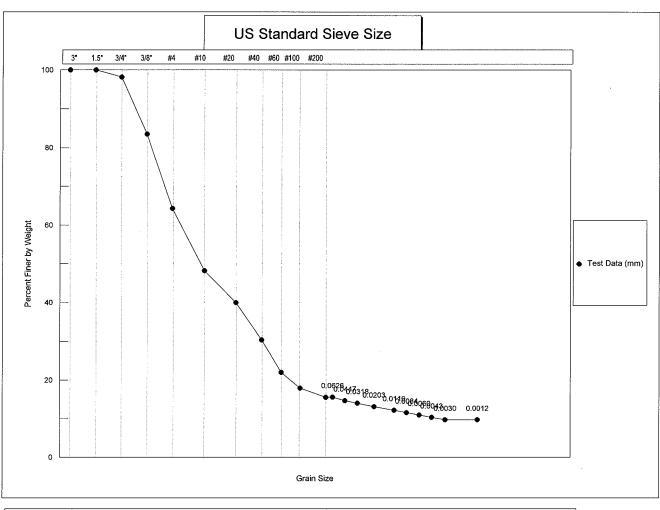
LATA Kentucky

Classification Not Performed

Boring No.: 001-316

10-14' Depth:

Sample No.: 001316GRNSZ1



COBBLES	GR	AVEL			SAND		SILT OR CLAY (mm)			
	COARSE	FI	NE	CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE C				ND		SILT	CLAY	WENTWORTH
TO BOULDERS	COARSE	MED	l	GRAN		MED	FINE			WENTWORTH

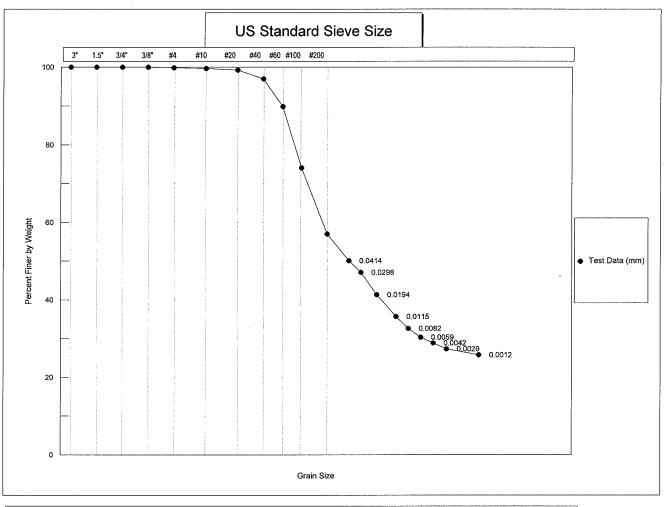
Classification:

LATA Kentucky

Boring No.: 001-316

Depth: 20-23'
Classification Not Performed

Sample No.: 001316GRNSZ2



COBBLES	GR	RAVEL			SAND			SILT O		
	COARSE	FIN	1E (CRS	MEDIUM	FINE				USCS
COBBLES	PE	BBLE G	RAVE	-	SA	ND		SILT	CLAY	
TO BOULDERS	COARSE	MED	FINE	GRAN	COARSE	MED	FINE			WENTWORT

Job Number: 2855-01

LATA Kentucky

Boring No.: Depth:

001-316

32-35'

Sample No.: 001316GRNS2873 9/m 6/27/12

Classification:

APPENDIX D AIR DISPERSION ANALYSIS



D.1 AIR DISPERSION ANALYSIS

D.1.1 INTRODUCTION

This appendix describes the air dispersion analysis of potential hazardous air pollutant (HAP) and/or toxic air pollutant (TAP) emissions from the implementation of the remedial action (RA) to be implemented at the Southwest Groundwater Plume source area at Paducah Gaseous Diffusion Plant (PGDP) at Solid Waste Management Unit (SWMU) 1. The property boundary concentrations for potential HAP and/or TAP emissions were estimated using BREEZE AERMOD Version 7.7.1. Report printouts and electronic model-ready input files are included in the attachment to this appendix.

Air Dispersion Model Selection

The BREEZE AERMOD Version 7.7.1 program was used to conduct air dispersion modeling using the latest version (12345) of the American Meteorological Society Environmental Protection Agency Regulatory Model (AERMOD) to estimate maximum ground-level concentrations. AERMOD is a steady-state plume model that incorporates air dispersion based on planetary boundary layer turbulence structure and scaling concepts, including treatment of both surface and elevated sources, and both simple and complex terrain.

Modeling Receptor Grids

Ground-level concentrations were calculated within one Cartesian receptor grid and at receptors placed along the U.S. Department of Energy (DOE) property line (property line). The property line grid receptors were spaced at a maximum of approximately 50 meters apart. The Cartesian receptor grid extending out a minimum of 600 meters beyond the property line was spaced at 200-meter intervals in all directions. The Cartesian receptor grid was generated to ensure concentrations were decreasing away from the property line. All resultant maximum concentrations occur well within this distance.

Terrain

AERMOD uses advanced terrain characterization to account for the effects of terrain features on plume dispersion and travel. AERMOD's terrain pre-processor, AERMAP (latest version 11103), imports digital terrain data and computes a height scale for each receptor from National Elevation Dataset (NED) data files. A height scale is assigned to each individual receptor and is used by AERMOD to determine whether the plume will go over or around a hill.

The modeled receptor terrain elevations input into AERMAP are the highest elevations extracted from United States Geological Survey (USGS) 1:24,000 scale (7.5-minute series) NED data for the area surrounding PGDP. For each modeled receptor, the maximum possible elevation within a box centered on the receptor of concern and extending halfway to each adjacent modeled receptor was chosen. This is a conservative technique for estimating terrain elevations by ensuring that the highest terrain elevations are accounted for in the analysis. HAP/TAP emission concentrations were calculated at all receptors.

Building Downwash Analysis

The emission unit was evaluated in terms of its proximity to nearby structures. The purpose of this evaluation was to determine if stack discharge might become caught in the turbulent wakes of these structures leading to downwash of the plume. Wind blowing around a building creates zones of turbulence that are greater than if the building were absent. The current version of the AERMOD dispersion model treats building wake effects following the algorithms developed by Schulman and Scire. This approach requires the use of wind direction-specific building dimensions for structures located within 5L of a stack, where L is the lesser of the height or projected width of a nearby structure. Stacks taller than the Good Engineering Practice (GEP) stack height, which is the structure height plus 1.5L are not subject to the effects of downwash in the AERMOD model. The emissions unit's stack height is greater than the GEP stack height. Therefore, there are no buildings which are considered nearby for the purposes of modeling and no further evaluation of cavity or wake effects is required.

D.1.2 IDENTIFICATION OF AIR POLLUTANTS

The potential HAPs/TAPs that could be emitted by the RA (LDA soil mixing with steam and ZVI injection) have been identified based on soil characterization. The soil treatment area characterization is documented in *the 90% RDR and previous investigation reports for SWMU 1*. The potential HAPs/TAPs that could be emitted are trichloroethene (TCE), vinyl chloride, *trans*-1,2-dichloroethene (DCE), *cis*-1,2-DCE, and 1,1-DCE.

D.1.3. ALLOWABLE OFF-SITE CONCENTRATIONS CALCULATIONS

The treated vapor/gases must comply with the contaminant concentration requirements of 401 KAR 63:020. This states that no owner or operator shall allow any affected facility to emit potentially hazardous matter or toxic substances in such quantities or duration as to be harmful to the health and welfare of humans, animals and plants.

D.1.3.1 TCE and Vinyl Chloride Allowable Off-site Concentrations

The maximum allowable air concentration for TCE and Vinyl Chloride were estimated using the EPA Region 9 Regional Screening Levels (RSL), formerly referred to as Preliminary Remediation Goals (PRGs), which are available from the EPA's website at: http://www.epa.gov/region9/superfund//prg/index.html. The TCE and Vinyl Chloride values are based on the carcinogenic risk posed by lifetime² exposure to each HAP/TAP. The health effects of exposure to TCE and Vinyl Chloride are measured by a target risk of one in one million (1 x 10⁻⁶). The residential RSLs were used to develop an allowable off-site concentration limits.

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¹ Earth Tech, Inc., Addendum to the ISC3 User's Guide, The PRIME Plume Rise and Building Downwash Model, Concord, MA.

² Lifetime exposure is assumed to be 70 years by convention for this air toxics risk assessment. http://www.epa.gov/reg3hwmd/risk/human/rb-concentration_table/usersguide.htm. In such assessments, if exposure duration is less than 70 years, inhalation exposure estimates and/or allowable off-site concentrations limits may be adjusted accordingly. http://epa.gov/ttn/fera/risk_atra_vol2.html. For simplicity in this report, allowable off-site concentration limits were not adjusted although exposure duration is expected to be less than 70 years for this project.

The ambient air allowable off-site concentrations for TCE and Vinyl Chloride are $0.43~\mu g/m^3$ and $0.16~\mu g/m^3$, respectively. The allowable off-site concentration for TCE was selected from the most recent EPA publication of RSLs, which occurred in November 2012.

The allowable off-site concentrations of TCE and vinyl chloride were also calculated based on the U.S. Environmental Protection Agency (EPA) Air Toxics Risk Assessment Reference Library, Volume 2, Facility Specific Assessment. These values were obtained from the US EPA website, located at the following address: http://www.epa.gov/ttn/atw/toxsource/table1.pdf.

Both TCE and vinyl chloride are possible carcinogens. The cancer chronic inhalation value for each is used in calculating the maximum allowable concentration. The value for TCE is 4.1E-06 per $\mu g/m^3$ and the value for vinyl chloride is 0.0000088 per $\mu g/m^3$. The allowable risk is assumed to be 1 x 10⁻⁶. The maximum allowable concentration is calculated by the following formula:

Allowable Risk = Estimate of continuous inhalation exposure X Inhalation Unit Risk Estimate

Or

Estimate of continuous inhalation exposure = Allowable Risk/Inhalation Unit Risk Estimate

For TCE the calculation would be as follows:

TCE Allowable concentration = $1 \times 10^{-6}/4.1E-06$ per $\mu g/m^3$

TCE Allowable concentration = $0.24 \mu g/m^3$

Using the same approach for vinyl chloride, the allowable concentration would be $0.11 \ \mu g/m^3$.

D.1.3.2 DCE Allowable Off-site Concentrations

The maximum allowable air concentrations for dichloroethene (DCE) were also estimated using the EPA RSL. The health effects of exposure to DCE are measured by a hazardous index, with a hazard index of 1 being an indication of the nearest off-site receptor having detrimental health effects from exposure to DCE. The residential RSL was used to develop an allowable off-site concentration limit.

DCE is present in three chemical forms, as follows: 1,1-DCE; *cis*-1,2-DCE, and *trans*-1.2-DCE. The ambient air allowable off-site concentration for each chemical form is 1,1-DCE—210 µg/m³; *cis*-1,2-DCE—37 µg/m³; and *trans*-1,2-DCE—63 µg/m³. The allowable off-site concentrations for 1,1-DCE and *trans*-1,2-DCE were selected from the most recent EPA publication of RSLs, which occurred in November 2012. The allowable off-site concentration value for *cis*-1,2-DCE was selected from the list of PRGs since EPA has not published a revised value for that chemical form since October 2004.

All of the allowable off-site concentrations for TCE, Vinyl Chloride and DCE are shown in Table D.1.

Table D.1. Allowable Off-site Concentration Limits

Pollutant	Allowable Off-site Concentration (µg/m³)	Reference Source
TCE	0.24/0.43*	EAP Air Toxics Risk Assessment Reference Library,
		Volume 2, Facility Specific Assessment/ Regional
		Screening Levels, last updated November 2012
Vinyl chloride	0.11/0.16*	EAP Air Toxics Risk Assessment Reference Library,
		Volume 2, Facility Specific Assessment/ Regional
		Screening Levels, last updated November 2012
1,1-DCE	210	Regional Screening Levels, last updated November 2012
cis-1,2-DCE	37	Preliminary Remediation Goals, last updated October 2004
trans-1,2-DCE	63	Regional Screening Levels, last updated November 2012

^{*}The first value is a result based on the EAP Air Toxics Risk Assessment Reference Library and the second value is based on Region 9 Screening Levels.

D.1.4 ESTIMATED EMISSION RATES

D.1.4.1 Emissions

During operation of the project, hazardous constituents in the subsurface will be volatilized underground and recovered by an off-gas extraction and vapor conditioning system. The system will capture the soil vapors, which will be treated and released through a stack. The current design uses three (3) vapor-phase granular activated carbon (VGAC) units to remove hazardous constituents from the off-gas prior to discharge to the atmosphere. The current design criteria for the treatment system is such that each VGAC will have a removal efficiency of a minimum of 90%, or 99.9% for 3 VGACs, for HAP/TAP.

In order to estimate the maximum off-site concentration the exhaust was assumed to contain the maximum concentration of each HAP. The following preliminary design parameters for the stack were used in the model to estimate the dispersion of the hazardous constituents:

- 6-inch diameter
- 15-ft high
- 600 to 1,500 scfm flow rate
- 90°F exhaust gas temperature
- The stack will be equipped with a raincap

The vertical component of the stack exit velocity is required to be used in the air dispersion modeling analysis. Because the proposed stack will be outfitted with a raincap, the modeled stack exit velocity was set to 0.001 meters per second.

The maximum emission rate in kilograms per day were estimated based on the following assumptions:

- The average mass concentration for each individual HAP/TAP for each boring, representing a worst-case scenario based on Remedial Design Support Investigation (RDSI) sampling results. For example, it was assumed that the average TCE concentration in boring 001-310 of 133,034 µg/kg was applied through the entire volume of each Large Diameter Auger (LDA) boring (representing approximately 111.7 cubic yards per boring) and the soil density was assumed to be 1.62 tons/yd³. Based on these assumptions, a calculated TCE mass of approximately 21.8 kg per LDA boring was estimated.
- A boring installation rate of four (4) borings per 10 hour workday.

- Air control measures utilizing three (3) VGAC units result in HAP/TAP concentration reductions of at least 99.9% prior to atmospheric discharge.
- The estimated daily emission rates were converted to a gram-per-second emission rate using 24 hour averaging period.

The maximum emission rates during operation are listed in Table D.2 in both kilograms per day (kg/day) and grams per second (g/s).

Table D.2. Estimated Emission Rates

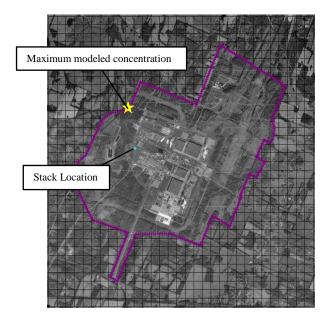
Pollutant	Stack I	Design Concentra	ation
	Uncontrolled	Uncontrolled	Controlled
	kg/day	g/s	g/s
TCE	87	1.0	1.0×10^{-3}
Vinyl chloride	$3.3x10^{-3}$	3.8x10 ⁻⁵	3.8x10 ⁻⁸
1,1-DCE	$2.0 \text{x} 10^{-3}$	2.3x10 ⁻⁵	2.3x10 ⁻⁸
cis-1,2-DCE	0.8	8.7×10^{-3}	8.7x10 ⁻⁶
trans-1,2-DCE	6.6x10 ⁻⁴	7.6×10^{-6}	7.6x10 ⁻⁹

D.1.4.3 Maximum Off-site Concentrations

The property boundary ambient concentration for each HAP/TAP was estimated using the air dispersion model BREEZE AERMOD Version 7.7.1.

Surface meteorology data from station number 3816 (Paducah, KY) and the nearest available upper air meteorology data from station 00013897 (Nashville, TN) were used. Dispersion analysis was performed using meteorological data from these stations for calendar years 2008, 2009, 2010, 2011 and 2012 (January 1, 2008 through December 31, 2012). The AERMOD-ready meteorological files were purchased from Trinity Consultants, Inc.

The air dispersion modeling analysis was performed assuming an emission rate of one gram per second. The resulting maximum modeled concentration, averaged over the entire year, was then multiplied by the aforementioned pollutant-specific controlled emission rate to estimate the off-site concentration for each pollutant. The results of the air dispersion modeling analysis suggest that the maximum annual average concentration occurs at a receptor (338132.20m, 4110280.70m) along the property boundary northwest of the proposed stack location, as illustrated below:



The estimated maximum annual average concentration for each pollutant is shown in Table D.3.

Table D.3. Estimated Off-site Concentrations

Pollutant	Off-Site Concentration Limit	Annual Average Maximum Off-site Concentration
	$\mu g/m^3$	$\mu g/m^3$
TCE	0.24/0.43*	6.3x10 ⁻³
Vinyl chloride	0.11/0.16*	2.4x10 ⁻⁷
1,1-DCE	210	1.4x10 ⁻⁷
cis-1,2-DCE	37	5.5x10 ⁻⁵
trans-1,2-DCE	63	4.8x10 ⁻⁸

^{*}The first value is a result based on the EAP Air Toxics Risk Assessment Reference Library and the second value is based on Region 9 Screening Levels.

The results of this air dispersion modeling analysis show the estimated maximum annual average concentration for each pollutant will be below the corresponding maximum allowable off-site concentration of respective pollutants. Additionally, the allowable off-site concentration limits for pollutants were developed using a lifetime (i.e., 70-year exposure period) per EPA's RSL User's Guide.³ The duration of potential exposure associated with the operation of the VGAC will be less than 70 years. Therefore, emissions associated with this project are not expected to be harmful to the health and welfare of humans, animals, or plants.

D.1.4.4 Sensitivity to Stack Concentration

The sensitivity of property boundary concentrations as a function of pollutant concentrations in the exhaust stream was analyzed. The maximum stack concentrations that resulted in the property boundary concentrations at the allowable limits were estimated using the air dispersion software. The exhaust flow

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³ http://www.epa.gov/reg3hwmd/risk/human/rb-concentration_table/usersguide.htm

rate was conservatively assumed to be 600 scfm, the minimum flow rate from the VGAC units. To add an additional measure of conservatism, a factor of safety of 1.5 was applied to the Maximum Exhaust Pollutant Concentration. Table D.4 lists the maximum exhaust concentrations.

Table D.4. Maximum Exhaust Pollutant Concentrations that Result in Property Boundary Concentrations at the Off-site Limit

Pollutant	Off-site Limit	Maximum Exhaust Pollutant Concentration	Maximum Exhaust Pollutant Concentration (with Safety Factor)
	μg/m ³	ppmv	ppmv
TCE	0.24/0.43*	34	23
Vinyl chloride	0.11/0.16*	72	48
1,1-DCE	210	47	31
cis-1,2-DCE	37	47	31
trans-1,2-DCE	63	47	31

^{*}The first value is a result based on the EAP Air Toxics Risk Assessment Reference Library and the second value is based on Region 9 Screening Levels.

Based on this analysis, it is concluded that the maximum exhaust concentrations described above may result in an exceedance of limits at the property boundary. The maximum exhaust pollutant concentrations, with the applied safety factor, represent the proposed operational limits or concentrations that may be utilized to trigger a work stoppage for evaluation of and correction to the applied off-gas treatment measures.



ATTACHMENT AIR DISPERSION ANALYSIS REPORTS AND MODEL READY INPUT FILES



CD—AERMOD INPUT AND OUTPUT FILES (see back cover).

